The World Biotech Report 1985

Volume 1: Europe

The World Biotech Report 1985 Volume 1: Europe

Proceedings of Biotech '85 Europe, Geneva, May 1985

Contents

ORIGINAL PAGE IS OF POOR QUALITY

Healthcare product development

1 The science & the commerce

Human growth hormone: microbial Tony Atkinson et al 1 expression & purification CAMR UK New developments in recombinant DNA Philippe Kourilsky 9 technology for prokaryotic & eukaryotic Institut Pasteur France systems Tissue culture systems for the Menachem Rubinstein 13 development of healthcare products Weizmann Institute of Science Israel Monoclonal antibodies: their impact on Thomas Clark 23 the European clinical reagent market European Business Associates Luxembourg Modern marketing of innovative Peter McCulloch 37 Porton Products diagnostic systems

2 Opportunities for genetic technologies

Rejuvenating engineering	antibiotics with genetic	Julian Davies Biogen SA	et al	47
		Switzerland		

UK

55

New developments in animal vaccine	Fred Brown
technology	Wellcome Biotechnology
	UK

Immunotherapy through lymphokines: a new approach	A Arthur Gottlieb Imreg USA	65
Strategies in ageing research	Robin Holliday National Institute for Medical Research UK	75
•	•	
Pharmaceutical production		
1 Growth & first stage processing		
The use of plate heat exchangers in large-scale animal cell culture	John Carvell et al APV International UK	83
Pilot & production scale microcarrier cultivation of mammalian cells on Cytodex	Per Vretblad et al BioCell Laboratories Sweden	97
Optimal design & operation of fermentation systems for rDNA products	Andrew Pickett Porton International UK	107
Quantitative evaluation of pilot plant unit operations for primary separation of bacterial broths	Björn Lindman Alfa-Laval Sweden	119
Solubilisation & activation of eukaryotic protein products produced as inclusion bodies in E.coli	Peter Lowe Celltech UK	127
2 Downstream processing		
Affinity chromatography as a production technique	M Vijayalakshmi,D Thomas University of Technology of Compiegne	131
the state of the s	France Samuel	
Ion exchange as a production technique for proteins	Georges Cueille et al Rhône-Poulenc Recherches France	141

Genetic design for processing: strategies	Roger Sherwood et al CAMR	161
Genetic design for downstream processing: immunoaffinity systems	Mathias Uhlén et al European Molecular Laboratory FRG	171
3 Process integration & control		
Biosensors for process monitoring & control	Anthony Turner Cranfield Institute of Technology UK	181
Automation of chromatographic processes	Hans Johansson Pharmacia AB Sweden	193
Integrated process control for product development & production	Leslie Spark CAMR UK	203
4 Regulatory standards	en de la companya de La companya de la co	
The control of the bio'ogical medicinal products of biotechnology	Elwyn Griffiths National Institute for Biological Standards & Control UK	217
Assuring biological product quality	John Curling Pharmacia AB Sweden	221
	The second secon	
Food development		
Food proteins - current trends & future developments	Graham Rodger ICI Agricultural Division UK	225
Advances in starter culture technology	Charles Daly University College, Cork Ireland	239

Mycoprotein - the development & scale- up of a novel food	Robert Marsh et al RHM Research UK	253
Framework for toxicity testing & regulation of novel food proteins	Peter Blias Federal Research Centre for Nutrition FRG	263
New plant genetics		
Introduction, expression & sexual transmission of genes in plants	Robert Schilperoort et al University of Leiden The Netherlands	277
Engineering herbicide tolerance	Robert Goodman Calgene USA	293
Molecular biology & the prospects for integrated biological & environmental control	Peter Dean Agricultural Genetics Co UK	301
The new plant genetics: restructuring the global seed industry	George Kidd L William Teweles USA	311
Strategy & finance		
Raising equity finance for development projects	Christopher Bloomfield County Bank Development Capital UK	323
Venture capital for biotechnology based companies	Roger Hay Innotech UK	337
Advances in sensors		
Planar microfabrication of chemical sensor systems	Imants Lauks Integrated Ionics USA	351
The development of novel biosensors	John Albery et al Imperial College, London UK	359
·		

