

AEROSOL PROCESSING OF MATERIALS

Toivo T. Kodas and Mark J. Hampden-Smith

Superior Micropowders, Albuquerque, NM

This book is printed on acid-free paper. ®

Copyright ©1999 by Wiley-VCH. All rights reserved.

Published simultaneously in Canada.

No part of this publication may be reproduced, stored in a retrieval system or transmitted in any form or by any means, electronic, mechanical, photocopying, recording, scanning or otherwise, except as permitted under Section 107 or 108 of the 1976 United States Copyright Act, without either the prior written permission of the Publisher, or authorization through payment of the appropriate per-copy fee to the Copyright Clearance Center, 222 Rosewood Drive, Danvers, MA 01923, (978) 750-8400, fax (978) 750-4744. Requests to the Publisher for permission should be addressed to the Permissions Department, John Wiley & Sons, Inc., 605 Third Avenue, New York, NY 10158-0012, (212) 850-6011, fax (212) 850-6008, E-Mail: PERMREQ@WILEY.COM.

98-3623

Library of Congress Cataloging in Publication Data:

```
Kodas, Toivo T. (Toivo Tarmo), 1958—
Aerosol processing of materials / by Toivo T. Kodas and Mark J. Hampden-Smith
p. cm.
Includes index.
ISBN 0-471-24669-7 (cloth: alk. paper)
1. Thin films. 2. Aerosols. 3. Chemical vapor deposition.
I. Hampden-Smith, Mark J. II. Title.
TA418 9 T45K63 1999
```

Printed in the United States of America

10 9 8 7 6 5 4 3 2 1

621.3815'2-dc21

AEROSOL PROCESSING OF MATERIALS

PREFACE

There is currently considerable commercial and scientific interest in the production of powders and the deposition of films employing aerosol-based methods. Existing applications that employ aerosol techniques range from the production of highly dispersed metal oxide powders for use in the pigment industry to the deposition of thin films of materials, which modify the optical characteristics of glass windows and display screens.

This book describes the principles and practice of aerosol science and engineering along with the relevant aspects of materials science and engineering. The book is organized in the following manner: the early chapters deal with the basic principles of aerosols. After a general introduction in Chapter 1, Chapters 2-7 describe the fundamental aspects of aerosols such as particle size, transport, growth, evaporation, and collision and coalescence. Chapter 8 describes the chemistry relevant to aerosol processes to materials and Chapter 9 describes the characteristics of nanostructured materials because aerosol methods are among the best synthetic routes to prepare this class of materials. This is followed by a discussion of the overall qualitative behavior and technology of gas-to-particle conversion; liquid-to-solid, and solid-to-solid conversion; and film formation in Chapters 10-15. These chapters combine the principles described in Chapters 1-9 to better understand the practicalities of these systems. Equipment that can be used to produce materials by aerosol methods is found in Chapter 16 and Chapter 17 describes the measurement techniques that have been used to characterize materials produced by aerosol methods.

ACKNOWLEDGMENTS

We are indebted to a number of people who have contributed in direct and indirect ways to this work. We appreciate the members of our research groups for their patience in reading, correcting and making suggestions to the drafts of the manuscript and we want to acknowledge Quint Powell, Dave Dericotte, James Brewster, Dr. Sanjeev Jain, Dr. Abhijit Gurav, and Dr. Paolina Atanasova, who were particularly insightful.

We thank the employees of Nanochem Research, Inc. and Superior MicroPowders, LLC for their patience and input over the last 5 years and their dedication to making many of the aerosol routes described in this book a manufacturing reality.

We are grateful to Professor Sotiris Pratsinis for his energy, enthusiasm and assistance in coming up with the idea for this book, the basic outline and detailed input on many chapters of this book, particularly Chapters 1–7.

We thank Judith Binder for her tireless work throughout the preparation of this manuscript. She more than anyone is responsible for pulling the details together into a useful form. In addition we thank Nena Davis and Kelley Burns for various editorial contributions.

Finally we thank our families for their love and patience during the time this work has taken. Toivo thanks Cynthia, Aidan, and Maila for enduring the countless hours spent away from them. Mark thanks Tessa, Emily, and Harry.

