H. SCOTT FOGLER

ELEMENTS of CHEMICAL REACTION ENGINEERING

PRENTICE-HALL INTERNATIONAL SERIES in the Physical and Chemical Engineering Sciences



ELEMENTS OF CHEMICAL REACTION ENGINEERING

H. SCOTT FOGLER

Ame and Catherine Vennema Professor of Chemical Engineering The University of Michigan, Ann Arbor Library of Congress Cataloging-in-Publication Data

FOGLER, H. SCOTT.

Elements of chemical reaction engineering.

(Prentice-Hall international series in the physical and chemical engineering sciences)

Includes bibliographies and index.

1. Chemical reactors. I. Title. II. Series. TP157.F65 1986 660.2'81 85-28270 ISBN 0-13-263476-7

Manufacturing buyer: Gordon Osbourne

© 1986 by Prentice-Hall, Inc. A Division of Simon & Schuster Englewood Cliffs, New Jersey 07632

All rights reserved. No part of this book may be reproduced, in any form or by any means, without permission in writing from the publisher.

Printed in the United States of America

10 9 8 7 6 5 4 3 2 1

ISBN 0-13-563456-5 052

Prentice-Hall International (UK) Limited, London Prentice-Hall of Australia Pty. Limited, Sydney Prentice-Hall Canada Inc., Toronto Prentice-Hall Hispanoamericana, S.A., Mexico Prentice-Hall of India Private Limited, New Delhi Prentice-Hall of Japan, Inc., Tokyo Prentice-Hall of Southeast Asia Pte. Ltd., Singapore Editora Prentice-Hall do Brasil, Ltda., Rio de Janeiro Whitehall Books Limited, Wellington, New Zealand

Preface

The man who has ceased to learn ought not to be allowed to wander around loose in these dangerous days.

M. M. Coady

This book is intended for use as both an undergraduate- and graduate-level text in chemical reaction engineering. The level of difficulty will depend on the choice of chapters to be covered and the type and degree of difficulty of problems assigned from those at the end of each chaper. Most problems requiring significant numerical computations can be solved with a personal computer which has at least BASIC as a programming language.

The thrust of this book is to present in a clear and concise manner the fundamentals of chemical reaction engineering. First, a structure is developed that allows the reader to solve reaction engineering problems through reasoning rather than through memorization and recall of numerous equations and the restrictions and conditions under which each equation applies. In perhaps no other area of engineering is mere formula plugging more hazardous; the number of physical situations in reaction engineering that can arise appears infinite, and the chances of a simple formula being sufficient for the adequate design of a real reactor are vanishingly small. However, the algorithms presented in the text for reactor design provide a framework with which one can develop confidence through reasoning rather than memorization.

Due to the rapid addition of new information and scientific principles, a true engineer must constantly expand his or her horizons beyond simple gathering of information and engineering principles. Thus the second goal of this book is to

XVIII Preface

increase the student's lifelong learning skills by presenting hueristics and problems that encourage the student to practice certain intellectual skills. To accomplish this, we use (1) conventional problems that reinforce the student's understanding of the basic concepts and principles (included at the end of each chapter); (2) problems whose solution requires reading the literature, handbooks, or other textbooks on chemical engineering kinetics; and (3) problems that give students practice in problem definition and alternative pathways to solutions.

Another important skill fostered in this text is a critical analysis of journal articles. For the last ten years students in the graduate reactor engineering class at the University of Michigan have been required to carry out an in-depth critique of a journal article on chemical engineering kinetics. Although the students were told that choosing an article with erroneous data or reasoning was not necessary for a successful critique, it was stated that finding an error made the whole assignment much more fun. Consequently, a select number of problems at the end of chapters involve the critique of journal articles on reactor engineering which may or may not have major or minor inconsistencies. In some cases a small hint is given to guide the student in his or her analysis.

