A.S.Kazanskaya V.A.Skoblo

CALCULATIONS OF CHEMICAL EQUILIBRIA

> Mir Publishers Moscow



TO THE READER

Mir Publishers would be grateful for your comments on the content, translation and design of this book. We would also be pleased to receive any other suggestions you may wish to make. Our address is:

USSR, 129820, Moscow I-110, GSP Pervy Rizhsky Pereulok, 2 MIR PUBLISHERS



А. С. Казанская, В. А. Скобло

РАСЧЁТЫ ХИМИЧЕСКИХ РАВНОВЕСИЙ

Сборник примеров и задач

Под редакцией проф. Г. М. Панченкова

«ВЫСШАЯ ШКОЛА» МОСКВА

- A. S. Kazanskaya
- V. A. Skoblo

CALCULATIONS OF CHEMICAL EQUILIBRIA Examples and Problems

Editedby Prof.G. M. Panchenkov

Translated from the Russian by G. Leib

Mir Publishers Moscow Pirst published 1978
Revised from the 1974 Russian edition

На английском языке

- © Издательство «Высшая школа», 1974
- © English translation, Mir Publishers, 1978

Contents

Preface 9

1.	Calculation of the Heat of a Chemical Reaction 11
1.1.	Relationship Between Heats of Reactions Proceeding at Constant Pressure (ΔH) and Constant Volume (ΔU) 14
1.2.	Calculation of the Heats of Reactions. Hess's Law 18
1.2.1.	Determining Reaction Heats by Combining Equations of Reactions 19
1.2.2.	Calculating the Heat of Reactions from the Heats of Combustion of the Substances Participating in Them 22
1.2.3.	Calculating the Heat of Reactions from the Heats of Formation of the Substances Participating in Them 28
1.3.	Empirical Methods for Determining the Standard Heats of Combustion and Formation of Organic Compounds from Simple Substances 31 A. Methods of Calculating the Standard Heats of Combustion $(\Delta H_{298}^{\circ})_{\rm comb}$ 31
1.3.1.	Konovalov's Method of Calculating $(\Delta H_{298}^{\circ})_{comb}$ 31
1.3.2.	Kharasch's Method of Calculating $(\Delta H_{298}^{\circ})_{\text{norm}}^{\text{lq}}$ 33
1.3.3. 1.3.4. 1.3.5.	Calculation of $(\Delta H^{\circ}_{298})_{\text{comb}}$ by the Method of Increments 36 Tatevsky's Method of Calculating $(\Delta H^{\circ}_{298})_{\text{comb}}$ 38 Laidler's Method of Calculating $(\Delta H_{298})_{\text{comb}}$ 39 B. Methods of Calculating the Standard Heats of Formation of Organic Compounds from Simple Substances $(\Delta H^{\circ}_{298})_{\text{form}}$ 41
1.3.6.	Calculation of $(\Delta H_{298}^2)_{\text{form}}$ of Organic Substances in the Gaseous State from the Bond Energies 41
1.3.7.	Calculation of $(\Delta H_{298}^{\circ})_{form}$ of Hydrocarbons by the Method of Increments 45
1.3.8.	Calculation of $(\Delta H^2_{208})_{form}$ of Gaseous Organic Compounds by the Method of Introducing Corrections for the Substitution of Hydrogen by —CH ₃ and Other Groups 46
1.3.9. 1.3.10. 1.3.11.	Maslovs' Method of Calculating $(\Delta H_{298}^2)_{\text{form}}$ 52 Franklin's Method of Calculating $(\Delta H_{298}^2)_{\text{form}}$ 57 Souders's, Matthews's, and Hurd's Method of Calculating $(\Delta H_{298}^2)_{\text{form}}$ 60
1.4.	Heat Capacity 62
1.4.1.	Definitions. Heat Capacity in Various Processes. Relationship Retween C_{∞} and C_{W} 62