NOMENCLATURE

A	total particle surface area per volume of gas, cm ² /cm ³
а	surface area of agglomerates or particles, cm ²
A_A	Avogadro's number, number/mole
a'	interatomic distance, cm
a_a	water activity in solution droplet, dimensionless
A_c	constant
a_c and a_{sol}	solute activity, dimensionless
a_o	monomer surface area, cm ²
A_r	rate constant
A_{s}	substrate surface area or heated area over which deposition
M^2	takes place, cm ²
a	surface area of sphere, cm ²
a_s	number of moles of solid required for reaction with one
D	mole of gaseous reactant
D D D ata	constants
$B_1, B_2, B_3, \text{ etc.}$	deposition efficiency, dimensionless
$egin{array}{c} b_{th} \ C \end{array}$	concentration, moles/cm ³ or molecules/cm ³
c	velocity vector, cm/sec
C_{A_s} C_b C_c C_D C_L C_o	concentration of species A in gas, moles/cm ³
C_b	percentage of atoms in grain boundary, dimensionless
C	Cunningham correction factor, dimensionless
C_D	drag coefficient, dimensionless
C_L	concentration of reactant in liquid, g/cm ³ or moles/cm ³
C_o	concentration of solute at center of drop, mole/cm ³ ; or
0	solubility over a flat surface, g/cm ³
C_p C_{pa} C_r C_s	heat capacity at constant pressure, erg/K mol
Cpa	heat capacity of wet air, erg/K mol
C_r	molar concentration of gaseous reactant, moles/cm ³
C_s	concentration at surface of particle or immediately above
	substrate, moles or molecules/cm ³
C_{sat}	saturation concentration, moles/cm ³ or molecules/cm ³
C_T	pre-exponential for temperature-dependent form of
	precursor vapor pressure, moles/cm ³
c_x	velocity in x-direction, cm/sec

xxii NOMENCLATURE

\dot{C}_{∞}	vapor concentration far from droplet, moles/cm ³ or molecules/cm ³
\bar{c}	mean molecular velocity, cm/sec
D	particle diffusion coefficient or diffusivity of gas or vapor, cm ² /sec
D_{cr}	effective diffusivity of vapor in crust, cm ² /sec
D_e	effective diffusion coefficient in film or porous layer, cm ² /sec
d_e	equivalent volume diameter, diameter of sphere corresponding to same volume as irregular particle, cm
D_{ϵ}	mass fractal dimension, dimensionless
D_{j}	diffusion coefficient in gas phase, cm ² /sec
d^g	average particle diameter for a lognormal distribution, cm
d_{g}	geometric mass average diameter, cm
d gm	geometric number average diameter, cm
$egin{array}{l} D_f \ D_g \ d_g \ d_{ m gm} \ d_{ m gn} \ d_{ m gr} \ D_L \ { m or} \ D_l \ D_$	average grain diameter, cm
D or D	liquid phase diffusion coefficient of solute, cm ² /sec
D_L of D_l	diffusion coefficient at reference conditions, cm ² /sec
	diameter of primary particle, cm
d_{o}	droplet or particle diameter, cm
a_p, a_{p1}, a_{p2}	critical particle diameter, cm
a_p	particle diameter, cm
a_{pi}, a_{pj}	mass average diameter, cm
a_{pm}	number (count) average diameter, cm
a_{pn}	initial particle diameter, cm
a_{po}	average primary particle diameter, cm
a_{pp}	equivalent sphere diameter of completely dried
d_p, d_{p1}, d_{p2} d_p^* d_{pi}, d_{pj} d_{pm} d_{pn} d_{po} d_{pp}	droplet, cm
$d_{p\overline{m}}$	diameter of particle with average mass, cm
D_{s}	surface fractal dimension, dimensionless
$egin{array}{c} D_s \ d_s \ d_t \ D_v \end{array}$	Sauter diameter, cm
d_t	tube or pipe diameter, cm
D_v	vapor diffusion coefficient in air, cm ² /sec
$d_{\overline{m}}$	mass mean diameter, cm
E	electric field
е	charge of an electron, statcoulomb
E_I	efficiency of impaction, dimensionless
$E_A \\ E_d$	activation energy, erg/mol K
E_d	deposition efficiency, fraction of particles entering that deposit inside tube or other channel or body, dimensionless
E_L	surface field strength for spontaneous emission of electrons or ions, statvolt/cm
F	rate at which molecules enter gas phase by diffusion from single droplet, molecules/sec
. f	Fanning friction factor, dimensionless

