V.S. Stepanov

Analysis of Energy Efficiency of Industrial Processes



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Preface

It is universally recognized that the end of the current and the beginning of the next century will be characterized by a radical change in the existing trends in the economic development of all countries and a transition to new principles of economic management on the basis of a resource and energy conservation policy. Thus there is an urgent necessity to study methods, technical aids and economic consequences of this change, and particularly, to determine the possible amounts of energy resources which could be conserved (energy "reserves") in different spheres of the national economy.

An increased interest towards energy conservation in industry, one of the largest energy consumers, is quite natural and is manifested by the large number of publications on this topic. But the majority of publications are devoted to the solution of narrowly defined problems, determination of energy reserves in specific processes and plants, efficiency estimation of individual energy conservation measures, etc. However, it is necessary to develop a general methodological approach to the solution of such problems and create a scientific and methodical base for realizing an energy conservation policy.

Such an effort is made in this book, which is concerned with methods for studying energy use efficiency in technological processes and estimation of the theoretical and actual energy reserves in a given process, technology, or industrial sector on the basis of their complete energy balances.

The book generalizes the results of studies in this field conducted over many years at plants of ferrous and non-ferrous metallurgy with the use of exergy analysis, which were performed by the author himself and with co-authors. These works were started in the 1960s at the Kazakh Energy Institute under the directory of I.Kh. Ozoling and are continued now in the Siberian Energy Institute, Siberian Branch of the Russian Academy of Sciences.

This book is of interest to diverse audience of specialists in the areas of thermodynamics, industrial energetics, and energy economy.

Data for the calculation of energy balances of processes and plants in Chaps. 5, 6 are obtained in a study conducted by the author at plants operating in the USSR. The calculations described in Chap. 8 are based on official statistics, on the data of reports and forecasts from the USSR Ministry of Metallurgy.

Chapters 7 and 8 are written jointly with T. B. Stepanova whose help at all the stages of work on the monograph is gratefully acknowledged. I wish to express my

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Irkutsk, March 1992

Vladimir S. Stepanov

Nomenclature

A	work, J
ΔA	work losses, J
A	ash content in fuel
a	fuel cost, currency /kg c.e. (coal equivalent)
B, b	anergy (total and specific), J
C	specific heat capacity, J/kg · K
C, c	annual costs, currency/year; currency/year · unit of process product
D	damage, monetary
d	number of considered technological schemes
E, e	exergy (total and specific), J, kW h; J/kg, J/mol, kW h/ton
EF	economic effect, currency/year
F	Helmholtz free energy, J
F	Faraday constant, k Coulomb/mol
G	Gibbs free energy, J
ΔG_{x}^{0}	standard Gibbs energy of formation of substance z , J
ΔG_{z}^{0} $\Delta G_{\mathrm{ion}}^{0}$ ΔG_{a}^{0} ΔG_{c}^{0}	standard Gibbs energy of ion formation in aqueous solution, J
ΔG_a^0	standard Gibbs energy of anion formation, J
$arDelta G_{ m c}^{ar{0}}$	standard Gibbs energy of cation formation, J
$(\Delta G_{ m s})_z$	change of Gibbs energy in formation of an infinitely dilute solution
	of substance z in water, J
$(\Delta G_z^0)_{\rm aq}$	standard Gibbs energy of forming substance z in aqueous solution, J
g	tons of consumption of raw material, per ton of process end product
H	enthalpy (total or specific), J; J/kg, J/mol
ΔH_z^0	standard heat of formation of substance z, J
$\Delta H_{ m ion}^{ ilde{0}} \ \Delta H_{ extbf{a}}^{0}$	standard enthalpy of ion formation in aqueous solution, J
ΔH_a^0	standard enthalpy of anion formation, J
$\Delta H_{ m c}^{0}$	standard enthalpy of cation formation, J
$(\Delta H_{\rm s})_z$	enthalpy change in formation of infinitely dilute solution
	of substance z in water, J
$(\Delta H_z^0)_{ m aq}$	standard heat of formation of substance z in aqueous solution, J
ΔH_{com}^0	heat of combustion, kJ/kg
I, i	energy (total and specific), J, kW h; J/kg, J/mol, kW h/ton
K, k	monetary capital investment
L	heat output, kW

XII Nomenclature

input and output material flows, ton Mmass of elements, anions, cations mnumber of considered energy carriers melectric capacity, kW N number of process links in a technological scheme N amount of process product n number of conisdered technologies in one link of technological chain n number of electrons in a reaction $n_{\rm e}$ oxygen content in fuel 0 energy conserved potential, J, kWh P pressure, Pa pheat, J, kWh Q heat losses, J/kg, J/mol, kW h/t ΔQ high calorific value, kJ/kg $Q_{\rm h}$ low calorific value, kJ/kg Q_1 heat amount per unit of substance, J/kg, J/mol, kW h/ton qspecific heat consumption in electricity production, g c.e./kW h qenergy conserved, J, kWh Rnumber of processes in a production scheme rentropy (total and specific), J/K; J/kg · K, J/mol · K S, sentropy change, J/K ΔS temperature in Kelvin, K Ttemperature of environment, K T_0 temperature on a Celsius scale, °C t time, h, y t internal energy, J Uvolume (total and specific), m3; m3/kg, m3/mol V, vindustrial pollutants (total and specific), m³; m³/ton of process product, V, vor ton pollutants per ton of process product fuel moisture Welectricity production, kWh $W_{\mathbf{w}}$ number of seasons in year wcosts (total and specific), currency/year; currency/year per unit Z, zof process product conversion factor of different energy carriers into common units α of energy, g c.e./kWh, kg c.e./GJ fraction of technology in product output specific fuel consumption, B g c.e./kW h, kg c.e./GJ coefficient of useful product extraction in a process Y content of useful component in raw and auxiliary materials 8 coefficient of cost elements ε interest of capital ε_{s} fraction of chemical compound (element) per unit of considered substance V $\varphi_{\text{ion}}^{\phi}$ standard electrode potential, V

