

# BOUNDARY LAYER ANALYSIS

## SECOND EDITION

Joseph A. Schetz  
Rodney D. W. Bowersox

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$$

$$u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = -\frac{1}{\rho} \frac{dp}{dx} + \nu \frac{\partial^2 u}{\partial y^2}$$

$$\frac{\partial p}{\partial y} \approx 0$$

American Institute of  
Aeronautics and Astronautics

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# *Boundary Layer Analysis*

## **Second Edition**

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*This book is dedicated to our very gracious, patient, and  
supportive wives, Katherine Schetz and Selina Bowersox.*

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# PREFACE

This book is intended as a text for courses in viscous fluid flow at high Reynolds numbers for advanced undergraduate and beginning graduate engineering students. Numerous homework problems ranging from the simple, but instructive, to the challenging are included. The emphasis is on understanding and analyzing flows of engineering interest. Thus, turbulent flows receive primary coverage, and a modern understanding of the physics of turbulent shear flows and turbulence models is discussed in detail. Further, the accurate analysis of practical flow problems, especially those involving turbulence, requires the use of computerized methods, so numerical methods are treated in depth. Coverage of the older analytical methods is also included, to aid in developing understanding and because such methods are still widely used in preliminary design, especially for design optimization studies.

Several computer codes for both modern numerical and older analytical methods in the form of applets written in the JAVA language have been developed and made available on the Internet (see the Supporting Materials page) to accompany this text. Numerous worked examples are provided to illustrate the use and capability of these applets. The applets were designed primarily for solving homework problems, but working professionals have also found them useful.

A second major theme of this volume is a concurrent treatment of the transfer of momentum, heat, and mass. This is primarily a book on viscous fluid dynamics, but the processes of convective heat and mass transfer are so closely connected to momentum transfer that a unified presentation was deemed valuable. Such a presentation allows the scope of the book to span the entire range from low-speed to hypersonic flows. In addition, including mass transfer permits a discussion of viscous flows with chemical reactions.

An introductory coverage of simple non-Newtonian fluids of the *power law* and *Bingham plastic* types is also provided to orient the student to some of the important differences found with such fluids, compared to the more usual Newtonian fluids.

Chapter 1 is devoted to an introduction to the subject of viscous flow and why it is important to the engineer. The relevant physical phenomena and properties and dimensionless numbers are discussed. Then, the exact



equations of motion for a constant-density fluid and the boundary layer assumptions are derived. The phenomena of flow separation and the *Kutta condition* are described next. The last section introduces the basic ideas associated with turbulent flows.

The subject matter of Chapter 2 is the approximate solution to laminar boundary layer problems, including heat and mass transfer, based on the integral forms of the equations. Worked examples and JAVA applets for the Thwaites-Waltz method and a corresponding integral method for heat transfer are presented.

Chapter 3 is concerned with the derivation of the boundary layer equations expressing conservation of total mass, momentum, energy, and mass of species, including variable density and properties.

The coverage in Chapter 4 begins with a few of the exact solutions for special cases of laminar flow. Then, *similar solutions* are discussed. The remainder of the chapter deals with numerical solutions of boundary layer problems using the finite difference method and the finite element method. Worked examples and JAVA applets are included.

Chapter 5 discusses high-speed laminar flows. Viscous heating, compressible transformations, numerical solutions, and viscous-inviscid interactions are covered. Again, worked examples and a JAVA applet are given.

Transition to turbulent flow is treated in Chapter 6, which has been expanded from the previous edition. Hydrodynamic stability and the  $e^N$  method are described. Finally, selected empirical information is presented to illustrate the influence of roughness, pressure gradients, injection or suction, supersonic flow, and the like.

Updated from the previous edition, a detailed discussion of the nature of the turbulent, wall-bounded flows and modern turbulence models is the focus of Chapter 7. The discussion is limited to constant-density flows for clarity. The problems of analyzing turbulent flow problems are emphasized. Integral and numerical methods are discussed, and extensive comparisons of predictions with experiment are provided. Worked examples and JAVA applets are presented.