f_0	fraction of material A in mixture, dimensionless
F_1 , F_2	Fuchs-Sutugin correction factor, dimensionless
	air molar flow rate, moles/sec
F_a	
$F_{\underline{E}}$	electrophoretic force exerted on particle, dyne
F_G	force of gravity, dyne
F_{i}	force acting on a particle, dyne
$F_{:::}$	free energy, erg/cm ³
F_	gas drag, dyne
F R	feed rate of reactant, moles/sec
r	
$F_{\mathcal{S}}$	gravitational force exerted on particle, dyne
f_t	transducer frequency, 1/sec
$egin{aligned} F_E \ F_G \ F_i \ F_{i,j} \ F_R \ F_r \ F_S \ f_t \ F_{ ext{th}} \ G \end{aligned}$	thermophoretic force exerted on particle, dyne
G	particle growth law, cm ³ /sec
g	acceleration due to gravity, cm/sec ²
G_c	constant, cm ² /sec
$H^{\tilde{c}}$	Henry's constant
h_g	heat transfer coefficient in gas surrounding particle,
· · g	erg/cm ² sec K
H_L	latent heat of water evaporation, erg/mol
	heat of reaction, erg/mol
H_r	
h_s	heat transfer coefficient around droplet, erg/cm ² sec K
h_w	heat transfer coefficient at reactor wall, erg/cm ² sec K
I	nucleation rate or particle current in volume space,
	molecules/cm ³ sec
i*	number of monomer units in particle of critical size,
	dimensionless
i	number of monomer units in particle, dimensionless
J	particle flux, number/cm ² sec
J_m	molecular flux, moles/cm ² sec
$\overset{\scriptscriptstyle{m}}{K}$ or $K_{\rm th}$	thermophoretic coefficient, dimensionless
k	thermal conductivity, erg/cm sec K
K'	volume compressibility coefficient
k*	
	number of monomers in critical-size particle, dimensionless
k_1	first-order reaction rate constant, 1/sec
k_B	Boltzmann's constant, erg/molecule, K
K_{C}	coagulation coefficient in continuum regime, cm ³ /sec
$K_{\rm eq}$	equilibrium constant, dimensionless
K_F	coagulation coefficient in free molecule regime, cm ^{5/2} /sec
k_g	mass transfer coefficient, cm/sec
k_H°	Hall-Petch intensity parameter, units vary with definition
п	[see Equation (9.14)]
k_L	first-order reaction rate constant in particle, 1/sec
k_m	vapor mass transfer coefficient for laminar tube flow
Kn	Knudsen number, dimensionless
k_o	pre-exponential constant, cm/sec
k_p	thermal conductivity of particle
•	

xxiv NOMENCLATURE

k_s	surface reaction rate constant, cm/sec
K_T	turbulent coagulation coefficient, cm ² /sec
L	dimension of system, cross section of flow, characteristic
	length, substrate diameter, tube length, thickness of
	coating, or thickness of concentration boundary layer, cm
L_f	latent heat of fusion, erg/mol
$\stackrel{L_{v}}{M}$	latent heat of vaporization, erg/g or erg/mol
M	molecular weight, g/mole
m'	exponent that depends on sintering mechanism,
26(1)	dimensionless
$M(d_p)$	cumulative mass distribution function with respect to diameter, g/cm ³
$m(d_p)$	continuous mass distribution function with respect to
$m(\alpha_p)$	diameter, g/cm ⁴
M_0, M_1, M_2	moments of particle size distribution [see Equation (2.16)]
M_1	molecular weight, g/mole
m_1	mass of a molecule or atom, g
m_d	mass concentration of solvent at droplet surface, g/cm ³
m_g	mass concentration of solvent far from particle, g/cm ³
M_i^g	mass of particles within an interval, g
$M_i(d_{pi})$	discrete mass size distribution [see Equation (2.6)]
M_j	jth moment of distribution [see Equation (2.16)]
M_m	atomic weight of depositing species, g/mole
m_m	solution molality
m_p^m	particle mass, g
M_s^p	solute molecular weight, g/mole
M_s'	saturation magnetization, emu/g
M_{∞}^{3}	total mass concentration, g/cm ³
\overline{m}	average mass of a particle, g
N , N_1 , or N_2	number concentration of aggregate, number/cm ³
$N(d_p)$	cumulative number distribution function with respect to
P	diameter, number/cm ³
$n(d_p)$	continuous number distribution with respect to diameter,
P	number/cm ⁴
n(s)	particle size distribution function with respect to surface
	area, number/cm ⁵
n(v)	particle size distribution with respect to volume,
	number/cm ⁶
n, n_1, n_g	atomic or molecular concentration, molecules/cm ³
n_{1s}	reactant concentration in gas phase at particle surface,
	molecules/cm ³
$N_{\!\scriptscriptstyle\mathcal{A}}$	Avogadro's number, moles/molecule
$N_{\mathcal{A}} \ N_{f} \ N_{i}$	number of primary particles, dimensionless
N_i	number of particles in an interval in an agglomerate,
	dimensionless

