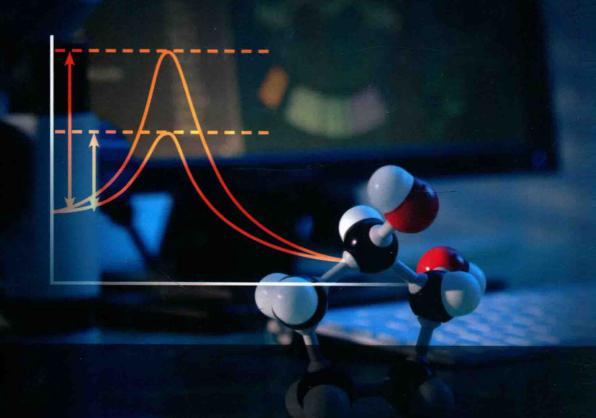
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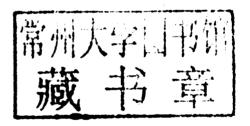


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Preface

You shall bring forth your work as a mother brings forth her child: out of the blood of your heart. Each act of creation shall leave you humble, for it is never as great as your dream and always inferior to that most marvelous dream which is Nature.

"Decalogue of the Artist," Gabriela Mistral, Chilean Nobel Laureate

This book is primarily intended for chemical and biochemical engineering students, but also for biochemists, chemists, and biologists dealing with biocatalytic processes. It was purposely written in a format that resembles the Schaum's textbooks of my long gone college years. An abridged coverage of the subject is provided in each chapter, followed by a number of sample exercises in the form of solved problems illustrating resolution procedures and the main concepts underlying them, along with supplementary problems for the reader to solve, provided with the corresponding answers. Learning through problem solving is designed to be both challenging and exciting to students. There is no book on enzyme biocatalysis with this format and purpose, so we sincerely hope to have made a contribution to the toolbox of graduate and undergraduate students in applied biology, chemical, and biochemical engineering with formal training in college-level mathematics, organic chemistry, biochemistry, thermodynamics, and chemical reaction kinetics. The book pretends to be a complement of a previous book, *Enzyme Biocatalysis* (Springer, 2008), which I had the privilege and pleasure to edit.

Chapter 1 is an introduction, giving an updated vision of enzyme biocatalysis, its present status, and its potential development. Chapters 2 and 3 refer to enzyme kinetics in homogeneous and heterogeneous systems, respectively, considering both fundamental and practical aspects of the subject. Chapter 4 is devoted to enzyme reactor design and operation under ideal conditions, while Chapters 5 and 6 deal with the main causes of nonideal behavior (mass-transfer limitations and enzyme inactivation, respectively). Chapter 7 presents an overview of the optimization of enzyme reactor operation and different tools for optimization. The book is complemented by two documents. Appendix A refers to mathematical methods for those readers not sufficiently acquainted with the subject, while Epsilon Software Information presents a software program (epsilon) for solving and representing enzyme reactor performance under different scenarios.

Writing is certainly a most exciting endeavor. Undoubtedly, writing about enzymes is beyond being the subject of our expertise, because enzymes are the catalysts of life, so writing about enzymes lies in the boundaries of writing about life. And life, as the Iraqi poet Abdul Wahab said, is about standing straight, never bent or bow, about remaining glad, never sad or low. We hope our readers will keep straight and glad while getting a little more acquainted with these catalysts of life.

A book is a journey from expectation to consolidation, an act of love from conception to birth. It has been a most rewarding experience to travel and conceive in the company of my

co-authors, two brilliant young colleagues of mine, Dr. Carlos Vera and Dr. Lorena Wilson, who were formerly my students and now fly well over my shoulders. My gratitude also to my colleague Dr. Raúl Conejeros, who authored Chapter 7 and beyond that contributed to spice this book throughout with mathematical modeling and elaborated thinking. Do not blame him too much; he is a good mix of wisdom and kindness. Our gratitude also to Dr. Felipe Scott for developing, together with Dr. Carlos Vera, the software Epsilon, presented in Epsilon Software Information to the development of the Epsilon Software.