Subscripts

a anion
aq aqueous
ave average
c cation

cc production of cogeneration plant by condensing mode

ch chemical cooling system

ck coke cl coal compl complex

con concentrate, concentration

cons consumed

cp cogeneration plant

ct production of cogeneration plant by thermal mode

e electron

ec existing condensation power plants

el electric energy

en energy
endo endothermic
enw electric network
es electrical smelting

ex exergy exo exothermic f fuel

f furnace facility

h high

hnw heat network

i additional reference speciesi original substance of the process

ib industrial boiler

id ideal

if intersystem power flow

 $\begin{array}{ccc} \text{ion} & \text{ion} \\ \text{ir} & \text{iron} \\ j & \text{element} \\ j & \text{process} \end{array}$

k final substance of the processk resulting reference species

low

l product from the process

los loss

m mechanical

XIV Nomenclature

mat material ml melting n nominal

nc new condensation power plants

oc oxygen converter oh open-hearth

or ore

p heat capacity at constant pressure

pproductptechnologypbpeak boilersprpreviousqthermalrraw materialresresulting

r heat recovery installation
s infinitely dilute solution

sm smelting, smelted st structural change

stb stand-by

str steel as rolled stock t technological

tot total
us useful
w waste
z substance

Superscripts

abs absolute add additional b base

ce coal extraction

ck coke

con concentration

cs cast

d discharge (industrial discharge)

ext extraction fut future

g gases (waste gases)

id ideal

met metallurgical opt optimal

or ore pel pellets production pr quenching qn real real relative rel rolling rol rolled stock rs SC scrap steel st steel as rolled stock str

Abbreviations

CCM continuous casting machine ESS energy supply system

SER secondary energy resources

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Introduction

Chapter 1 briefly describes the concepts and laws of thermodynamics that form the basis for the exergy method. It also considers in detail the technique for drawing and analyzing the complete energy balance of a process, methods for computing the chemical energy and exergy of substances which have been developed with the participation of the author and differ from those proposed by other researchers (Chaps. 2 and 3).

Chapter 4 presents the method of complex analysis of processes and plants which includes both the thermodynamic and techno-economic analysis on the example of utilizing thermal secondary energy resources. Such an analysis allows the determination of both the amounts of secondary energy resources which are theoretically and technically applicable for the utilization and the degree of their economically optimal use.

Despite the fact that the fundamentals of the exergy method of analysis have largely been elaborated, this method has not yet found broad practical application. Therefore, the author has tried to show the practical value of this method, its simplicity and the results that can be obtained.

Chapters 5 and 6 give examples of drawing up the complete energy balance of individual technological processes and complexes of ferrous and non-ferrous metallurgy, determining their efficiency, analyzing their losses with identification of irrevocable losses and those that are theoretically recoverable.

In Chaps. 7 and 8 we estimate the energy reserves of industries (comprised of technological processes) using the usual methodological principles based on the concept that energy conservation in an industry results from more efficient energy use in its individual technological processes, as demanded by the final products.

Thus, the contents of the book can be divided into three sections. The first includes Chaps. 1–4 and can be titled "The theoretical bases for the analysis of energy use in technological processes". The second section (Chaps. 5, 6) is devoted to the application of the developed methods for the analysis of metallurgical processes and technological schemes. The third part (Chaps. 7, 8) illustrates the application of these methods for solving larger problems, such as estimation of energy reserves in industries, forecasting the structure, i.e., the types of fuels used and amounts of future energy consumption.

1. The Technological Process as a Subject of Thermodynamic Analysis

All processes proceeding in nature and technical facilities transform some given form of energy into another. Therefore, material changes that underlie any technological process should be considered as the consequences of the energy transformations.

In assessing the thermodynamics of a process, the capability of different processes to selectively utilize energy inputs is evaluated. Only energy of the required kind is consumed while other energy forms are rejected. Because this selectivity is a function of the physical and chemical parameters of a system, to optimize a technological production process the interrelation between material and energy changes, the laws of energy transformation must be understood.

Thus, in the analysis of technological processes it is required to study material transformations and first of all, the processes causing them and the laws of energy transformations. The goal of thermodynamics to devise methods for such studies [13, 28, 38, 67, 69, 87, 89–92, 199, 202].

1.1 Thermodynamic Systems and Processes

A thermodynamic system is a set of material bodies and fields interacting with each other and with the environment. The choice of the system is purely arbitrary and depends only on the objectives of the experiment. Thermodynamic phenomena can be considered to be macrophysical, independent of the underlying microphysical processes if the dimensions of the studied bodies are large in comparison to the size of elementary particles and the distances between them.

Thermodynamic systems are characterized by the so-called state parameters that are divided into *intensive* and *extensive* (additive). Intensive parameters (such as pressure and temperature) do not depend on the amount of a substance in the system, whereas extensive or additive ones (e.g. volume, heat capacity) are proportional to the system mass.

Interactions between a system and the environment are taken into account only in so far as they are connected with the energy and substance exchange of interest. If there is no energy and substance exchange, the system is called *isolated*. If they interact only due to energy exchange, the system is called *closed*. If interaction between them is represented by both energy and substance exchanges,