Government & Industry

1 Boonomics of strategic raw materials

	• • • • • • • • • • • • • • • • • • •	
The economics of strategic raw materials for biotechnology - sugar	Caroline Cormack Int'l Confederation of European Beetgrowers France	383
Industrial need for cheaper raw materials	Derek Stringer ICI UK	387
The EEC starch regime & the new bioprocess industries	Nick Young Wye College (University of London) UK	393
2 New regulations	•	
Barriers to trade in biotechnology: existing & potential	Irving Fuller USTR Office of the President USA	397
Biotechnology & environmental protection in the European Community	Goffredo del Bino CEC Belgium	407
The oil industry		
Impact of biotechnology on the oil industry	Garfield Royer Standard Oil (Indiana) USA	411
Sulphate-reducing bacteria in oil- bearing reservoirs	Barry Herbert Shell Research UK	417
Scleroglucans for enhanced oil recovery	Alain Donche Elf Aquitaine France	429

Microbial corrosion: the effect of sulphate-reducing bacteria on mild steel	John Levi et al British Petroleum UK	437
Microbial transformation of chemicals in oil reservoirs: how this knowledge can be applied	Douglas Munnecke Genencor USA	447
Advances in bioprocessing research with yeasts	D Hitzman, E Zuech Phillips Petroleum USA	459
Chemicals & Enzymes		
1 Industry - the next decade		
Industrial microbiology: enabling technologies	Gerard Fairtlough Celltech UK	467
Potential applications of biotechnology for speciality chemicals	Pierre Bost Rhône-Poulenc Santé France	469
Chemicals & enzymes industry - the next decade & beyond	William Amon Jr Cetus USA	471
2 New products & processes	194000 · 194000 · 194000 · 194000 · 194000 · 194000 · 194000 · 194000 · 194000 · 194000 · 194000 · 194000 · 19	
Microbes as producers of added value commodity chemicals	Bernard Witholt et al University of Groningen The Netherlands	477
Plants as producers of high value secondary metabolites	R Whitaker, D Evans DNA Plant Technology USA	489
Prospects for novel biomaterials . development	T Jarman, J Light PA Technology UK	505

3 Environmental pollution control

	4
Industry working with government: the role of the policymaker	Ole Münster 513 Ministry of the Environment Denmark
Biotechnology, products liability & the public interest	A Schwartz, S Bent 521 Schwartz, Jeffery, Schwaab, Mack, Blumenthal & Evans USA
Microbial degradation of cyanide	Chris Knowles 537 University of Kent UK
4 Immobilized systems	•
Cell/surface interactions: a biotechnological overview	Harold Fowler 543 University of Bath UK
Animal cells - a suitable case for immobilization?	A Rosevear, C Lambe 559 AERE Harwell UK
Immobilized microbial & plant cells: techniques & applications	Peter Brodelius 573 Federal Institute of Technology Switzerland
Preparation & application of single enzyme systems in immobilised non-living cells	Klaus-Dieter Vorlop 587 Institut für Technische Chemie Braunschweig FRG
Membrane bioreactors - trends & opportunities	Stephen Matson 597 Sepracor USA

5 Enzymes, engineering & industry

Industrial applications of enzyme engineering	Herb Heyneker et al Genencor USA	611
Stabilisation of enzymes with soluble additives	Charles Gray University of Birmingham UK	617
Thermophilic enzymes for industrial applications	Heiner Grüninger Institute of Biotechnology ETH-Zurich Switzerland	627
Building a business in biocatalysis	Olivier Midler Genencor Europe France	639