A significant part of this book was written in Spain, at the Chemical Engineering Department of the Universitat Autònoma de Barcelona, where I was (again) warmly hosted while undertaking a sabbatical (my third one there) during the second semester of 2012. My personal gratitude to my colleagues there, Dr. Josep López and Gregorio Álvaro, who made me feel at home and who shared the ecstasy and the agony of this pregnancy.

My gratitude to the people at my institution, the Pontificia Universidad Católica de Valparaíso, who supported and encouraged this project, particularly to the rector, Professor Claudio Elórtegui, and the Director of my School of Biochemical Engineering, Dr. Paola Poirrier. Special thanks to Dr. Atilio Bustos, Head of the Library System, for his enthusiastic support and advice. My deepest appreciation also to the people at Wiley: Rebecca Stubbs and Sarah Tilley, and Shikha Pahuja at Thomson Digital, who were always helpful, warm, and supportive.

Last but not least, my gratitude to my life partner Dr. Fanny Guzmán, expert in peptide synthesis, loving care, and savoir-vivre.

Engineering is about products and processes. A book is both. We hope you will enjoy the product as much as we have enjoyed the process.

> Andrés Illanes Valparaíso, July 2013

Nomenclature

Symbol	Description	Dimensions	Chapter No.
A			
a	molar concentration of substrate A	$[ML^{-3}]$	2, 4
a	cube edge; major axis of oblate ellipsoid	[L]	3
a	constant.		Appendix A
A	surface area of catalyst particle	$[L^2]$	3
A	sectional area of reactor	$[L^2]$	5, 7
A	specific activity ratio of intermediate to initial enzyme species		6
A'	specific activity ratio of final (partly active) to initial enzyme species		6
A_S	surface area of catalyst	$[L^2]$	3
a_i	initial molar concentration of substrate A	$[ML^{-3}]$	4, 6
a_{sp}	catalyst-specific activity	$[IUM^{-1}]$	3, 4, 5, 6, 7
В			
b	molar concentration of substrate B	$[ML^{-3}]$	2, 4
b	minor axis of oblate ellipsoid		3
В	vector of parameter		7, Appendix A
\mathbf{B}^*	optimum vector parameter		Appendix A
b_0, b_i, b_{ii}	zero-, first-, and second-order		7
	parameters for the surface-of- response model		
B_1^*, B_2^*	vectors of first- and second-order		7
	regression coefficients of the surface-of-response model		
b_i	initial molar concentration of substrate B	$[ML^{-3}]$	4, 6
b_i	parameter i		Appendix A
Bi	Biot number		3, 5
b_{ij}	second-order interaction parameters for the surface-of-response model		7
C			
c	molar concentration of enzyme-	$[ML^{-3}]$	2
C	substrate complex (ES)		1 5 Am
C	constant	rMr -31	4, 5, Appendix A
[C]	concentration of analyte C	$[ML^{-3}]$	2, 3, 4, 5, 6, 7, Appendix A