n_i	particle concentration for discrete size i , number/cm ³
$N_i(d_{pi})$	number discrete size distribution [see Equation (2.6)]
$n_{\rm in}$	particle concentration entering bend, number/cm ³
	lognormal distribution, number/cm ⁴
n_l	particle concentration exiting bend, number/cm ³
n _{out}	
N_o	initial or inlet particle concentration, number/cm ³
n_p	number of primary particles in an aggregate, dimensionless
n_s	saturation concentration of monomer, molecules/cm ³
Nu _M	Nusselt number for mass transport, dimensionless
n_w	vapor concentration at reactor wall, molecules/cm ³
N_{∞}	total particle or aggregate concentration, number/cm ³
	gas pressure, dyne/cm ² or cm Hg
p	
p_1	partial pressure of species 1, dyne/cm ²
p_{1s}	reactant partial pressure at particle surface, dyne/cm ²
P_d	aerosol penetration, dimensionless
p_d	vapor or partial pressure at particle surface, dyne/cm ²
p_{ds}	solvent vapor pressure at droplet surface, dyne/cm ²
Pe	Peclet number, dimensionless
p_e	equilibrium vapor pressure over flat surface, dyne/cm ²
p_i	partial pressure of species i corresponding to complete
Pi	evaporation, dyne/cm ²
p_o	total pressure at reference conditions, dyne/cm ²
Pr	Prandtl number, dimensionless
	reactant partial pressure outside concentration boundary,
p_r	dyne/cm ²
p_s	vapor pressure at droplet surface at T_s , dyne/cm ²
	vapor pressure for pure solvent, dyne/cm ²
P _{sat}	equilibrium water vapor pressure at T_a , dyne/cm ²
p_s	
p_{∞}	partial pressure of solvent far from droplet, dyne/cm ²
Q	aerosol or gas flow rate, cm ³ /sec
q	number of charges on a particle
q_{rms}	rms charge on a particle
r	radial coordinate, cm
R, R_G, R_g	gas constant, cm ³ atm/mol K
r_1 or r_2	monomer radius or radius of curvature, cm
R_a	characteristic length of aggregate, cm
R_c	collision radius, cm
Re	Reynolds number, dimensionless
Re_j	jet Reynolds number, dimensionless
Re _L	Reynolds number based on length L , dimensionless
	Reynolds number based on particle diameter,
Re_p	dimensionless
n.	
Re_t	tube Reynolds number, dimensionless
r_i, r_j	particle radius, cm
R_p	droplet or particle radius, cm

xxvi NOMENCLATURE

$r_p R_r$	radius of primary particle, cm
R_r	reaction rate, molecules/cm ³ sec
r_s	surface reaction rate, molecules/cm ² sec
R_t	tube radius, cm
r_v	rate of reaction per unit volume, moles/cm ³ sec
S	saturation ratio, dimensionless
S	stopping distance, cm
S	surface area of a particle, cm ²
S*	critical saturation ratio, dimensionless
S_1 or S_2	surface area, cm ²
Sc	Schmidt number, dimensionless
Sh	Sherwood number, dimensionless
St	Stokes number, dimensionless
T	temperature, K or °C
ť	time, sec
T_{c}	Curie temperature, K
T_d	droplet temperature, K or °C
T_c T_d T_e T_g T_o	temperature at entrance or far from surface, K or °C
T_{σ}	gas temperature at entrance or far from surface, K or °C
$\mathring{T_a}$	reference temperature for gas above substrate or inlet
	temperature, K
T_{n}	temperature of particle, K or °C
T_{pre}	preheater temperature, K or °C
$T_{s}^{\rho,\sigma}$	droplet temperature, K or °C
$T_{ ho}$ $T_{ m pre}$ T_s $T_{ m w}$ $T_{ m \infty}$	temperature at surface or wall, K or °C
T_{∞}	temperature far from particle, K or °C
U	average gas velocity, cm/sec
и	particle velocity, cm/sec
U_o or u_e	velocity of gas far from surface (free-stream velocity),
	cm/sec
V	total aerosol volume, cm ³ /cm ³
V_1 and V_2	volumes of particles and coating on particle, respectively,
-	cm ³
v and v'	particle volume, cm ³
v	gas velocity vector, cm/sec
ν^*	critical particle size, cm
v_0	monomer volume, cm ³
v_1	molecular volume, cm ³
v_a	atomic volume, cm ³
$ ilde{V_{ m dif}}$	diffusion velocity, cm/sec
V_e	electrical migration velocity, cm/sec
v_{g}	geometric mean volume, cm ³
v_i and v_i	particle volume, cm ³
\dot{V}_{M}	particle deposition velocity, cm ³
5.5	