Many of the problems at the end of the various chapters were selected from those which have appeared in California Board of Registration for Civil and Professional Engineers—Chemical Engineering Examinations (PECEE) over past years. The permission for use of these problems, which, incidentally, may be obtained from the Documents Section, California Board of Registration for Civil and Professional Engineers—Chemical Engineering, 1004 6th Street, Sacramento, CA 95814, is gratefully acknowledged. (*Note:* These problems have been copyrighted by the California Board of Registration and many not be reproduced without their permission.) Additional problems are available on diskettes for use with the personal computer. Information about these interactive programs may be obtained from the author.

The strategy behind the presentation of material is the application, modification, or extrapolation of several basic ideas in chemical reaction engineering to solve a wide variety of problems. These ideas are referred to as the *Pillars of Chemical Reaction Engineering*, on which different applications rest. The pillars holding up the application of chemical reaction engineering are shown in Figure P-1.

The architecture and construction of the structure shown in Figure P-1 had many participants, most notably Professors Amundson, Aris, Smith, Levenspiel, and Denbigh. The contents of this book may be studied in virtually any order after the first four chapters, with few restrictions. A flow diagram showing possible paths is shown in Figure P-2.

In a three-hour undergraduate course at the University of Michigan approximately eight chapters are covered in the following order: Chapters 1, 2, 3, 4, Sections 5.1-5.3, 6.1-6.5, and Chapters 8, 10, 11, and parts of 13.

The reader will observe that although metric units are used primarily in this text (e.g., kmol/m³, J/mol), a variety of other units are also employed (e.g., lb/ft³).

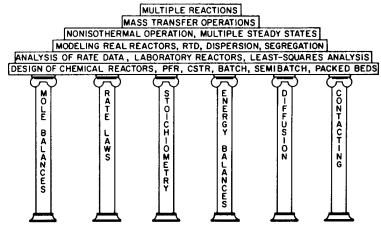


Figure P-1

This is intentional. It is our feeling that whereas most papers published in the future will use the metric system, today's engineers as well as those graduating over the next ten years will be caught in the transition between English, SI, and metric units. As a result, engineers will be faced with extracting information and reaction rate data from older literature which uses English units, as well as the current literature using metric, and should be equally at ease with both. However, all intensive laws tend often to have exceptions. Very interesting concepts take

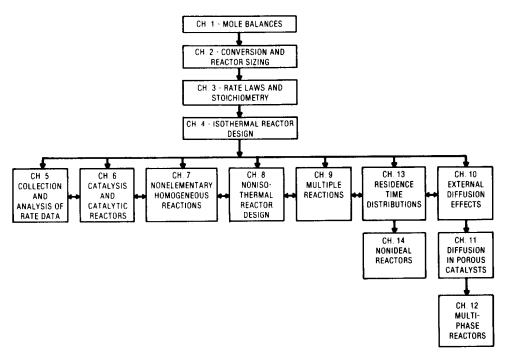


Figure P-2

XX Preface

orderly, responsible statements. Virtually all laws instinctively are normal thoughts. General observations become laws under experimentation.

The notes in the margins are meant to serve two purposes. One is to act as a guide or commentary as one reads through the material. Second, they identify key equations and relationships that are used to solve chemical reaction engineering problems.

Approximately three years after my first book, *The Elements of Chemical Kinetics and Reactor Calculations*, was published, I decided to revise and expand the programmed learning approach of the text. I asked Professor Lee Brown, whose research interests are kinetics and catalysis, to join me in rewriting the book, as he had used my programmed text in his course. I had always been impressed with the penetrating problems posed by Lee, which could not be solved by mere formula plugging. Dr. Brown later left the academic life for industry, and his limited time prevented him from participating to the extent that we originally expected. However, Dr. Brown collaborated in Chapters 13 and 14 (which are of joint authorship), provided material for Chapters 3, 6, and 8, and gave a critical reading of the entire book.