Symbol CA _i ce ce'	Description annual cost of item i coenzyme concentration modified coenzyme concentration	Dimensions [USD] [ML ⁻³] [ML ⁻³]	Chapter No. 7 2 2
D d	molar concentration of enzyme-inhibitor complex (EI)	$[ML^{-3}]$	2
D	differential operator	Age to	Appendix A
D_0	diffusion coefficient in water	$[L^2T^{-1}]$	3
$D_{\rm eff}$	effective diffusion coefficient	$[L^2T^{-1}]$	3, 5, 6, 7
d_P	diameter of catalyst spherical particle	[L]	3, 6
_			
E e	concentration of active enzyme	$[IUL^{-3}]$	2, 4, 5, 6, 7, Appendix A
Е	enzyme activity	[IU]	4, 5, 6
E	relative error or enzyme species	[.0]	Appendix A
e_0	initial concentration of active enzyme	$[IUL^{-3}]$	2, 6, 7
E_0	initial enzyme activity	[IU]	6
E_a	energy of activation in Arrhenius	$[ML^2T^{-2}]$	2, 5, 7
∠ a	equation		2, 3, 7
$E_{\mathbf{C}}$	contacted enzyme activity	[IU]	3
ees	enantiomeric excess of the S-enantiomer	1	3
E _I	immobilized enzyme activity	[IU]	3
E_{ia}	energy of activation of inactivation in Arrhenius equation	$[ML^2T^{-2}]$	2, 3, 7
$E_{ia,\;M}$	energy of activation of inactivation in Arrhenius equation in the presence of a modulator	$[ML^2T^{-2}]$	7
E_L	enzyme activity lost by immobilization	[IU]	3
em	molar concentration of enzyme— modulator M complex	$[ML^{-3}]$	6
E_R	enzyme activity remaining in solution after immobilization	[UI]	3
E(t)	enzyme activity over time	[IU]	6
F			
f	molar concentration of enzyme– inhibitor–substrate complex (EIS)	$[ML^{-3}]$	2
f	size distribution frequency		3
f	number of factors assessed by the		7
•	surface-of-response methodology		<i>F</i>
F	ratio of V_{max} to V'_{max}		2
F	reactor feed flow rate	$[L^3T^{-1}]$	4, 5, 6, 7
F_0	initial reactor feed flow rate	$[L^3T^{-1}]$	6

Symbol F ₀	Description Fisher-Snedecor distribution for a null	Dimensions	Chapter No. 7
f(x) F(x) f(x,y)	hypothesis function of vector x vector of functions of x implicit function of vector x and		Appendix A Appendix A Appendix A
$F_{\alpha,g,h}$	dependent variable y Fisher–Snedecor distribution for a confidence level of $1-\alpha$ with g degrees of freedom in the numerator and h degrees of freedom in the denominator		7
Н			
h	film volumetric mass-transfer coefficient for substrate	$[L^3T^{-1}]$	3, 6
h	packed-bed reactor length	[L]	7
h	integration step size		3,5, Appendix A
H	total reactor length	[L]	7
h'	film linear mass-transfer coefficient for substrate	[LT ⁻¹]	3, 5
\mathbf{h}^{+}	proton (molar) concentration	$[ML^{-3}]$	2, 3
h_0^+	proton (molar) concentration in the bulk medium	$[ML^{-3}]$	3
h_P	film volumetric mass transfer coefficient for product	$[L^3T^{-1}]$	Epsilon Software Information
I			
i	inhibitor molar concentration	$[ML^{-3}]$	2
J J J	Jacobian matrix substrate flow rate objective function	[MT ⁻¹]	Appendix A 3 7
K			
k	catalytic rate constant		2, 4, 5, 6, 7, Appendix A
K	equilibrium constant of dissociation of enzyme–substrate complex into enzyme and substrate	$[ML^{-3}]$	2
k_0	pre-exponential term in Arrhenius equation		2, 7
k_{B}	Boltzmann universal constant		3
k_{D}	first-order inactivation rate constant	$[T^{-1}]$	2, 3, 6, Appendix A