Poster presentations

Effect of immobilizing Chlorella sorokiniana on photosynthesis & excretion of organic compounds	J P Callegari et al IIF-IMC CERIA Belgium	651
Surface & electric fields effects in preparation of cell-size liposomes	D S Dimitrov, M Angelova Central Laboratory of Biophysics Bulgaria	655
Microbiological leaching of copper sulphide concentrates	S N Groudev et al Higher Institute of Mining & Geology Bulgaria	661
Production of fructose, 1,6 diphosphate by permeabilized yeast cells cross- linked with glutaraldehyde-albumin	F Melelli, G Bisso Biomedica Foscama SpA Italy	663
The use of bioactivity monitor for process optimization & scale up of Bacillus thuringiensis fermentation	E Zomer et al Unikoor Israel	665
The physiological basis of variable productivity during fermentation	J R Woodward Leeds University UK	671
Cellobiohydrolase hyperproducing fungal mutants induced by gamma radiation	Basil Macris NRC "Democritos" Greece	675
Cell dielectrophoresis, adhesion & fusion in axisymmetric electric fields	D S Dimitrov et al Central Laboratory of Biophysics Bulgaria	677
Selection of solid-liquid separation equipment for batch intracellular enzyme production	Neil Morris Teesside Polytechnic UK	683
Influence of enzyme modification on the activity & stability of enzymes: an analysis by a series-type mechanism	A Sadana, J Henley University of Mississippi USA	685
Citric acid for beverages - a new economic submerged fermentation process	O Zehentgruber et al Vogelbusch GmbH Austria	687

Power input, K_{L} a values in pneumatically agitated fermentors with extracellular microbial polysaccharides	J-B Gros, C-G Dussap Université de Clermont II France	691
Biochemical & technological characteristics of systems for ethanol production by Zymomonas mobilis	M J Beker et al Latvian Academy of Sciences USSR	693
Use of oxygen in yeast fermentation	Michael Heisel et al Linde AG PRG	695
Enzymatic synthesis of optically active amino acids	Kenji Soda et al Kyoto University Japan	699
Growth & sporulation of Penicillium roqueforti in solid, divided substrate fermentation	J-B Gros et al Université de Clermont II France	701
The use of biotechnology for the control of nitrate in potable water	T Zabel et al Water Research Centre UK	703
A host/vector system for low cost, large scale production of proteins	M Mieschendahl et al Battelle-Institut FRG	707
Monomer circular phasmid DNA molecules can be effectively packed in vitro a used as vector DNA molecules	N K Yankovsky et al Institute for Genetics & Selection of Industrial Microorganisms USSR	709
Feasibility review of preparative in vitro protein synthesis	M L Riordan Arthur D Little USA	715
Enzyme productivity in chemostat fermentations with retention of biomass	C Emborg et al Technical University Denmark	717

xvii

Fermentation monitoring using mass spectrometry	E Heinzle ETH-Zurich Switzerland	719
Formaldehyde removal in a fluidised bed biological reactor: operation & modelling	C Solà et al Universitat Autonoma de Barcelona Spain	721
Enhancement of straw pulp mill waste water treatment by biomass engineering	Francis Saunders International Biochemicals Group UK	723
Prevaporation as an alternative to entrainer-distillation for dehydration of alcohol	Peter Seewann Vogelbusch GmbH Austria	727
Removal of heavy metals from sewage sludge by bacteria	J Glynn Henry et al University of Toronto Canada	731
Separating proteins from cell lysates with cross-flow filtration	Raymond Gabler et al Millipore USA	733
A new method of oligonucleotide synthesis	B Hamill, D Picken Cruachem UK	735
Serial chromatographic process to purify monoclonal Ab from hybridoma cell culture: ion exchange on Sepharose ^R & MonoBeads TM	U-B Fredriksson et al Pharmacia Biotechnology Group Sweden	743
The immobilisation of cells on surfaces	Harold Fowler University of Bath UK	755