The important subject of laminar and turbulent internal flows has been highlighted by devoting a separate chapter, Chapter 8, to that topic alone.

Chapter 9 covers free shear flows, such as wakes, jets, and shear layers. Both laminar and turbulent cases are considered over the range from low to high speeds. Worked examples as well as a JAVA applets are provided.

Wall-bounded turbulent flows of variable density and properties are discussed in Chapter 10. Both low- and high-speed cases are included. Worked examples and JAVA applets are presented.

Chapter 11 contains a detailed presentation of current knowledge for truly three-dimensional boundary layer flows, including three-dimensional jets.

A key addition to the second edition is a completely new chapter, Chapter 12, that provides an introduction to the numerical solution of high-Reynolds-number viscous flow problems using the full Navier-Stokes equations rather than invoking the boundary layer approximation. The primary focus is on the finite volume methods. The important subject of grid generation is discussed. A convenient JAVA applet has been developed and is presented, and this permits the student to make computations using both boundary layer and Navier-Stokes equations formulations and to compare the results, limitations, and computational burden. The use of the Navier-Stokes applet is illustrated with a worked example. Finally, this applet allows the student to perform simulations that involve separated flows.

Throughout the first eleven chapters of the book, separating, but not separated, flows are discussed because the analysis of the latter cannot be handled with the usual boundary layer equations. Separated flows can be handled only with the methods presented in Chapter 12. Last, unsteady flows are not covered, and that is justified by the observation that those phenomena are usually omitted in courses at the level intended here.

The goal of this effort was to write a book appropriate for mechanical, aerospace, civil, ocean, and chemical engineering students. The treatment assumes that the student has taken at least one general undergraduate course in fluid mechanics and one in mathematics with partial differential equations. It also assumes that the student is computer literate. The computer codes accompanying this book are written in JAVA and made available on the Internet (see the Supporting Materials page). A course that would encompass the bulk of the material in this volume would likely be a two-semester graduate course. A good one-semester graduate course at the undergraduate or graduate level can be formed with a judicious selection of all the material supplied. The selection of topics to be covered in a given course will clearly be strongly influenced by the subject area of the students. It is suggested, however, that all students receive some coverage of numerical solution techniques and turbulence models.

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August 2011



# NOMENCLATURE

$a$	= speed of sound and amplification factor
$A$	= area or constant
$A, B$	= inviscid flux Jacobians ( $\partial f/\partial Q, \partial g/\partial Q$ )
$A_\nu, B_\nu$	= viscous flux Jacobians ( $\partial f_\nu/\partial Q, \partial g_\nu/\partial Q$ )
$b_{1/2}$	= half-width
$B_1, B'_2, B'_1, B'_2$	= constants
$B_{fh}$	= injection/suction parameters
$c$	= average speed of molecules
$c'_i$	= fluctuating value of species concentration
$c_i$	= species concentration
$\bar{C}_i$	= mean value of species concentration
$C_1, C_2, C_\mu$ etc.	= constants
$c_{b1}, c_{b2}, c_{w1}$ , etc.	= constants in Spalart-Allmaras turbulence model
$c_p$	= specific heat at constant pressure
$c_v$	= specific heat at constant volume
$c_r, c_i$	= real and imaginary parts of the phase velocity
$C_f$	= skin friction coefficient
$\bar{C}_f$	= average skin friction coefficient
$C_p$	= pressure coefficient
$C_D$	= drag coefficient
$D, d$	= diameter and minor axis in three-dimensional jets
$D$	= dissipation term in the finite volume flux evaluation
$\mathcal{D}$	= drag
$D_h$	= hydraulic diameter
$D_{ij}$	= binary diffusion coefficient
$D_T$	= turbulent diffusion coefficient
$e$	= internal energy
$E_1(k_1)$	= kinetic energy of axial fluctuations at wave number $k_1$
$f$	= friction factor
$f(\cdot)$	= function of $(\cdot)$
$f_i$	= body force vector
$f_1, f_2, f_\mu$	= factors in $K\epsilon$ model
$f_{\nu 1}, f_{\nu 2}, f_{t2}, f_w$	= quantities in Spalart-Allmaras turbulence model
$f, g, h$	= inviscid flux vectors in the $x$ -, $y$ -, and $z$ -directions, respectively