Symbol	Description	Dimensions	Chapter No.
K_D	dissociation constant of enzyme– substrate complex into enzyme and substrate	$[ML^{-3}]$	2
$k_{D,0}$	pre-exponential term in Arrhenius equation	$[\mathbf{T}^{-1}]$	2, 7
k_{D1}	first-order inactivation rate constant in first stage of inactivation	$[\mathbf{T}^{-1}]$	6
k_{D2}	first-order inactivation rate constant in second stage of inactivation	$[\mathbf{T}^{-1}]$	6
$k_{D,M}$	first-order inactivation rate constant of enzyme–modulator M complex	$[T^{-1}]$	6
$k_{D,M,0}$	pre-exponential term in Arrhenius equation in the presence of modulator M	$[\mathbf{T}^{-1}]$	7
K_{eq}	equilibrium constant		2
k _i	Runge-Kutta method coefficients		Appendix A
K_{I}	inhibition constant	$[ML^{-3}]$	3, 4
K_{IC}	dissociation constant of enzyme– competitive inhibitor complex	$[ML^{-3}]$	2, 6, 7
K _{INC}	dissociation constant of enzyme– noncompetitive inhibitor complex	$[ML^{-3}]$	2, 4, 6
K' _{INC}	dissociation constant of enzyme– substrate–noncompetitive inhibitor tertiary complex	$[ML^{-3}]$	2, 4
K_{M}	Michaelis-Menten constant	$[ML^{-3}]$	2, 3, 4, 5, 6, 7, Appendix A
K_{MA}	dissociation constant of secondary complex EA into E and A	$[ML^{-3}]$	2, 6
K'_{MA}	dissociation constant of tertiary complex EAB into EB and A	$[ML^{-3}]$	2
K_{MAP}	apparent Michaelis-Menten constant	$[ML^{-3}]$	2, 3
K_{MB}	dissociation constant of secondary complex EB into E and B	$[ML^{-3}]$	2
K'_{MB}	dissociation constant of tertiary complex EAB into EA and B	$[ML^{-3}]$	2, 6
$K_{M,P}$	dissociation constant of EP into E and P (reversible reaction)	$[ML^{-3}]$	2
$K_{M,S}$	dissociation constant of ES into E and S (reversible reaction)	$[ML^{-3}]$	2
K_{P}	electrostatic partition coefficient at the matrix-medium interface		3
K_P	inhibition constant by product		4, Epsilon Software Information

$\begin{aligned} & \textbf{Symbol} \\ & K_S \\ & K_{p,S} \\ & K_{p,h^+} \end{aligned}$	Description dissociation constant of the inactive tertiary complex ESS into ES and S partition coefficient for substrate partition coefficient for protons	Dimensions	Chapter No. 2, 3, 4, 5, 6, 7, Appendix A 3 3
$egin{array}{c} L \\ L \\ L \\ L_{\mathrm{eq}} \\ L_{R} \end{array}$	optical path in spectrophotometer cell catalytic slab width equivalent catalyst particle length packed-bed reactor length	[L] [L] [L]	2 3, 5, 7 3, 7 5
$\begin{aligned} & \mathbf{M} \\ & \mathbf{m_{cat}} \\ & \mathbf{M_{cat}} \\ & \mathbf{m_i} \\ & \mathbf{MW} \end{aligned}$	concentration of biocatalyst mass of immobilized enzyme catalyst characteristic equation root molecular weight	[ML ⁻³] [M]	4, 5, 6 3, 4, 5, 6, 7 Appendix A
N n	stoichiometric coefficient of product with respect to substrate		4
$egin{array}{c} n \\ N \\ N_1 \end{array}$	number of observations number of sections lumped modulation factor in first stage		7, Appendix A Appendix A
n_{1P}	of enzyme inactivation modulation factor by product in first stage of inactivation		6
n_{1S}	modulation factor by substrate in first stage of inactivation		6
N_2	lumped modulation factor in second stage of enzyme inactivation		6
n _{2P}	modulation factor by product in second stage of inactivation		6
n_{2S}	modulation factor by substrate in second stage of inactivation		6
$\begin{array}{c} n_{M} \\ N_{R} \\ N_{t1/2} \end{array}$	modulation factor by modulator M number of staggered reactors number of half-lives of catalyst use		6, 7 6 6
O OD	optical density		2
P p	product molar concentration number of parameters	$[ML^{-3}]$	2, 3, 4, 7 7, Appendix A