There are so many colleagues and students who contributed to this book that it would require another chapter to thank them all in an appropriate manner. Unfortunately, since Prentice-Hall has already requested a page reduction, this is not possible. However, certain people cannot go unacknowledged. The first is Neal Amundson, "The Chief," who I am sure is unaware of the various ways in which he has touched the author's career. Three of my colleagues at Michigan have, at different times and in different ways, been very important to the author personally and professionally. This book is dedicated to them: Guiseppe Parravano, Joe Martin, and Don Katz. I am also indebted to Max Peters and Octave Levenspiel, who first spawned my interest in chemical reaction engineering; Klaus Timmerhaus, who provided early guidance and a model to follow; Rane Curl, Uzi Mann, Erdogan Gulari, and Johannes Schwank, for their many insights and stimulating discussions; and certainly to Lee Brown for his friendship, penetrating questions, and artful presentation of material. Two other colleagues, Bob Kabel at Penn State and R. S. Shankar at I.I.T. Bombay, provided not only comments on the prepublication manuscript but also problems found at the ends of some chapters. To my colleagues in the department, thank you for your support and confidence, and for generating an atmosphere that spawns creativity and scholarship in teaching and research. J. S. Schultz was instrumental in helping to create such an atmosphere. A number of graduate and undergraduate students also contributed to the material in the book, primarily Abhaya Datye, T. Y. Hsieh, and Steve Le Blanc. Tim Nolan, Herb Alvord, Don DiMassi, Sunil Rege, and Greg McCabe helped proofread the final draft manuscript. Bruce Pynnonen was instrumental in helping to proofread the galley proof, and Tia Badalamente was invaluable in proofreading the page proofs. I would also like to thank Barbara Zeiders and her staff at Service to Publishers for their patient and outstanding job in taking the final manuscript through the final page proofs.

Preface xxi

My wife Janet, family Peter, Robert, and Kristin, and parents, Ralph and Anne, contributed greatly to the support necessary to complete a task such as this. Many people contributed to typing portions of the original manuscript, including, in the early stages, Diana Delonnay and Jill Taber. However, this book would never have been completed were it not for Susan Montgomery, an alumna of my undergraduate chemical reaction course. Susan typed, retyped, edited, pasted, proofread, and commented on the entire book many times in addition to handling the many details associated with putting the manuscript in final form.

H.S.F.

Ann Arbor February 1986

Contents

PREFACE		XVII
CHAPTER 1: MOLE BALANG	CES	1
1.1 definition of the rate	OF REACTION, $-r_A$	2
1.2 THE GENERAL MOLE BALA	NCE EQUATION	6
1.3 BATCH REACTORS		8
1.4 CONTINUOUS-FLOW REACTO	ORS	10
1.4.1 Continuous-Stirred	Tank Reactor	10
1.4.2 Tubular Reactor		11
1.5 INDUSTRIAL REACTORS		15
SUMMARY		19
QUESTIONS AND PROBLEMS	3	20
SOME THOUGHTS ON PROB	LEM SOLVING	23
SUPPLEMENTARY READING	ł	27
CHAPTER 2: CONVERSION	AND REACTOR SIZING	28
2.1 DEFINITION OF CONVERSION	N	28
2.2 DESIGN EQUATIONS		29
2.2.1 Batch Systems		29
2.2.2 Flow Systems		31