Human growth hormone: microbial expression & purification

Tony Atkinson, Director
Jeremy R Court & Roger F Sherwood
Microbial Technology Laboratory

George W Jack
Therapeutic Products Laboratory
CAMR
UK

Growth hormone (GH), prolactin and chorionic somatomammotropin (CS) are a family of polypeptides related by general function, immunochemistry and structure (1); this despite their specific biological activities and synthesis of the latter in the placenta and the two former hormones in the pituatory. All 3 hormones commonly possess lactogenic and growth promoting properties and have a similar size (190 to 199 amino acids dependent on specie) and protein structure. Recent rDNA work, extending previous studies, has shown the existence of multiple genes for human GH (hGH) and for human CS (hCS) has demonstrated that hCS is a variant of hGH and indicates a variable rate of evolution in this gene family.

Rat GH was the first of the growth hormone gene family to be cloned and sequenced (2), thus yielding the amino acid structure of the mature- and pre- hormone and was later expressed as a fusion protein with -lactamase in E.coli (3). Subsequently hGH was cloned (4) and expressed (5,6) in E.coli; as now also have bovine GH (7-10) and porcine GH (9).

The conditions necessary for high level expression of hGH, bGH and pGH have been thoroughly investigated. In one example (9) both bGH and pGH were constructed following similar principles to Goeddel et al (5) for the construction of hGH. In these cases a substantial N-terminal portion of the hormone gene (in contrast to the prehormone possessing a signal peptide) is made synthetically and fused in phase to the remainder of the gene, to produce an ATG initiation codon in front of the triplet codon for the first amino acid (phe in all cases). Synthetic met-hGH has thus been expressed at high Tevel (2 to 15% soluble protein) employing 2 tandem <u>lac</u> promoters in the plasmid pHGH 107 (5) or a tandem trp-lac promoter construction (11). High level expression (20 to 30% soluble protein) of met-bGH and met-pGH have been obtained employing trp promoter vehicles. Somewhat surprisingly it was shown that reduction in the usually critical distance between the Shine-Dalgarno ribosomal binding site and the ATG codon in the original pHGH 107 met-hGH construct from the latter's 11 base pairs to 7 base pairs (the natural spacing of the lac promoter) actually reduced expression of the gene by about 40%. In an entirely separate construction Schoner et al (10) showed that a met-bGH gene produced by direct fusion of the ATG codon onto the first triplet codon (for phe) of bGH yielded a system expressing poorly with either the E.coli trp or lpp promoters in a thermoinducible runaway replication vehicle. However, expression levels of up to 30% soluble cell protein could be obtained by introducing additional codons 3' to the ATG initiation codon. High level expression of met-bGH, without introducing extra codons, was obtained by converting the coding sequence to a two-cistron expression system (10) to obviate the low efficiency of mRNA secondary structures, overcome fortuitously in the Seeburg et al (9) construction by the use of synthetic and different codons in the N-terminal construction.

Growth hormones constructed to be intracellular, as above, are produced, as are many other over-expressed foreign proteins, as dense cytoplasmic inclusion bodies (12) in which many of the aggregated proteins' thiols are in the reduced rather than the oxidised form. The exception however is met-hGH which appears to be freely soluble and biologically active in the E.coli cell (13) although the formation of granules of met-hGH in some instances has been noted (12). Active, soluble and "natural" hGH can be produced in bacteria. For instance, while P.aeruginosa transformed with a

plasmid containing a gene encoding the mature form of hGH, preceded by an ATG codon, expresses met-hGH in its cytoplasm; the hGH protein of cells transformed with a plasmid containing a gene for the natural hGH precursor is transported across the inner membrane and has the N-terminal amino acid sequence of authentic mature hGH of Phe-Pro-Thr-Ile (14).