Symbol p ₀	Description molar concentration of product in the	Dimensions [ML ⁻³]	Chapter No.
n	bulk reaction medium	DAT	2
P_{C} P_{I}	contacted protein	[M]	3
P_R	immobilized protein protein remaining in solution after	[M] [M]	3
rR	immobilization		
ps	molar concentration of product at the biocatalyst surface	$[ML^{-3}]$	3
p_{sp}	specific protein load		3
Q			
q	coupled analyte concentration	$[ML^{-3}]$	2
q	number of regression variables		7
R			
r	variable radius of spherical particle	[L]	3
R	ideal gas constant	$[ML^2T^{-2}\theta^{-1}]$	2, 3, 7
r'	rate of transformation of substrate into product		3
\mathbb{R}^2	coefficient of determination		Appendix A
	agitation rate	$[T^{-1}]$	3
$r_a R_{adj}^2$	adjusted coefficient of determination		Appendix A
R_F^{adj}	allowable flow-rate fluctuation as a		6
	result of downstream operations		
R_P	radius of catalyst spherical particle	[L]	3, 5
S			
S	substrate concentration within the catalyst	$[ML^{-3}]$	2, 3, 4, 5, 7,
s_0	molar concentration of substrate in the	$[ML^{-3}]$	Appendix A
30	bulk reaction medium		
s_{0i}	molar initial (or inlet) substrate concentration in the bulk reaction medium	$[ML^{-3}]$	5
s^2	residual mean square for n – p degrees		Appendix A
	of freedom		
S(B)	sum of square error	2	Appendix A
s_i	initial (or inlet) substrate molar concentration	$[ML^{-3}]$	2, 4, 6, 7
s_S	molar concentration of substrate at the biocatalyst surface	$[ML^{-3}]$	3, 7
SS_E	sum of squares due to residuals (error)		7
SS_R	sum of squares due to regression (model)		7
- S = IV	1 (model)		*

$\begin{array}{c} \textbf{Symbol} \\ \textbf{SS}_{R\ k/,p-k} \end{array}$	Description regression sum of squares for k variables, given that p minus k variables are already in the model	Dimensions	Chapter No. 7
$SS_{R,p-k}$	regression sum of squares for the reduced model containing p minus k variables		7
T			
t	time	[T]	2, 3, 4, 5, 6, 7,
			Appendix A
T	absolute temperature	$[\theta]$	2, 3, 7
t_0	initial time	[T]	7
t _{1/2}	half-life of enzyme catalyst	[T]	2, 6
t_C	total time of one cycle of reactor operation	[T]	6
t_{dless}	dimensionless time of reactor operation		4
t_f	final time	[T]	7
T_{lo}	temperature lower bound	$[\theta]$	7
$t(n-p, \alpha/2)$	upper $\alpha/2$ quantile of Student's		7, Appendix A
•	t-distribution for n – p degrees of freedom		
t _s	reactor staggering time	[T]	6
T_{up}	temperature upper bound	[θ]	7
ч			
U			
u	control variable		7
u_{lo}	control variable lower bound		7
u _{up}	control variable upper bound		7
V			
v	initial reaction rate	$[ML^{-3}T^{-1}]$	2, 4, 5, 6,
¥	initial reaction rate		Appendix A
v	model parameter vector or vector whose elements are different from zero		7
V	reactor volume	$[L^3]$	7
v'	enzymatic reaction rate	$[MT^{-1}]$	3
v"	reaction rate per unit volume of catalyst	$[ML^{-3}T^{-1}]$	3
V_{bed}	bed volume of packed-bed reactor	[L ³]	4, 5
$V(b_i)$	variance of the parameter b _i	[2]	Appendix A
$V(O_1)$	variance of the parameter b_1 variance–covariance matrix of B		Appendix A
$V_{\rm eff}$	effective volume of reaction	$[L^3]$	4, 5, 6, 7
	effective reaction rate	$[ML^{-3}T^{-1}]$	5
V _{effective}	maximum reaction rate	$[ML^{-3}T^{-1}]$	2, 4, Appendix A
V_{max}		$[ML^{-3}T^{-1}]$	2, 4, Appendix A
V_{maxAP}	maximum apparent reaction rate of	[MIL I]	△.
	product formation		