1.4.2. 1.4.3. 1.5. 1.6.	Temperature Dependence of Heat Capacity. Relationship Between Mean and True Heat Capacities 65 Some Empirical Methods of Calculating the Standard Heat Capacity C_p° of Gaseous Organic Substances 73 Temperature Dependence of the Heat of a Reaction 76 Determining the Heat of a Reaction According to the Equilibrium Constant 83 Problems 86
2.	Entropy 105
2.1. 2.2. 2.3. 2.4. 2.5.	Calculation of Entropy 107; Calculation of Absolute Value of Entropy 118 Standard Entropy at 298.15 K (S_{298}°) 131 Some Approximate Methods for Calculating the Standard Entropy at 298.15 K 137 Calculation of the Change in Entropy as a Result of a Reaction 144 Problems 146
3. 3.1. 3.2. 3.3.	Methods for Calculating the Changes in the Gibbs Energy ΔG_T in the Course of a Reaction 158 Basic Methods of Calculation 158 An Empirical Method for Calculating $(\Delta G_T^\circ)_{form}$ of Organic Compounds from Simple Substances 169 Calculation of Equilibrium Constant 172
4.	Problems 175 Calculation of Chemical Equilibrium in Ideal Gaseous
4.1. 4.2.	Systems 183 Calculating Composition of Equilibrium Mixture When One Reaction Proceeds 183 Calculating Composition of Equilibrium Mixture When Several Parallel or Consecutive Reactions Proceed 188 Problems 198
5.	Thermodynamic Calculation of Chemical Equilibrium in Real Gaseous Systems 204
5.1. 5.1.1. 5.1.2. 5.1.3. 5.1.4. 5.1.5. 5.2.	Methods of Calculating Fugacity 205 Calculating the Fugacity According to the Volume Correction α for a Real Gas 205 Approximate Calculation of Fugacity 208 Calculations Using an Equation of State 209 Calculations According to the Activity Coefficient 210 Calculations Through the Compression Factor 215 Calculating the Composition of an Equilibrium Mixture in a Real System 217 Empirical Methods for Calculating the Critical Parameters 220

5.4.	Calculation of Enthalpies of Substances and Heats of Reactions Conducted at High Pressures 228 .
	Problems 234 Combined Problems 240

Appendices: 247 Thermodynamic Properties of Selected Simple Substances and Compounds 247 Numerical Values of the Thermal Characteristic of Konovalov's

Equation

Heat Corrections for the Kharasch Equation 262

Numerical Values of Constants Used to Calculate the Standard Heats of Combustion and Formation of Alkanes from Simple Substances at 298.15 K According to Tatevsky 267

5. Contributions of Selected Bonds and Atomic Groups to Standard Heats of Combustion and Formation from Simple Substances at 298.15 K for Organic Compounds in the Gaseous and Liquid States According to Laidler 267 Bond Energies 268

Bond Energies

Corrections for Approximate Calculation of Standard Heats of Formation from Simple Substances, Heat Capacities, and Entropies (in Idealized Gaseous State) by the Method of Introducing Corrections for the Substitution of Hydrogen by -CH3 and Other Groups 269

Products of Principal Moments of Inertia of Halomethanes and 8. Their Symmetry Numbers Needed for Calculating Thermodynamic Properties According to Yu. Maslov and P. Maslov 273

Group Contributions $\Delta H_{\mathrm{form}}^{\circ}$ and $\Delta G_{\mathrm{form}}^{\circ}$ According to Frank-9.

Group Contributions for Calculating $(\Delta H_T)_{form}$ According to 10. Souders, Matthews, and Hurd 282

11. Characteristic Temperatures of Selected Gases 285

12. Einstein's Functions for Calculating the Vibrational Component of the Heat Capacity of a Gas 286

13. Heat Capacity C_p° of Standard Substances of Aliphatic and Cyclic

Compounds According to Kelley, Parks, and Huffman 286 Constants of Eq. (2.34) for Calculating Standard Entropies at 14. 298.15 K for Selected Kinds of Solid Inorganic Substances

Constants A and B of Eqs. (2.35) and (2.36) for Calculating Stand-15. ard Entropies at 298.15 K for Selected Gases 287

Values of M_n for Calculating Thermodynamic Functions Accord-16. ing to Temkin and Shwartsman 288