Met-hGH has been expressed at high level in E.coli and purified to homogeneity on the large scale (13). Employing a derivative of the plasmid pHGH 107 (5) in which a trp promoter was inserted after the two tandem lac promoters (11), fermentation of E.coli RV308 containing the derivative plasmid under low tryptophan fermentation conditions gives constitutive production of met-hGH. Plasmid copy number, generation time of the E.coli cell, expression of the met-hGH gene and overall yield are unaffected by replacement of tetracycline (1 to 5 mg/l) in the culture with ampicillin (20 to 40 mg/l). All large scale cultures were routinely grown in the presence of 1 mg/l tetracycline and the data from several such cultures is summarised in Table 1.

Table 1

500 | Culture Parameters of the Production of met-hGH in E.coli

Generation time of E.coli cell	50 to 70 minutes
Average 500 1 culture time	6.5 to 9.0 hours
Cell yield	20 to 30g cell paste/1
Overall yield	10 to 15 Kg cell paste
Molecules of met-hGH per cell	9x10 ⁵ to 1.5x10 ⁶
Average % soluble cell protein	8 to 15%
mg met-hGH/l culture	250-320 mg/l
Overall yield	125-160g met-hGH

Although met-hGH yields tended to decline variably at the end of log phase growth, this problem could be obviated by rapid (5 minute) cooling of the culture from 37°C to less than 10°C.

Accurate monitoring of met-hGH yields in culture required the development of a rapid reliable assay system free of the time constraints imposed by RIA or Rocket immunoelectrophoresis. A turbidometric assay was therefore developed employing sheep anti-hGH serum to precipitate authentic standard hGH or met-hGH in crude E.coli lysates in the presence of a non-jonic detergent such as Triton X-100. Monitoring the increase in A over 30 minutes at ambient temperature provided a rapid assay of hGH concentration in the range 0.1 to 16 mg/l. Data from this assay system, although consistently 20 to 30% lower than RIA or Rocket systems over the range 50 to 350 mg/l met-hGH was sufficiently rapid, sensitive and reliable to use in monitoring cultures and the initial extraction stages.

Early regulations required the killing of cells in the fermenter. In the case of met-hGH this could be accomplished, without loss or damage of this protein, by rapidly raising the pH from pH 7.0 (initial) to pH 11.5 to 12.0 with 10M NaOH. After 5 minutes exposure to this pH the count had fallen from 1.5x10 viable cells/ml to about 6 viable cells/ml. It was noticeable however that at pH values below 11 the survival of E. coli was several logs higher and that at pH 11.5 E.coli survival was dramatically enhanced if cultures had previously been controlled in growth at pH 7.0 by the automatic addition of KOH or NaOH rather than, as normally, the addition of NH3. Treatment at this pH resulted in lysis and release of met-hGH into the culture supernatent. Reduction of the pH to pH 7 to 8 caused precipitation of denatured proteins and a loss of 30 to 50% of the met-hGH which bound to the precipitated material. Lowering the pH to pH 8.5 reduced the loss but did not eliminate it and caused less precipitation of denatured protein. Complete recovery of met-hGH could be achieved by inclusion of non-ionic detergents, such as Triton X-100 or some of the Tween series, to final concentration above 0.1% in the alkaline lysis, followed by removal of denatured protein at pH 6.0 to 8.0

Met-hGH could be purified to homogeneity in a 4 step process from either a concentrated alkali whole culture lysate as above, or from pressure disrupted viable E.coli cells. Ammonium sulphate precipitation (20 to 50% satⁿ.), followed by NaCl gradient elution on DEAE-sepharose at pH 8.5, gel filtration on Sephadex G-100 or AcA 44 at pH 8.0 and hydrophobic chromatography on phenyl-sepharose accomplished the purification. In the latter step the material was loaded (4 mg met-hGH per ml bed) at pH 8.0 in lM NaCl and when unbound material had been removed met-hGH was eluted with water. The purification protocol is summarised in Table 2.