viii		Contents
2.3	APPLICATIONS OF THE DESIGN EQUATIONS	33
2.4	REACTORS IN SERIES	37
2.5	SOME FURTHER DEFINITIONS	47
	SUMMARY	49
	QUESTIONS AND PROBLEMS	51
	SOME THOUGHTS ON PROBLEM SOLVING	56
	SUPPLEMENTARY READING	57
СНА	PTER 3: RATE LAWS AND STOICHIOMETRY	59
3.1	BASIC DEFINITIONS	59
	3.1.1 The Reaction Rate Constant	60
	3.1.2 The Reaction Order	63
	3.1.3 Elementary Reactions and Molecularity	65
	3.1.4 Reversible Reactions	67
	3.1.5 Nonelementary Reactions	68
3.2	PRESENT STATUS OF OUR APPROACH	69
2 2	TO REACTOR SIZING AND DESIGN	70
3.3	3.3.1 Batch Systems	70 71
	3.3.2 Constant-Volume Reaction Systems	73
	3.3.3 Flow Systems	76
	3.3.4 Volume Change with Reaction	77
3.4	REACTIONS WITH PHASE CHANGE	86
	SUMMARY	89
	QUESTIONS AND PROBLEMS	92
	SOME THOUGHTS ON PROBLEM SOLVING	99
	SUPPLEMENTARY READING	103
СНА	PTER 4: ISOTHERMAL REACTOR DESIGN	105
4.1	DESIGN STRUCTURE FOR ISOTHERMAL REACTORS	106
4.2	SCALE-UP OF LIQUID-PHASE BATCH REACTOR DATA	
	TO THE DESIGN OF A CSTR	106
	4.2.1 Batch Operation	108
	4.2.2 Design of CSTRs	112
4.3	TUBULAR FLOW REACTORS	121
4.4	PRESSURE DROP IN REACTORS	126
	4.4.1 Flow through a Packed Bed	126
	4.4.2 Pressure Drop and the Rate Law	130
	4.4.3 Pressure Drop in Pipes	135

Cor	ntents	İX
4.5	REVERSIBLE REACTIONS	136
	4.5.1 Role of Nitric Oxide in Smog Formation	138
4.6	UNSTEADY-STATE OPERATION OF REACTORS	142
	4.6.1 Startup of a CSTR	143
	4.6.2 Semibatch Reactors	144
	4.6.3 Reactive Distillation	152
4.7	RECYCLE REACTORS	154
	SUMMARY	158
	QUESTIONS AND PROBLEMS	159
	SOME THOUGHTS ON PROBLEM SOLVING	175
	SUPPLEMENTARY READING	178
CHA	APTER 5: COLLECTION AND ANALYSIS OF RATE DATA	179
5.1	BATCH REACTOR DATA	180
	5.1.1 Differential Method of Rate Analysis	180
	5.1.2 Gas-Phase Reactions with Total Pressure	
	as the Measured Variable	182
	5.1.3 Integral Method	189
5.2	METHOD OF INITIAL RATES	195
5.3	METHOD OF HALF-LIVES	197
5.4	LEAST-SQUARES ANALYSIS	199
	5.4.1 Linearization of the Rate Law	199
	5.4.2 Nonlinear Analysis	200
	5.4.3 Weighted Least-Squares Analysis	201
5.5	DIFFERENTIAL REACTORS	203
5.6	EVALUATION OF LABORATORY REACTORS	206
	5.6.1 Integral (Fixed-bed) Reactor	206
	5.6.2 Stirred Batch Reactor	207
	5.6.3 Stirred Contained Solids Reactor (SCSR)	208
	5.6.4 Continuous-Stirred Tank Reactor (CSTR)	208
	5.6.5 Straight-through Transport Reactor	209
	5.6.6 Recirculating Transport Reactor	210
	5.6.7 Summary of Reactor Ratings	211
5.7	EXPERIMENTAL DESIGN	211
	5.7.1 Finding the Rate Law	211
	5.7.2 Experimental Planning	213
	SUMMARY	216
	QUESTIONS AND PROBLEMS	218
	SOME THOUGHTS ON PROBLEM SOLVING	225
	SUPPLEMENTARY READING	229