17. Group Contributions and Corrections for Deviation in Structure of Hydrocarbon for Calculating $(\Delta G_T)_{form}$ According to Chermen and van Krevelen 288

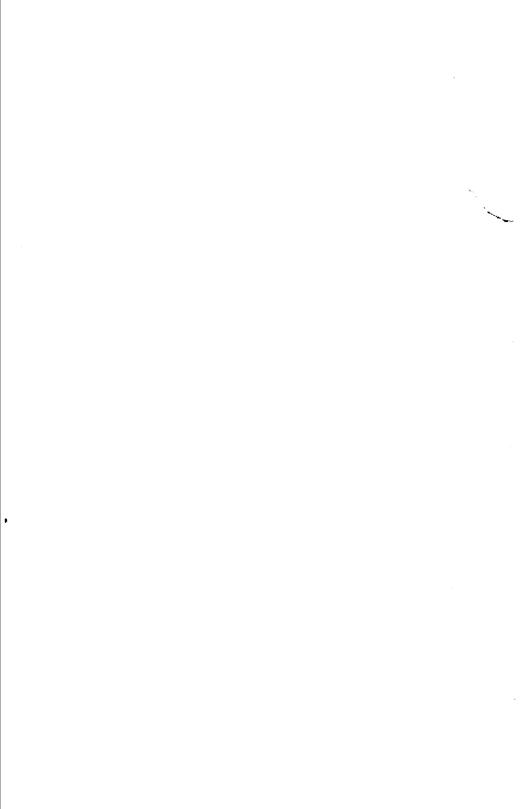
18. Solution of the Equation of the Law of Mass Action for Different Types of Reactions 293

Activity Coefficient of Individual Gases and Liquids 19. 20. Compression Factors of Individual Gases and Liquids 304

21. Atomic and Structural Constants for Calculating Critical Parame-

ters According to Lydersen 308 Contributions for Calculating Critical Parameters According to 22. Forman and Thodos 309

23. Change in Enthalpy of Gases and Liquids upon Compression 314 References 318 Answers to Problems



Preface

The main object of this training aid is to teach students how to calculate chemical equilibria. A chemical engineer must be able to calculate whether or not a given chemical process will proceed, determine the stability of substances in given external conditions, compute the equilibrium and, consequently, the maximum yields of the products in given conditions, and find the optimal external

parameters for conducting a process.

We have given great attention to calculating the heats of chemical reactions, heat capacities, entropies, and fugacities. Apart from problems involving the direct application of the fundamental laws of chemical thermodynamics, the book contains interesting examples showing various empirical and approximate methods of calculations. For instance, space is devoted to calculations of the heats of combustion by the methods of D. Konovalov, M. Kharasch, of increments, of introducing corrections for the substitution of hydrogen by methyl and other groups, of P. Maslov, J. Franklin, M. Souders, C. Matthews, and C. Hurd. Approximate methods, which play a great part in engineering calculations of chemical processes, are considered for heat capacities, standard entropies, and Gibbs energies.

A large section is devoted to calculating the change in the Gibbs energy as a result of chemical reactions and of the compositions of equilibrium mixtures. Since in practical work one often has to do with non-ideal systems, we have set out the basic methods of calculating fugacities, as well as the use of fugacities and activity coefficients for determining the equilibrium composition of a mixture of non-ideal systems. We have also described empirical methods of calculating the critical parameters (the method of A. Lydersen, J. Forman, and G. Thodos), and the calculation of enthalpies and heats of reactions conducted at high pressures.

We begin each chapter with a brief theoretical introduction treating the main formulas needed for solving the problems. The introduction is given only to remind our readers of the basic laws used in solving the problems, and cannot in any way replace a textbook

in chemical thermodynamics. Each chapter gives a number of examples with detailed solutions in order to show how to apply the thermodynamic laws and formulas in solving concrete problems. Next, problems for independent work are given—the answers to which can be found at the end of the book.

The Appendices contain reference tables. They are needed, first, for solving the problems; and, second, they are of an independent significance because they will permit students to solve many thermodynamic problems proposed by the instructor or confronting them when studying special chemical subjects and chemical technology as well as when performing course or diploma work or designs. The Appendices are followed by a list of monographs and reference books that can be used in solving problems in chemical thermodynamics.