77.0	values of denosited enesies am3
ν_m	volume of deposited species, cm ³
ν_p	volume of a primary particle, cm ³
V_s	sedimentation settling velocity, cm
$V_p \ V_s \ V_\iota$	total or terminal velocity, cm/sec
$V_{ m th}$	thermophoretic velocity, cm/sec
v_{tr}	thermophoretic velocity in radial direction, cm/sec
v_{tz}	thermophoretic velocity in z direction, cm/sec
	gas velocity in x direction, cm/sec
$\frac{U_X}{\overline{U}}$	average particle volume, cm ³
$\overline{\nu}$	variable of integration, cm ³
W	spread of the particle size distribution, dimensionless
W_{ij}	factor for coagulation, dimensionless
$X^{''}$	residence time, dimensionless
x	reactor axial coordinate, cm
x_A	mole fraction in liquid, dimensionless
$x_{\rm rms}$	root mean square diffusion distance, cm
x_s	mole fraction of solvent, dimensionless
	concentrations of particles of size i , dimensionless
Y_{ν}	concentrations of particles in sections k , dimensionless
$egin{array}{l} y_i \ Y_k \ y_w \ Z \ \overline{Z} \end{array}$	water vapor mole fraction in air, dimensionless
7.	number of charges per particle, dimensionless
7	average number of charges per particle, dimensionless
z	coordinate in axial direction, cm
z_i	number of charges on particle, dimensionless
$Z_{s,\mathrm{max}}$	maximum number of acquired charges, dimensionless

GREEK

α	thermophoretic coefficient, dimensionless
α_c	ratio of characteristic times for collision and fusion,
-	dimensionless
$lpha_g$	thermal diffusivity of gas, cm ² /sec
α_p	thermal diffusivity of particle, cm ² /sec
α_s^r	sticking coefficient, dimensionless
β_C	collision frequency in continuum regime, cm ³ /sec
$eta_{ ext{Ch}}$	collision frequency function for charged particles, cm ³ /sec
β_F	collision frequency in free-molecule regime, cm ³ /sec
β_{FA}	coagulation frequency function of agglomerates, cm ³ /sec
$\beta_{i,j}$	collision frequency function, cm ³ /sec
β_T	collision frequency for turbulent coagulation, cm ³ /sec
$\beta(v,v')$	collision frequency of particles of size v and v' , cm ³ /sec
γ	surface tension, erg/cm ²
γ_A	activity coefficient, dimensionless