x			Contents
СНА	PTER 6	E CATALYSIS AND CATALYTIC REACTORS	231
6.1	CATA	LYSTS	231
	6.1.1	Definitions	231
	6.1.2	Catalyst Properties	233
6.2	STEPS	IN A CATALYTIC REACTION	235
	6.2.1	Adsorption Isotherms	238
	6.2.2	Surface Reaction	244
	6.2.3	Desorption	245
	6.2.4	The Rate-Limiting Step	245
6.3	SYNTI	HESIZING A RATE LAW, MECHANISM, AND RATE-LIMITING STEP	246
	6.3.1	Is the Adsorption of Cumene Rate Limiting?	249
	6.3.2	Is the Surface Reaction Rate Limiting?	253
	6.3.3	Is the Desorption of Benzene Rate Limiting?	254
	6.3.4	Summary of the Cumene Decomposition	255
6.4	DESIG	N OF REACTORS FOR GAS-SOLID REACTIONS	258
	6.4.1	Basic Guidelines	258
	6.4.2	The Design Equation	258
6.5	нете	ROGENEOUS DATA ANALYSIS FOR REACTOR DESIGN	261
	6.5.1	Deducing a Rate Law from the Experimental Data	262
	6.5.2	Finding a Mechanism Consistent	
		with Experimental Observations	264
		Evaluation of the Rate-Law Parameters	265
	6.5.4	Reactor Design	268
6.6		LYST DEACTIVATION	273
		Deactivation by Sintering or Aging	274
		Deactivation by Coking or Fouling	276
		Deactivation by Poisoning	276
		Temperature-Time Trajectories	280
	6.6.5	Effect of Deactivation on Selectivity	282
	0.0.0	Determining the Order of Deactivation	284
6.7	MOVII	NG-BED REACTORS	288
	SUMM	ARY	294
	QUEST	TIONS AND PROBLEMS	296
	SOME	THOUGHTS ON PROBLEM SOLVING	310
	SUPPL	EMENTARY READING	314
СНА	PTER 7	: NONELEMENTARY HOMOGENEOUS REACTIONS	316
7.1	FUND.	AMENTALS	317
	7.1.1	Active Intermediates	317
	7.1.2	Pseudo-Steady-State Hypothesis (PSSH)	319

Contents	xi
	731

7.2	SEAR	CHING FOR A MECHANISM	320	
	7.2.1	General Considerations	321	
	7.2.2	Hydrogen Bromide Reaction	324	
7.3	ENZY	MATIC REACTION FUNDAMENTALS	328	
	7.3.1	Definitions and Mechanisms	328	
	7.3.2	Michaelis-Menten Equation	331	
		Batch Reactor Calculations	334	
	SUMM	IARY	336	
	QUES	TIONS AND PROBLEMS	337	
	SOME	THOUGHTS ON PROBLEM SOLVING	345	
	SUPPI	EMENTARY READING	348	
СНА	PTER 8	B: NONISOTHERMAL REACTOR DESIGN	349	
8.1			349	
		DNALE		
8.2		ENERGY BALANCE	351	
		First Law of Thermodynamics	351	
		Evaluating the Work Term	352	
	8.2.3	Dissecting the Molar Flow Rates to Obtain the Heat of Reaction	353	
	8.2.4	Dissecting the Enthalpies	355	
		Relating $\Delta H_R(T)$, $\Delta H_R(T_R)$, and ΔC_p	356	
		Constant or Mean Heat Capacities	358	
		Variable Heat Capacities	358	
	8.2.8		361	
8.3	NONIS	SOTHERMAL CONTINUOUS-FLOW REACTORS		
		EADY STATE	362	
	8.3.1	Application to the CSTR	363	
	8.3.2	Adiabatic Tubular Flow Reactor	372	
	8.3.3	Steady-State Tubular Flow Reactor		
		with Heat Exchange	379	
8.4	EQUIL	EQUILIBRIUM CONVERSION		
	8.4.1	Adiabatic Temperature and Equilibrium Conversion	384	
	8.4.2	Optimum Feed Temperature	387	
8.5	UNSTI	EADY-STATE OPERATION	388	
	8.5.1	The General Equation	389	
	8.5.2	Unsteady Operation of Plug-Flow Reactors	390	
	8.5.3	Unsteady CSTR Operation	392	
	8.5.4	Batch Reactors	393	