The present collection of examples and problems has been compiled using the experience gained through many years of teaching the course of chemical thermodynamics to students of the faculty of chemistry and chemical technology of the I. M. Gubkin Institute of the Petrochemical and Gas Industry in Moscow. It is based on up-to-date material published in recent years in monographs, reference books on physical chemistry and chemical thermodynamics, and in separate articles in various journals. Students study chemical thermodynamics after a course in physical chemistry. Although they are acquainted with the solution of some of the problems in the course of physical chemistry, our teaching experience has shown the great need for the proposed type of problem book, purposefully directed at training students in the methods of calculating chemical equilibria. The book will also be of interest for workers of research institutions and engineers specializing in chemistry and chemical technology.

Chapters 1 and 2 were compiled by V. A. Skoblo, and Chapters 3,

4 and 5 by Λ. S. Kazanskaya.

We express our deep gratitude to the late prof. V. A. Kireev, senior scientific worker A. A. Lopatkin, associate professor V. P. Dreving, and all of those in the department of physical chemistry of the Byelorussian State University headed by associate professor A. A. Vecher for their attentive critical analysis which helped us to improve the quality of the book.

G. M. Panchenkov

Calculation of the Heat of a Chemical Reaction

Chemical processes are attended by the liberation or absorption of heat which is called the heat of a reaction (or the heat effect by some authors). A chemical reaction consists in the breaking of a definite number of chemical bonds between the atoms in a molecule and in the formation of new bonds. If the energy liberated in the formation of the new bonds exceeds that spent for breaking the bonds in the initial molecules, the reaction is attended by the liberation of heat (an exothermic process); if the energy liberated in the formation of the new bonds is less than that of breaking the bonds, the reaction is attended by the absorption of heat from the surroundings (an endothermic process). Consequently, in chemical transformations, the internal energy of the reacting molecules changes.

The change in the internal energy dU in the course of a chemical transformation occurs, according to the first law of thermodynamics, at the expense of the absorption (or liberation) of the heat δQ and the performance of the work δW . We shall write the analytical expression of the first law of thermodynamics in the form

$$dU = \delta Q - \delta W \tag{1.1}$$

The change in the internal energy as a result of a chemical reaction does not depend on the path followed by it, but depends only on the initial and final states of the system.

The heat of a reaction in the general case is not a change in a function of state and, therefore, depends on the path of a process. In two very simple cases, however, when a process occurs at a constant pressure p or a constant volume V, the independence of the path also extends to the heat of the process (including a chemical reaction). If a reaction proceeds at V= const, and no electrical or other kinds of work is performed, i.e. W=0, then according to Eq. (1.1), with the temperature T constant, the heat of a reaction is

$$Q_V = U_2 - U_1 = \Delta U \tag{1.2}$$

The heat of a chemical reaction Q_V (the subscript V denotes that V = const) equals the change in the internal energy as a result of

the reaction. If a reaction proceeds at constant pressure and only the work of volume expansion is performed (other kinds of work are absent), the analytical expression of the first law of thermodynamics will become

$$\delta Q = dU + p \ dV \tag{1.3}$$

where the elementary work δW is represented only by the work of expansion, i.e. $\delta W = p \ dV$. Integration of Eq. (1.3) with p = const yields

$$Q_p = U_2 - U_1 + p (V_2 - V_1)$$
or
$$Q_p = (U_2 + pV_2) - (U_1 + pV_1)$$
(1.4)

Since p and V are parameters of state, while U is a function of state, the sum (U + pV) is also a function of state. Its change does not depend on the path of a process, but only depends on the initial and final states of the participants of a reaction. This function is called *enthalpy* and is designated by the symbol H:

$$U + pV = H (1.5)$$

Consequently

$$Q_p = H_2 - H_1 = \Delta H \tag{1.6}$$

If a reaction proceeds at constant pressure, then when T = const, its heat equals the change in enthalpy as a result of the reaction.

Thus, in the above cases (1.2) and (1.6), the heat of a chemical process equals the change in the functions of state; therefore, it does not depend on the path of a process, but only depends on the initial and final states.