$f^+, g^+, h^+$	= positive eigenvalue inviscid flux vectors
$f^-, g^-, h^-$	= positive eigenvalue inviscid flux vectors
$f_v, g_v, h_v$	= viscous flux vectors in the $x$ -, $y$ -, and $z$ -directions, respectively
$F_i$	= element force vector
$g$	= acceleration of gravity, Clauser similarity variable, Johnson-King variable, Spalart-Allmaras quantity, and $G/(1 - G_w)$
$G$	= stagnation enthalpy ratio
$h$	= enthalpy
$h$	= film coefficient
$h_D$	= film coefficient for diffusion
$h_1, h_3, h_c$	= metric coefficients
$H$	= stagnation enthalpy
$H(\Lambda)$	= shape factor
$i$	$\equiv \sqrt{-1}$
$j$	= index
$J$	= integrated momentum flux
$k$	= thermal conductivity and average roughness size
$k_m$	= Crocco-Lees mixing constant
$k_T$	= turbulent thermal conductivity
$k_1$	= wave number of fluctuations
$K$	= turbulent kinetic energy
$K(T)$	= equilibrium constant
$K_1, K_2$ , etc.	= constants and geodesic curvatures
$K_{ij}$	= element stiffness matrix
$\ell$	= turbulent length scale and arc length
$\ell_m$	= mixing length
$\ell_1$	= major axis in three-dimensional jets
$L_m$	= length scale in Johnson-King model
$Le$	= Lewis number
$Le_T$	= turbulent Lewis number
$m$	= index along surface
$\dot{m}_i$	= diffusive mass flux of species $i$
$M$	= maximum value of index $m$ and Mach number
$M_{cl}$	= convective Mach number
$M_\tau$	= Mach number in compressibility correction
$n$	= index across layer, frequency, and transverse streamline coordinate
$n_y$	= $y$ -component of normal vector to surface
$N$	= maximum value of index $n$
$Nu$	= Nusselt number
$Nu_{Diff}$	= Nusselt number for diffusion

$N_{\text{He}}$	= Hedstrom number
$N_{\text{Pl}}$	= plasticity number
$p$	= pressure and exponent for power law fluids
$p_i$	= partial pressure of species $i$
$p'$	= fluctuating pressure
$P$	= mean pressure, scaled pressure, and perimeter
$P_t$	= total pressure
$P_c, P_T, P_V$	= power law decay exponents
$Pr$	= Prandtl number
$Pr_T$	= turbulent prandtl number
$\mathcal{P}$	= production of turbulent kinetic energy
$q_i$	= heat flux vector
$q_T$	= turbulent heat flux
$q_w$	= wall heat transfer rate
$q^*$	= friction velocity in three-dimensional flows
$Q$	= total velocity in three-dimensional flows and state vector for the conservation laws
$Q_{n,m}$	= state vector at the finite volume cell $n, m$ center
$r$	= radial coordinate, recovery factor, element coordinate, and quantity defined in Spalart-Allmaras turbulence model
$r_0(x)$	= body radius
$r_{1/2}$	= half-radius
$R$	= pipe radius, gas constant, and radius of curvature
$R_{n,m}$	= residual for the finite volume discretization for cell $n, m$
$Ri$	= Richardson number
$Re$	= Reynolds number
$R_0$	= body nose radius of curvature
$Re_t$	= turbulent Reynolds number
$s, \bar{s}$	= transformed streamwise and streamline coordinate and element coordinate
$\Delta s$	= face length of finite volume cell
$S$	= eigenvector (columns) matrix
$S^+$	= positive eigenvector matrix
$S^-$	= negative eigenvector matrix
$\tilde{S}$	= quantity defined in Spalart-Allmaras turbulence model
$Sc$	= Schmidt number
$Sc_T$	= turbulent Schmidt number
$St$	= Stanton number
$St_{\text{Diff}}$	= Stanton number for diffusion
$S(\Lambda)$	= Shear parameter
$t$	= time
$\Delta t_{\text{CFL}}$	= inviscid Courant, Friedrichs and Lewy condition