xxviii NOMENCLATURE

$\gamma_{i,j}$ dimensionless function activity coefficient of solution, dimensionless γ_{sol} and γ_c activity coefficient of solute, dimensionless ΔH_{vap} enthalpy of evaporation of precursor, erg/mole K delta function, dimensionless crust thickness, cm ε dielectric constant, dimensionless ε_c rate of gas molecule collisions, $1/\sec$ ε_d rate of energy dissipation, cm²/sec² total number of collisions with particle surface per unitime, number/sec prefactor, dimensionless η_r particle volume, dimensionless η_r size of smallest eddies, cm θ reaction time, dimensionless θ_1 characteristic time for reaction, dimensionless θ_2 numerical coefficient, dimensionless θ_2 numerical coefficient (or deposition velocity) by turbulent diffusion, cm/sec λ gas mean free path, cm heat of phase transition, erg/cm³ gas viscosity, g/cm sec	t
γ_s activity coefficient of solution, dimensionless activity coefficient of solute, dimensionless $\lambda_{\rm sol}$ and γ_c enthalpy of evaporation of precursor, erg/mole K delta function, dimensionless crust thickness, cm ε dielectric constant, dimensionless ε_c rate of gas molecule collisions, $1/\sec$ rate of energy dissipation, cm ² /sec ² total number of collisions with particle surface per unit time, number/sec prefactor, dimensionless particle volume, dimensionless η_r particle volume, dimensionless size of smallest eddies, cm θ reaction time, dimensionless θ_1 characteristic time for reaction, dimensionless θ_2 numerical coefficient, dimensionless ε temperature, dimensionless ε mass transfer coefficient (or deposition velocity) by turbulent diffusion, cm/sec ε gas mean free path, cm heat of phase transition, erg/cm ³	t
$\begin{array}{lll} \Delta H_{\mathrm{vap}} & & & & & & \\ \Delta H_{\mathrm{vap}} & & & & & & \\ \Delta elta function, dimensionless \\ \delta_c & & & & \\ \varepsilon & & & & \\ \varepsilon & & & & \\ dielectric constant, dimensionless \\ \varepsilon_c & & & \\ \mathrm{rate} \ of \ gas \ molecule \ collisions, \ 1/sec \\ \varepsilon_d & & & \\ \mathrm{rate} \ of \ energy \ dissipation, \ cm^2/sec^2 \\ \epsilon & & & \\ \mathrm{total} \ number \ of \ collisions \ with \ particle \ surface \ per \ unit \ time, \ number/sec \\ \epsilon_p & & & \\ \mathrm{prefactor, \ dimensionless} \\ \eta_r & & & \\ \mathrm{particle} \ volume, \ dimensionless \\ \eta_r & & \\ \mathrm{size} \ of \ smallest \ eddies, \ cm \\ \theta & & & \\ \mathrm{reaction} \ time, \ dimensionless \\ \theta_1 & & \\ \mathrm{characteristic} \ time \ for \ reaction, \ dimensionless \\ \theta_2 & & \\ \mathrm{numerical} \ coefficient, \ dimensionless \\ \theta_2 & & \\ \mathrm{numerical} \ coefficient, \ dimensionless \\ \kappa & & \\ \mathrm{mass} \ transfer \ coefficient \ (or \ deposition \ velocity) \ by \\ & & \\ \mathrm{turbulent} \ diffusion, \ cm/sec \\ \lambda & & \\ \mathrm{gas} \ mean \ free \ path, \ cm \\ \lambda_p & & \\ \mathrm{heat} \ of \ phase \ transition, \ erg/cm^3 \\ \end{array}$	t
$\begin{array}{lll} \Delta H_{\mathrm{vap}} & \mathrm{enthalpy\ of\ evaporation\ of\ precursor,\ erg/mole\ K} \\ \delta & \mathrm{delta\ function,\ dimensionless} \\ \delta_c & \mathrm{crust\ thickness,\ cm} \\ \varepsilon & \mathrm{dielectric\ constant,\ dimensionless} \\ \varepsilon_c & \mathrm{rate\ of\ gas\ molecule\ collisions,\ 1/sec} \\ \varepsilon_d & \mathrm{rate\ of\ energy\ dissipation,\ cm^2/sec^2} \\ \epsilon & \mathrm{total\ number\ of\ collisions\ with\ particle\ surface\ per\ unitime,\ number/sec} \\ \epsilon_p & \mathrm{prefactor,\ dimensionless} \\ \eta & \mathrm{particle\ volume,\ dimensionless} \\ \eta_r & \mathrm{size\ of\ smallest\ eddies,\ cm} \\ \theta & \mathrm{reaction\ time,\ dimensionless} \\ \theta_1 & \mathrm{characteristic\ time\ for\ reaction,\ dimensionless} \\ \theta_2 & \mathrm{numerical\ coefficient,\ dimensionless} \\ \theta^2 & \mathrm{temperature,\ dimensionless} \\ \kappa & \mathrm{mass\ transfer\ coefficient\ (or\ deposition\ velocity)\ by} \\ & \mathrm{turbulent\ diffusion,\ cm/sec} \\ \lambda & \mathrm{gas\ mean\ free\ path,\ cm} \\ \lambda_p & \mathrm{heat\ of\ phase\ transition,\ erg/cm^3} \\ \end{array}$	t
$\begin{array}{lll} \delta & \text{delta function, dimensionless} \\ \delta_c & \text{crust thickness, cm} \\ \varepsilon & \text{dielectric constant, dimensionless} \\ \varepsilon_c & \text{rate of gas molecule collisions, 1/sec} \\ \varepsilon_d & \text{rate of energy dissipation, cm}^2/\text{sec}^2 \\ \epsilon & \text{total number of collisions with particle surface per unitime, number/sec} \\ \epsilon_p & \text{prefactor, dimensionless} \\ \eta & \text{particle volume, dimensionless} \\ \eta_r & \text{size of smallest eddies, cm} \\ \theta & \text{reaction time, dimensionless} \\ \theta_1 & \text{characteristic time for reaction, dimensionless} \\ \theta_2 & \text{numerical coefficient, dimensionless} \\ \theta^* & \text{temperature, dimensionless} \\ \kappa & \text{mass transfer coefficient (or deposition velocity) by} \\ & \text{turbulent diffusion, cm/sec} \\ \lambda & \text{gas mean free path, cm} \\ \lambda_p & \text{heat of phase transition, erg/cm}^3 \\ \end{array}$	t
dielectric constant, dimensionless ε_c rate of gas molecule collisions, 1/sec ε_d rate of energy dissipation, cm²/sec² total number of collisions with particle surface per unit time, number/sec ε_p prefactor, dimensionless η_r particle volume, dimensionless η_r size of smallest eddies, cm reaction time, dimensionless θ_1 characteristic time for reaction, dimensionless θ_2 numerical coefficient, dimensionless θ^* temperature, dimensionless κ mass transfer coefficient (or deposition velocity) by turbulent diffusion, cm/sec λ gas mean free path, cm λ_p heat of phase transition, erg/cm³	t