xii		Contents
8.6	NONADIABATIC REACTOR OPERATION: OXIDATION	
	OF SULFUR DIOXIDE EXAMPLE	397
	8.6.1 Manufacture of Sulfuric Acid	397
	8.6.2 Catalyst Quantities	401
	8.6.3 Reactor Configuration	401
	8.6.4 Operating Conditions	402
8.7	MULTIPLE STEADY STATES	412
	8.7.1 Heat-Removed Term, $R(T)$	413
	8.7.2 Heat of Generation, $G(T)$	413
	8.7.3 Ignition-Extinction Curve	415
	8.7.4 Steady-State Bifurcation Analysis	419
	SUMMARY	425
	QUESTIONS AND PROBLEMS	426
	SOME THOUGHTS ON PROBLEM SOLVING	445
	SUPPLEMENTARY READING	450
СНА	PTER 9: MULTIPLE REACTIONS	452
9.1	CONDITIONS FOR MAXIMIZING THE DESIRED PRODUCT	
	IN PARALLEL REACTIONS	454
	9.1.1 Maximizing S for One Reactant	455
	9.1.2 Maximizing S for Two Reactants	457
9.2	MAXIMIZING THE DESIRED PRODUCT IN SERIES REACTIONS	461
9.3	STOICHIOMETRIC TABLE FOR MULTIPLE REACTIONS	465
9.4	HYDRODEALKYLATION OF MESITYLENE	471
	9.4.1 Description of the Reacting System	471
	9.4.2 Optimization of Xylene Production	
	in a Packed-Bed Reactor	475
9.5	NONISOTHERMAL CHEMICAL REACTIONS	479
9.6	WHAT IF THE PROCEDURE IN TABLE 9-2 CAN'T BE APPLIED?	481
	SUMMARY	491
	QUESTIONS AND PROBLEMS	494
	SUPPLEMENTARY READING	508
СНА	PTER 10: EXTERNAL DIFFUSION EFFECTS	
	IN HETEROGENEOUS REACTIONS	509
10.1	MASS-TRANSFER FUNDAMENTALS	510
	10.1.1 Definitions	510
	10.1.2 Molar Flux	511
	10.1.3 Fick's First Law	513

Conte	ents		xiii
10.2	10.2.1	DIFFUSION Evaluating the Molar Flux Boundary Conditions	514 517 517
		Modeling Diffusion without Reaction	523
		Temperature and Pressure Dependence of D_{AB}	523 523
	10.2.5	Modeling Diffusion with Chemical Reaction	523
10.3	EXTERN	NAL RESISTANCE TO MASS TRANSFER	524
	10.3.1	Mass-Transfer Coefficient	525
	10.3.2	Mass Transfer to a Single Particle	528
	10.3.3	Mass-Transfer-Limited Reactions in Packed Beds	532
	10.3.4	Mass-Transfer-Limited Reaction on Surfaces of Metals	539
10.4	WHAT	IF? (PARAMETER SENSITIVITY)	544
	SUMMA	RY	549
	QUESTI	ONS AND PROBLEMS	550
	SOME T	HOUGHTS ON PROBLEM SOLVING	558
	SUPPLE	MENTARY READING	559
СНАР	TER 11:	DIFFUSION AND REACTION IN POROUS CATALYSTS	560
11.1	DIFFUS	ION AND REACTION IN SPHERICAL CATALYST PELLETS	561
	11.1.1	Effective Diffusivity	561
	11.1.2	Derivation of the Differential Equation Describing Diffusion and Reaction	562
	11.1.3	Writing the Equation in Dimensionless Form	565
	11.1.4	Solution to the Differential Equation for a First-Order Reaction	567
11.2	INTERN	AL EFFECTIVENESS FACTOR	569
11.3	FALSIF	ED KINETICS	572
11.4		LL EFFECTIVENESS FACTOR	574
11.5		TION OF DIFFUSION- AND REACTION-LIMITED REGIMES	577
11.5		Wiesz-Prater Criterion for Internal Diffusion	577
		Mears' Criterion for External Diffusion	579
11.6	MASS T	RANSFER AND REACTION IN A PACKED BED	580
11.7	DETER!	MINATION OF LIMITING SITUATIONS FROM REACTION DATA	586
	SUMMA	RY	587
		ONS AND PROBLEMS	588
	•	MENTARY READING	595