At present, customary practice is to write the heat of a reaction as follows. The stoichiometric equation of a reaction is attended by indication of the difference between the internal energies (or enthalpies) of the products and the reactants, i.e. $\Delta U = Q_V$ (or $\Delta H = Q_P$)—the growth in internal energy (or enthalpy). If this growth is positive, the reaction proceeds with the absorption of heat; and if it is negative, heat is liberated. For example, the oxidation of liquid benzene at constant pressure to carbon dioxide and liquid water proceeding with the liberation of heat is written as follows:

$$C_6H_6(lq) + \frac{15}{2}O_2(g) = 6CO_2(g) + 3H_2O(lq)$$

 $Q_p = \Delta H = -780980 \text{ cal}$

The symbols (c), (lq), and (g) are used after the chemical formula of a substance to indicate whether it is crystalline (solid), liquid, or gaseous, respectively. These symbols are usually omitted when the state of aggregation of the components of a reaction is obvious. For instance, the hydrogenation of acetylene to ethane conducted at

constant pressure and at 25 °C proceeds in the gaseous phase. It may therefore be written as follows:

$$C_2H_2 + 2H_2 = C_2H_6$$
, $Q_p = \Delta H = -74430$ cal

This reaction, like that in the preceding example, is exothermic. The need to indicate the state of aggregation of reaction components is due to the fact that the heat of a reaction depends on the state of aggregation of the reactants and products. If the state of aggregation changes as a result of a chemical reaction, its heat also includes the heat of the relevant phase transition (heat of vaporization or condensation, fusion or freezing, sublimation or condensation).

The heat of a reaction depends on whether or not the temperature of the reactants and products is the same. If the products of a reaction proceeding with the liberation of heat have a higher temperature than the reactants, part of the liberated heat will go for heating the reactants. Consequently, the measured heat of the reaction will be less than when the temperature of the reactants and products is the same.

Therefore, when measuring the heat of a reaction, the temperature of the reactants must exactly equal that of the products.

For the convenience of further thermodynamic calculations, we shall denote the heat of a chemical reaction in conditions of constant pressure by the symbol ΔH , and in conditions of constant volume by the symbol ΔU . In laboratory and industrial conditions, we most often encounter reactions proceeding at constant pressure.

If ΔH is positive, the reaction, as noted above, is endothermic. For example for the thermal cracking of gas oils $\Delta H = +70-250$ kcal/kg of converted starting material; for the pyrolysis of kerosenes $\Delta H = +400-500$ kcal/kg; for platforming $\Delta H = +180$ kcal/kg; and for the catalytic cracking of petroleum fractions $\Delta H = +50-130$ kcal/kg.

If ΔH is negative, the process is exothermic. For example for the regeneration of the catalysts of catalytic cracking $\Delta H = -8000$ kcal/kg; for the hydrogenation of isooctene $\Delta H = -245$ kcal/kg; and for the alkylation of isobutane with isobutene $\Delta H = -250$ kcal/kg.

In previous publications, the thermochemical heats were used. They are denoted by the symbols \overline{Q}_V and \overline{Q}_p and differ from the thermodynamic heats described above (which we shall use in the following) in their sign:

$$Q = -\bar{Q}$$

This must be taken into consideration in reading chemical literature.

In the thermochemical writing of chemical reactions, the righthand side of a reaction is followed by a term characterizing the liberation or absorption of heat as its result. Equations written in this way are called *thermochemical*. The exothermic reactions considered above have the form

$$C_6H_6(lq) + \frac{15}{2}O_2(g) = 6CO_2(g) + 3H_2O(lq) + 780\,980$$
 cal

 $\mathrm{C_2H_2}\,+2\mathrm{H_2}=\mathrm{C_2H_6}\,+74$ 430 cal

The endothermic reaction of formation of acetylene is written as follows:

$$2C(c) + H_2(g) = C_2H_2(g) - 54 190 \text{ cal}$$

It is essential for thermochemical calculations that all the heats of reactions be related to identical conditions; otherwise their values will be incompatible. This is due to the fact that the heat of a chemical reaction depends on temperature and to a smaller extent on pressure. The heats of chemical reactions are customarily reduced to standard conditions. For individual solids and liquids, their state at 1 atm and the given temperature is taken as the standard one. For individual gases, their state in the form of a hypothetic ideal gas whose fugacity equals unity at the given temperature is taken as the standard one. The properties of individual gases at 1 atm do not differ too much from their properties in standard conditions; this difference is usually disregarded in calculations not requiring a high accuracy. Attention must be given to the circumstance that for a gaseous chemical reaction conducted in standard conditions it is not the total pressure that equals 1 atm, but the partial pressure of each of the gaseous reagents.

The heat of a chemical reaction conducted in standard conditions is designated ΔH_T° . The superscript indicates the standard state while the subscript is the temperature (in kelvins) at which the reaction is conducted. The standard heat of a reaction can be calculated for any temperature T, but most often 298.15 K (25.00 °C) is used. In this case, the standard heat of a reaction is denoted by ΔH_{298}° . The temperature 298.15 K is chosen because other very important characteristics of processes are given for this temperature. Calorimetric measurements are also related to it.

1.1

Relationship Between Heats of Reactions Proceeding at Constant Pressure (ΔH) and Constant Volume (ΔU)

In a chemical reaction, a change in the number of moles of one component unambiguously determines the change in the number of moles of the remaining components. We can therefore say that for systems in which a reaction occurs the internal energy will be a function not only of temperature and volume, but also of the number of moles n of one of the reagents:

$$U = f(V, T, n) \tag{1.7}$$

The total differential of the internal energy

$$dU = \left(\frac{\partial U}{\partial T}\right)_{V, n} dT + \left(\frac{\partial U}{\partial V}\right)_{T, n} dV + \left(\frac{\partial U}{\partial n}\right)_{V, T} dn \tag{1.8}$$

If we consider a system at T = const and p = const, then Eq. (1.8) may be rewritten in the form

$$\left(\frac{\partial U}{\partial n}\right)_{p, T} = \left(\frac{\partial U}{\partial V}\right)_{T = n} \left(\frac{\partial V}{\partial n}\right)_{p, T} + \left(\frac{\partial U}{\partial n}\right)_{V, T} \tag{1.9}$$

Differentiation of Eq. (1.5) yields

$$\left(\frac{\partial H}{\partial n}\right)_{p, T} = \left(\frac{\partial U}{\partial n}\right)_{p, T} + p \left(\frac{\partial V}{\partial n}\right)_{p, T} \tag{1.10}$$

Using Eq. (1.9) in (1.10), we get

$$\left(\frac{\partial H}{\partial n}\right)_{p, T} = \left(\frac{\partial U}{\partial n}\right)_{V, T} + \left[\left(\frac{\partial U}{\partial V}\right)_{T, n} + p\right] \left(\frac{\partial V}{\partial n}\right)_{p, T} \tag{1.11}$$

For the change in volume upon the conversion of one mole, we can write

$$\Delta V = \left(\frac{\partial V}{\partial n}\right)_{p,T} \tag{1.12}$$

But at V = const, we have

$$dQ_V = (dU)_{V, T} = \left(\frac{\partial U}{\partial n}\right)_{V, T} dn \tag{1.13}$$

or

$$Q_{V} = (\Delta U)_{V, T} = \left(\frac{\partial U}{\partial n}\right)_{V, T} \Delta n \tag{1.14}$$

If $\Delta n = 1$, then

$$Q_V = \left(\frac{\partial U}{\partial n}\right)_{V, T} \tag{1.15}$$

We can prove by similar reasoning that

$$Q_p = \left(\frac{\partial H}{\partial n}\right)_{p, T} \tag{1.16}$$

Introducing Eqs. (1.12), (1.15), and (1.16) into Eq. (1.11), we get

$$Q_{p} = Q_{V} + \left[\left(\frac{\partial U}{\partial V} \right)_{T} + p \right] \Delta V \tag{1.17}$$

or

$$\Delta H = \Delta U + \left[\left(\frac{\partial U}{\partial V} \right)_T + p \right] \Delta V \tag{1.18}$$