dielectric constant, dimensionless ε_c rate of gas molecule collisions, 1/sec ε_d rate of energy dissipation, cm²/sec² total number of collisions with particle surface per unit time, number/sec ε_p prefactor, dimensionless η_r particle volume, dimensionless η_r size of smallest eddies, cm reaction time, dimensionless θ_1 characteristic time for reaction, dimensionless θ_2 numerical coefficient, dimensionless θ^* temperature, dimensionless κ mass transfer coefficient (or deposition velocity) by turbulent diffusion, cm/sec λ gas mean free path, cm λ_p heat of phase transition, erg/cm³	t
rate of gas molecule collisions, $1/\sec$ ε_d rate of energy dissipation, cm^2/\sec^2 ε total number of collisions with particle surface per unit time, number/sec ε_p prefactor, dimensionless η_r particle volume, dimensionless η_r size of smallest eddies, cm θ reaction time, dimensionless θ_1 characteristic time for reaction, dimensionless θ_2 numerical coefficient, dimensionless θ^* temperature, dimensionless κ mass transfer coefficient (or deposition velocity) by turbulent diffusion, cm/sec λ gas mean free path, cm λ_p heat of phase transition, erg/cm ³	t
rate of energy dissipation, cm ² /sec ² total number of collisions with particle surface per unit time, number/sec prefactor, dimensionless particle volume, dimensionless particle volume, dimensionless reaction time, dimensionless characteristic time for reaction, dimensionless numerical coefficient, dimensionless θ_1 characteristic time for reaction, dimensionless θ_2 numerical coefficient, dimensionless θ_3 temperature, dimensionless θ_4 mass transfer coefficient (or deposition velocity) by turbulent diffusion, cm/sec θ_4 gas mean free path, cm heat of phase transition, erg/cm ³	t
total number of collisions with particle surface per unitime, number/sec ρ prefactor, dimensionless η particle volume, dimensionless η, size of smallest eddies, cm θ reaction time, dimensionless θ ₁ characteristic time for reaction, dimensionless η ₂ numerical coefficient, dimensionless θ* temperature, dimensionless κ mass transfer coefficient (or deposition velocity) by turbulent diffusion, cm/sec λ gas mean free path, cm λ _p heat of phase transition, erg/cm ³	t
time, number/sec ϵ_p prefactor, dimensionless η particle volume, dimensionless η_r size of smallest eddies, cm θ reaction time, dimensionless θ_1 characteristic time for reaction, dimensionless θ_2 numerical coefficient, dimensionless θ^* temperature, dimensionless κ mass transfer coefficient (or deposition velocity) by turbulent diffusion, cm/sec λ gas mean free path, cm λ_p heat of phase transition, erg/cm ³	
η particle volume, dimensionless η_r size of smallest eddies, cm θ reaction time, dimensionless characteristic time for reaction, dimensionless θ_2 numerical coefficient, dimensionless θ^* temperature, dimensionless κ mass transfer coefficient (or deposition velocity) by turbulent diffusion, cm/sec λ gas mean free path, cm λ_p heat of phase transition, erg/cm ³	
η particle volume, dimensionless η_r size of smallest eddies, cm θ reaction time, dimensionless θ_1 characteristic time for reaction, dimensionless θ_2 numerical coefficient, dimensionless θ^* temperature, dimensionless κ mass transfer coefficient (or deposition velocity) by turbulent diffusion, cm/sec λ gas mean free path, cm λ_p heat of phase transition, erg/cm ³	
$\begin{array}{ll} \theta & \text{reaction time, dimensionless} \\ \theta_1 & \text{characteristic time for reaction, dimensionless} \\ \theta_2 & \text{numerical coefficient, dimensionless} \\ \theta^* & \text{temperature, dimensionless} \\ \kappa & \text{mass transfer coefficient (or deposition velocity) by} \\ & \text{turbulent diffusion, cm/sec} \\ \lambda & \text{gas mean free path, cm} \\ \lambda_p & \text{heat of phase transition, erg/cm}^3 \end{array}$	
eta_1 characteristic time for reaction, dimensionless numerical coefficient, dimensionless eta^* temperature, dimensionless mass transfer coefficient (or deposition velocity) by turbulent diffusion, cm/sec λ gas mean free path, cm λ_p heat of phase transition, erg/cm ³	
θ_2 numerical coefficient, dimensionless θ^* temperature, dimensionless mass transfer coefficient (or deposition velocity) by turbulent diffusion, cm/sec λ gas mean free path, cm λ_p heat of phase transition, erg/cm ³	
κ mass transfer coefficient (or deposition velocity) by turbulent diffusion, cm/sec λ gas mean free path, cm λ_p heat of phase transition, erg/cm ³	
κ mass transfer coefficient (or deposition velocity) by turbulent diffusion, cm/sec λ gas mean free path, cm λ_p heat of phase transition, erg/cm ³	
turbulent diffusion, cm/sec λ gas mean free path, cm λ_p heat of phase transition, erg/cm ³	
λ gas mean free path, cm heat of phase transition, erg/cm ³	
λ_p heat of phase transition, erg/cm ³	
P = -	
ν kinematic viscosity of gas, cm ² /sec	
ρ density, g/cm ³	
ρ_1 droplet density, g/cm ³	
ρ_b molar density, mole/cm ³	
ρ_f gas density, g/cm ³	
ρ_L density of pure water, g/cm ³	
$\rho_{\rm liq}$ density of liquid, g/cm ³	
ρ_p particle density, g/cm ³	
ρ_s solute density, g/cm ³	
$\rho_{\rm sol}$ density of solid, g/cm ³	
σ surface tension, erg/cm ²	
σ_d hard-sphere molecular diameter, cm	
$\sigma_{\rm g}$ or $\sigma_{\rm gs}$ geometric standard deviation of size distribution,	
dimensionless	
σ_s surface energy of TiO ₂ , dyne/cm or erg/cm ²	
$\sigma_{\rm ys}$ yield strength, dyne/cm ²	
$ au_{\rm as}$ characteristic time for reaction in particle when ash	
diffusion controls, sec	
$ au_C$ characteristic time for particle collisions, sec	
. C	
$ au_{\rm CC}$ characteristic time for coagulation in continuum regin	ne,