xiv			Contents
СНАБ	TER 12	: MULTIPHASE REACTORS	596
12.1	SLURR	Y REACTORS	597
	12.1.1	Rate of Gas Absorption	599
	12.1.2	Transport to Catalyst	599
	12.1.3	Diffusion and Reaction in the Catalyst Pellet	600
	12.1.4	The Rate Law	600
	12.1.5	Determining the Limiting Step	600
	12.1.6	Slurry Reactor Design	609
12.2	TRICK	LE BED REACTORS	610
	12.2.1	Fundamentals	611
	12.2.2	Limiting Situations	614
	12.2.3	Evaluating the Transport Coefficients	614
	SUMMA	ARY	622
	QUEST	IONS AND PROBLEMS	622
	SUPPLI	EMENTARY READING	627
СНАР	ter 13:	DISTRIBUTIONS OF RESIDENCE TIMES	
		FOR CHEMICAL REACTORS	629
13.1	GENER	AL CHARACTERISTICS	629
	13.1.1	Residence-Time Distribution Function	632
13.2	MEASU	REMENT OF THE RESIDENCE-TIME DISTRIBUTION	633
	13.2.1	Pulse Input	633
	13.2.2	Positive-Step Tracer Experiment	638
	13.2.3	Negative-Step Tracer Experiment	639
13.3	CHARA	CTERISTICS OF THE RTD	640
	13.3.1	Integral Relationships	640
	13.3.2	Mean Residence Time	642
	13.3.3	Other Moments of the RTD	644
	13.3.5	Normalized RTD Function $E(\Theta)$	647
	13.3.5	Internal-Age Distribution $I(t)$	647
	13.3.6	RTDs and Chemical Reaction Rates	650
13.4	THE R	TD in ideal reactors	651
	13.4.1	RTDs in Batch and Plug-Flow Reactors	651
	13.4.2	Single CSTR RTD	651
	13.4.3	The RTD in CSTRs in Series	653
	13.4.4	Plug Flow-CSTR Series RTD	656
	13.4.5	Laminar Flow Reactor	659

Conte	ents	XV
13.5	RTDs in real reactor systems	661
	13.5.1 Tubular Reactor RTDs	661
	13.5.2 RTDs in a Continuous-Stirred Tank	665
	13.5.3 Tests on Some Fluidized Beds	666
13.6	REACTOR MODELING WITH THE RTD	668
13.7	MICROMIXING: THE SEGREGATION MODEL	669
	13.7.1 Segregation Model	669
	13.7.2 Analysis of Reactors with Completely Segregated Mixing	670
	SUMMARY	673
	QUESTIONS AND PROBLEMS	674
	SUPPLEMENTARY READING	679
СНАР	TER 14: ANALYSIS OF NONIDEAL REACTORS	680
14.1	THE BASIC IDEA	680
	14.1.1 Mathematical Tractability	681
	14.1.2 Physical Realism	681
	14.1.3 The Model Must Have at Most Two Parameters	681
14.2	MODELING REAL REACTORS WITH COMBINATIONS	(0)
	OF IDEAL REACTORS	682 682
	14.2.1 Real CSTR Modeled with an Exchange Volume	685
	14.2.2 Real CSTR Modeled Using Bypassing and Dead Space	686
14.3	TESTING A MODEL AND DETERMINING ITS PARAMETERS	687
	14.3.1 Two CSTRs with Interchange14.3.2 Tracer Use to Determine Parameters	007
	in CSTR-with-Deadspace-and-Bypass Model	692
14.4	MODELS OF TANK REACTORS	696
14.5	MODELS OF TUBULAR REACTORS	697
	14.5.1 Nonideality in Tubular Reactors	697
	14.5.2 Dispersion Model	697
14.6	MAXIMUM MIXEDNESS	707
14.7	using the RTD versus the need for a model	712
	SUMMARY	712
	QUESTIONS AND PROBLEMS	714
	SUPPLEMENTARY READING	719