$T$	= static temperature
$\mathbf{T}_{x,y,z}$	= surface force vector
$T_b$	= bulk temperature
$T^*$	= reference temperature
$T_t$	= total (stagnation) temperature
$T_0$	= time period
$\bar{T}$	= mean temperature
$T'$	= fluctuating temperature
$T_*$	= heat transfer temperature
$T^+$	$\equiv (T_w - \bar{T})T_*$
$u$	= streamwise velocity
$u_{\text{ave}}$	= average velocity
$u_i$	= nodal velocity in FEM
$\bar{u}$	= transformed velocity and velocity from previous iteration in FEM
$\bar{\bar{u}}$	= mass-weighted mean streamwise velocity
$u'$	= fluctuating velocity
$u_*$	= friction velocity
$u^+$	$\equiv U/u_*$
$u_c$	= convective velocity
$U$	= mean streamwise and scaled velocity
$U_p$	= primary direction velocity in a channel
$U_w$	= velocity of moving wall
$v$	= transverse or radial velocity
$v_w$	= transverse velocity at the wall
$v_i$	= nodal velocity in FEM
$\bar{v}$	= transformed velocity and velocity from previous iteration in FEM
$\bar{\bar{v}}$	= mass-weighted mean transverse velocity
$v_0^+$	= dimensionless transverse velocity at the wall
$v'$	= fluctuating transverse velocity
$V$	= mean transverse, scaled and general velocity
$V_0$	= entrainment velocity
$V_{n,m}$	= volume of finite volume cell $n, m$
$V_{C,N}, V_{C,M}$	= contravariant velocities
$V_\phi$	= velocity from scalar potential in a channel
$V_\psi$	= velocity from vector potential in a channel
$w$	= spanwise velocity in three-dimensional flows
$w'$	= fluctuating spanwise velocity
$\bar{W}$	= mean spanwise velocity in three-dimensional turbulent flows and channel half-height
$W_i$	= molecular weight
$W(y/\delta)$	= wake function

$w_A$	= reaction source term
$x$	= streamwise coordinate
$\bar{x}$	= transformed streamwise coordinate
$x_1, x_3$	= coordinates in three-dimensional flows
$x_{PC}$	= length of potential core
$X_i$	= mole fraction of species $i$
$X$	= scaled streamwise coordinate
$y$	= transverse coordinate
$\bar{y}$	= transformed transverse coordinate
$y^+$	= transverse coordinate for the law of the wall, $\equiv yu_*/\nu$
$y_{\max}$	= length scale in Baldwin-Lomax model
$Y$	= transformed and scaled transverse coordinate
$Y_{1/2}, Z_{1/2}$	= half-widths in three-dimensional jets
$z$	= Spanwise coordinate in three-dimensional flows
$z_A$	= dimensionless mass fraction
$Z$	$\equiv k^m \ell^n$
$Z(p, T)$	= compressibility factor
<i>Other</i>	
$\alpha$	= wave number, amplification factor, atom mass fraction, constant in Wilcox $K\omega$ turbulence model, and dissipation model coefficient
$\alpha_T$	$\equiv k_T/\rho c_p$
$\alpha(p)$	= friction law coefficient for power law fluids
$\beta$	= pressure gradient parameter, wave number, quantity in Wilcox $K\omega$ turbulence model, and dissipation model coefficient
$\beta^*$	= constant in Wilcox $K\omega$ turbulence model
$\beta_w$	= wall streamline angle
$\beta_\xi, \beta_\omega$	= pressure gradient parameters in three dimensions
$\beta(p)$	= friction law function for power law fluids
$\chi$	= quantity defined in Spalart-Allmaras turbulence model
$\chi_\omega$	= vortex stretching parameter in Wilcox $K\omega$ turbulence model
$\bar{\chi}$	= hypersonic interaction parameter
$\psi$	= planar stream function
$\Psi$	= axisymmetric stream function
$\hat{\psi}$	= disturbance stream function
$\varepsilon$	= dissipation of turbulent energy
$\varepsilon_{n,m}$	= truncation error
$\varepsilon_{xy}$	= strain
$\rho$	= density
$\lambda$	= Pohlhausen pressure gradient parameter, pipe resistance coefficient, and second viscosity coefficient