_	characteristic time for coagulation in free-molecule regime,
$ au_{CF}$	sec
7	characteristic time for diffusion in particles, sec
$ au_D$	characteristic time for concentration profile to achieve
$ au_{ ext{dg}}$	steady state, sec
τ_e	evaporation time, sec
$ au_f$	characteristic time for sintering or fusion, sec
$ au_{fs}$	coagulation parameter, dimensionless
$ au_{ ext{GC}}$	characteristic time for particle growth in continuum regime, sec
$ au_{GF}$	characteristic time for particle growth in free-molecule
Gr	regime, sec
$ au_{ m gs}$	characteristic time for reaction in particle when gas phase transport controls, sec
_	characteristic time for particle growth by surface reaction,
$ au_{GSR}$	sec
$ au_{GV}$	characteristic time for particle growth by volume reaction,
_	sec
$ au_L$	characteristic time for diffusion in coating, sec
$ au_p$	characteristic time for particle formation, sec
$ au_{ m pd}$	time between particle collisions with same region on surface, sec
$ au_r$	reactor residence time, sec
$ au_{ ext{rs}}$	characteristic time for reaction in particle when chemical
-	reaction controls, sec
$ au_S$	time needed for an aerosol to reach a self-preserving
J	distribution, sec
$ au_{_{\mathcal{S}}}$	settling time, sec
$ au_{sat}$	characteristic time to saturate gas with vapor from
sat	evaporating droplets, sec
$ au_{SC}$	time needed to reach self-preserving distribution in
30	continuum regime, sec
$ au_{SF}$	time needed to reach self-preserving distribution in free-
31	molecule regime, sec
$ au_{m}$	characteristic time for heat transfer in gas phase around a
$ au_{\mathrm{Tg}}$	particle, sec
$ au_{th}$	time for particle transport by thermophoresis, sec
$ au_{Tp}$	characteristic time for heat transfer in solid particle or
	droplet, sec
ϕ .	water osmotic coefficient
X	dynamic shape factor, dimensionless
ψ	normalized charge = $q/q_{\rm rms}$
$\psi(\eta)$	self-preserving size distribution, dimensionless

NOMENCI ATURE

ACRONYMS

YYY

AACVD aerosol-assisted chemical vapor deposition

AES Auger electron spectroscopy
BET Brauner-Emmett-Teller

CSTAR continuous stirred tank aerosol reactor

CVD chemical vapor deposition
DTA differential thermal analysis
FTIR Fourier transform infrared
GDE general dynamic equation
LFAR laminar-flow aerosol reactor
MLCC multilayer ceramic capacitor
NMR nuclear magnetic resonance

PCB printed circuit board PE plasma enhanced

PFAR plug-flow aerosol reactor PSD particle size distribution

RF radio frequency

SEM scanning electron microscope

SPSD self-preserving size distribution, dimensionless

SSA specific surface area

TEM transmission electron microscope

TGA thermogravimetric analysis TMEDA tetramethylethylenediamine

UHV ultrahigh vacuum

AEROSOL PROCESSING OF MATERIALS