Symbol V _{maxAP0}	Description pre-exponential term in Arrhenius	Dimensions [ML ⁻³ T ⁻¹]	Chapter No. 2
$V_{max,P}$	equation maximum reaction rate of product to	$[ML^{-3}T^{-1}]$	2
	substrate conversion (reversible reaction)	2 .	
$V_{max,S}$	maximum reaction rate of substrate to product conversion (reversible reaction)	$[ML^{-3}T^{-1}]$	2
V_{max}^{\prime}	maximum reaction rate of product formation from enzyme-substrate-	$[ML^{-3}T^{-1}]$	2
V'_{max}	inhibitor tertiary complex maximum reaction rate	$[MT^{-1}]$	3, Epsilon
* max	maximum reaction rate	[WII]	Software Information
$V_{\text{max}}^{\prime\prime}$	maximum reaction rate per unit volume of catalyst	$[ML^{-3}T^{-1}]$	3, 7
V_{proc}	total processed volume	$[L^3]$	6
V_R	reaction volume	$[L^3]$	5
v_s	solute molar volume	$[L^3M^{-1}]$	3
X			
X	variable width of catalytic slab	[L]	3
x	state variables		7
X	vector of independent variables		Appendix A
X	limiting substrate to product conversion		3, 4, 5, 6
X	matrix of independent variables		7, Appendix A
X_0	initial (steady-state) conversion of limiting substrate into product		6
x_c	coded variables		7
x_g	vector of values for the model variables $(p \times 1)$		7
x_h	highest value for uncoded input variable		7
$\mathbf{x_i}$	input variable i	rod	7
$\mathbf{x_l}$	lowest value for uncoded input variable		7
Y			
y	dependent variable		Appendix A
Y	vector of observed values		7, Appendix A
ŷ	predicted response by the model		7
\bar{Y}	average of the observed values		7, Appendix A
Y_E	enzyme immobilization yield		3
y_i	output variable i		7
\mathbf{y}_{i}	ith observation for the dependent		Appendix A
	variable		

Symbol \hat{y}_i	Description predicted response for the ith	Dimensions	Chapter No. 7
Y_P	observation protein immobilization yield		3
Z			
Z	dimensionless variable width of catalytic slab		3, 7, Appendix A
Z	valence of ionic species		3
Greek Lette	rs		
α	ratio of rate constant of formation of B from E'B and transition rate from EA to E' + B (ping-pong mechanism)		2, 4
α	Damkoehler number		3, 5, 6
α	significance level		7, Appendix A
α_S	Damkoehler number for substrate		Epsilon Software Information
α_P	Damkoehler number for product		Epsilon Software Information
β	dimensionless substrate concentration		3, 7, Appendix A
β_0	dimensionless substrate concentration in the bulk reaction medium		3, 5, Appendix A
β_{0i}	initial (or inlet) dimensionless substrate concentration		5
β_c	dimensionless substrate concentration within the catalyst at the center of the slab		7
β_{i}	initial (or inlet) dimensionless substrate concentration		6
β_S	dimensionless substrate concentration at the biocatalyst surface		3, 5
γ	dimensionless product concentration $(p \cdot K_P^{-1})$		3
γ_0	dimensionless product concentration in bulk reaction medium ($p_0 \cdot K_P^{-1}$)		3, 5
γoi	initial (or inlet) dimensionless product concentration		5
$\gamma_{\rm S}$	dimensionless product concentration at the biocatalyst surface $(p_S \cdot K_P^{-1})$		3
δ	stagnant liquid film width	[L]	3
$rac{\delta}{\Delta extsf{H}^0}$	relative error tolerance standard enthalpy change of dissociation	[MI ² T ^{−2} 1	Appendix A 2
Δ11	of ES into E and S	[ML I]	2