$\lambda^*$	= mean free path between molecules
$\Lambda$	= Thwaites-Walz pressure gradient parameter, convective spectral radius, and diagonal eigenvalue matrix
$\Lambda^+$	= positive diagonal eigenvalue matrix
$\Lambda^-$	= negative diagonal eigenvalue matrix
$\tau, \tau_{xy}$	= shear
$\tau_T$	= turbulent shear
$\tau_0$	= yield stress for plastic fluid
$\Omega$	= intermittency and vorticity parameter
$\Omega_e$	= element area
$\Gamma_e$	= element perimeter
$\mu$	= laminar viscosity
$\mu_a$	= apparent viscosity for non-Newtonian fluid
$\mu_{BP}$	= viscosity factor for Bingham plastic fluid
$\mu_{PL}$	= viscosity factor for power law fluid
$\mu_T$	= turbulent viscosity
$\mu_{Tx}$	= turbulent viscosity in the streamwise direction
$\mu_{Tz}$	= turbulent viscosity in the crossflow direction
$\kappa$	= constant in the law of the wall and inverse of channel radius of curvature and Q vector interpolation function parameter
$\kappa_T$	= constant in the temperature law of the wall
$\nu$	= laminar kinematic viscosity
$\nu_T$	= turbulent kinematic viscosity
$\tilde{\nu}$	= variable in Spalart-Allmaras turbulence model
$\phi_i$	= element interpolation function
$\phi$	= amplitude function and dummy variable and Q vector interpolation function parameter
$\phi_{1,2}$	= deformation angle
$\delta$	= boundary layer thickness
$\delta_T$	= thermal boundary layer thickness
$\delta_c$	= concentration boundary layer thickness
$\delta^*, \Delta^*$	= displacement thickness
$\delta_k^*$	= kinematic displacement thickness
$\delta_1^*, \delta_2^*$	= displacement thicknesses in three-dimensional flows
$\Delta_{PS}$	= Perry-Schofield length scale
$\Delta$	= Clauser integral boundary layer thickness
$\theta$	= momentum thickness
$\theta_{11}, \theta_{12}, \theta_{21}, \theta_{22}$	= momentum thicknesses in three-dimensional flows
$\Theta, \Theta_r$	= excess temperature
$\zeta$	$\equiv \delta_T/\delta$
$\Pi$	= wake parameter
$\xi$	= dummy variable and stretched time



$\sigma_d, \sigma_K, \sigma_\omega$	= constants in Wilcox $K\omega$ turbulence model
$\eta$	= similarity variable
$\bar{\eta}$	= transformed transverse coordinate
$\omega$	= dimensionless frequency, variable in $K\omega$ turbulence model, and transformed lateral coordinate
$\omega_x, \omega_y, \omega_z$	= components of vorticity
$\sigma_K, \varepsilon, \tau$	= Prandtl numbers for $K, \varepsilon, \tau$
$\Gamma$	= see Eq. (10.8)
$\gamma$	= ratio of specific heats and stability parameter in three-dimensional flows
$\xi$	= transformed streamwise coordinate
$\text{III}$	= exponent in laminar viscosity relation

*Subscripts*

$c$	= values on the centerline
$e$	= values at the edge of the boundary layer
$j$	= initial values in a jet
$t$	= stagnation values
$w$	= wall values
$\infty$	= conditions in the approach flow

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