$\begin{array}{l} \textbf{Symbol} \\ \Delta H_{\rm I}^0 \end{array}$	Description standard enthalpy change of dissociation	Dimensions [ML ² T ⁻²]	Chapter No. 2
ΔS^0	of EI into E and I or EIS into ES and I standard entropy change of dissociation	$[ML^2T^{-2}\theta^{-1}]$	2
A G0	of ES into E and S	n m 2m-2n-1	2
$\Delta S_{ m I}^0$	standard entropy change of dissociation of EI into E and I, or EIS into ES and I	$[ML^2T^{-2}\theta^{-1}]$	2
3	error		3
3	molar extinction coefficient		2
3	porosity of the catalyst matrix		3
3	void fraction of catalyst bed		4, 5, 7
3	error vector		7, Appendix A
E	enantioselectivity		3
ϵ_{i}	error for the ith observation		Appendix A
ζ	tortuosity of the catalyst matrix pores		3
η	local (or surface) effectiveness factor		3, 5
$\eta_{ m G}$	global (mean integral value)		3, 5, 6, 7
	effectiveness factor in the catalyst particle		
$\eta_{ m P}$	global effectiveness factor under product inhibition		3
K	ratio of Michaelis to uncompetitive inhibition constants $(K_M \times K_S^{-1})$		3
λ	optical wavelength	L	2
λ	dimensionless reactor bed length		5
μ	viscosity of the solution	$[ML^{-1}T^{-1}]$	3
ν	dimensionless reaction rate $(v \times V_{max}^{-1})$		3, 5, 6
π	volumetric productivity of reactor operation	$[ML^{-3}T^{-1}]$	4
π_{sp}	specific productivity of reactor operation	$[T^{-1}]$	4
ρ	dimensionless radius of the spherical catalyst particle		3, 5, Appendix A
$ ho_{ m app}$	apparent density of catalyst	$[ML^{-3}]$	4, 5, 6, 7
$\sigma_{\rm i}$	standard deviation of b _i	•	Appendix A
τ	fluid residence time in the reactor	[T]	4, 5
$\varphi(t)$	enzyme decay function		6
Φ	Thièle modulus for substrate		3, 5, 6, Appendix A
$\Phi_{ m P}$	Thièle modulus for product		3
$\Phi^{ m R}$	Thièle modulus for R enantiomer		3
Φ^{S}	Thièle modulus for S enantiomer		3
Ψ	electrostatic potential of the support	$[ML^{2}T^{-2}Q^{-1}]$	3
Othor			
Other ∈	electron charge		3

Epsilon Software Information

Available alongside this book is a copy of the software epsilon which allows the simulation of the operation of enzymatic reactors. epsilon has been designed to illustrate the main topics included in this book, offering an additional tool to improve the understanding of the design and operation of enzymatic reactors (specifically Chapters 4 to 6). Guidelines for software installation are given below:

i. Program Installing

Two situations may occur during installation:

- *Matlab*[®] is already installed in user's computer

 The program was built using Matlab[®]'s compiler toolbox. Hence, if Matlab[®] is installed in the user's computer, open the distrib folder and run the file Epsilon_32. exe or Epsilon_64.ex, depending on the system's architecture.
- Matlab[®] is not installed in user's computer
 First, open the Matlab[®] package (Epsilon_64_pkg or Epsilon_32_pkg, depending on the system's architecture). Two files will be created in the current directory. Second, open MCRInstaller.exe and follow the installer instructions. Once the installation is complete, open the newly created Epsilon_64.exe or Epsilon_32.exe.

ii. Program Description

This software was designed with a simple interface, with the purpose of allowing the comparison of reactor behavior under different scenarios (reaction kinetics and operation modes). The program considers reactor performance for biocatalysts having the most common enzyme kinetics (Michaelis-Menten, competitive and non-competitive inhibition by product and uncompetitive inhibition by substrate) and operating in usual reactor configurations (BSTR, CPBR and CSTR). The program also allows incorporating the effect of external diffusional restrictions (EDR) or catalyst inactivation during reactor operation. Figure 1 shows the interface of epsilon.