SULFUR DIOXIDE REMOVAL FROM WASTE GASES

SECOND EDITION

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A.V. Slack G.A. Hollinden

NOYES DATA CORPORATION

Park Ridge, New Jersey

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1975

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PREFACE TO SECOND EDITION

Almost all of that which was said nearly four years ago in the preface to the first edition of this book applies equally well today. Sulfur oxide removal from waste gases is still a problem of major concern, and the technology is still changing very rapidly.

There have been several major changes and developments in the field. Some of the methods described in the first edition are omitted from the present one because they have been casualties of the competitive situation. Others that were mentioned only sketchily or not at all have come to the fore and now occupy significant positions.

Probably the main development is the rapid increase in the number of full-scale scrubber installations, of which there were very few in 1971. This is particularly true in Vapan where regulations are fast becoming more stringent.

A better understanding of the basic chemical and physical factors in SO₂ absorption has also been developed over the past few years, but there is still some distance to go.

The authors appreciate the many indirect contributions by development, engineering, and operating people in the field. Since most of the work is not yet published, a book like the present one could not be written without such contributions.

A.V. Slack

SAS Corporation, Sheffield, Alabama March 30, 1975

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TVA Office of Power, Chattanooga, Tennessee March 30, 1975

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PREFACE TO FIRST EDITION

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This book is not a reference work, but rather a status report on a technology that is being developed under forced draft. Sulfur oxide removal from waste gases is not a new problem. Smelter operators for more than a century have coped with the unwanted fumes produced by oxidation of the sulfur in the ore during roasting. Power plants, refineries, sulfuric acid plants, and Claus sulfur plants have perhaps a more recent history, but even for these industries the problem goes back for half a century or more. It is only in the last few years, however, that sulfur oxide removal has become a major research and development effort. Pressures to improve the environment have made it necessary to greatly expand activity in the field, in somewhat of crash program.

Presently there are hundreds of organizations around the world giving attention to the problem, in a general way or in developing removal methods and evaluating them for use. Processes are in all stages of development, from the idea stage to plant trials. Numerous and widely differing chemical paths are being explored, and process flowsheets ranging from very simple to very complicated are being developed.

In this context, a reference book does not seem appropriate because the technology is changing too fast. There is no basic body of information that could be presented, because the various processes under study not only cut across much of the entire field of sulfur chemistry but also involve many of the chemical engineering unit operations. Moreover, the nitrogen oxide and particulate matter problems cannot be dissociated from that of removing sulfur oxides.

Because of this, the book is intended to serve only as an overview of the current development situation, written from the viewpoint of one who is involved both in process development and in the selection of processes for use by a major utility. An effort has been made to list all the major processes (and as many of the minor ones as feasible), summarize the basic chemistry of each, analyze the engineering problems, identify advantages and disadvantages, evaluate the effect of major economic factors, and make a guess as to how each process compares with the others.

Preface

This is obviously an ambitious undertaking and one that cannot be wholly accurate and well-documented; it is, however, the type of analysis that must be carried out by those responsible for fitting plants around the world with sulfur oxide removal facilities. No process yet proposed is a completely satisfactory solution to the problem but many have promise; at some point it is necessary to set them all side by side and see which looks best, even though in a preliminary and incomplete way. This book represents such a beginning.

The information on which the analyses presented herein are based comes from many sources. Some of it is readily available as published material, but the bulk is from two sources: unpublished reports and published documents not widely distributed or publicized, and discussions with other workers in the field. There is a large amount of such information that is nonproprietary but not widely known. Of particular benefit have been visits to research organizations in all the countries of Europe and Asia (with the exception of the USSR) that have active programs in the field.

It should be emphasized that the analysis presented is for the current situation only. With the fast moving pace in the field, such an overview made a year from now may be quite different. New processes will be announced, older ones will change in status, and commercial units now being constructed will add the final proof to some processes. If this book has any value, it is in getting everything together to serve as a starting point in analyzing sulfur oxide removal technology with adjustments to be expected as the technology matures. In spite of best efforts, errors no doubt have crept into the descriptions and evaluations of some of the processes. Hopefully, these will be few. in the Farris action you in the

The list of acknowledgements due is too long to include. The main contribution have come from the large number of research and development people with whole I have discussed the problems in developing an effective and economical sulfur oxide removal technology (and whose indulgence I invite where my evaluations differ from theirshan Several of my coworkers have reviewed and corrected the text, and my secretary, Mrs. Juanita Hargett, carried out the mechanics of the project quite efficiently, hinally, without the patience and forbearance of my wife, this project would have failed in the early stages.

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THE PROBLEM

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Of the several air pollutants that plague the world, sulfur oxides (SO₂, sulfur dioxide, and SO₃, sulfur trioxide) have received special attention—more so than any other polluting material except perhaps particulate matter (dust). The severity of the problem—effects on people, animals, and vegetation—is a matter on which there are varying opinions and will not be debated here. A more important consideration for the present discussion is that control of sulfur oxide emission has come to be regarded as a matter of great importance both by governmental regulatory agencies and the general public.

A major concern is the very large amount of sulfur oxides emitted. Various estimates have been made; the general consensus is that the U.S. emission in 1970 was over 35,000,000 tons. Similar data for other parts of the world are not readily available but it is known that emission is heavy in all highly industrialized countries, particularly in areas such as the Ruhr Valley in Germany and the Tokyo area in Japan. Emission is also increasing at a rapid rate. The potential emission for the year 2000 has been estimated to be over three times that for 1970.

SOURCES

Practically all SO₂ (and SO₃) comes from combustion of naturally occurring sulfur compounds, either as elemental sulfur or as a constituent of an ore or a fossil carbonaceous material. Examples are organic sulfur compounds in coal and petroleum, pyrites (FeS₂) both as such and as a constituent of coal, hydrogen sulfide (H₂S) in sour natural gas, and metal sulfide ores. The reasons for oxidizing these materials are varied; elemental sulfur and pyrites are burned to make SO₂ in the process of producing sulfuric acid, metal ores are roasted to burn away the sulfur in recovering the elemental metal (e.g., zinc, copper, and lead), the H₂S is separated from natural gas and part of it burned to SO₂ as one step in conversion to elemental sulfur, and coal and oil are burned for heating and for power production.

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In most cases the overall process includes a unit for recovering SO₂ from the gas stream emitted, either because sulfur or sulfuric acid is the primary product or because the SO₂ concentration in the gas is high enough to make recovery as a by-product economical. (However, there is still a pollution problem because recovery is never complete.) The burning of carbonaceous fuel is a major exception; the exit gases from heat recovery units are so dilute in SO₂ that no effort normally is made to remove the pollutant from the stack gas. The relative contributions of the various sources to the SO₂ emission problem are given in Table 1.1.

TABLE 1.1: WORLD-WIDE SO2 EMISSION

Sources	Emissions, 10	s tons per yr
Cos1	102	
Petroleum	28	
Monferrous smelting	16	* + 7% V
Industrial	_6	
Total men-generated SO2:	1	152
ang tanggan gita	ja	
Mexime 4 years again	60	
Lend B28 (802 equivalent)	140	
Todel metural sources oxidized to SO2:	-	200
Sulfur in SO _h from sea salt (SO ₂ equivalent)	- 1	88
Total world-wide:		440

It is clear from these data that coal is the main culprit, contributing almost 70% of the total man-made emission. Moreover, other data show that production of power from coal and oil accounts for almost half the man-made total.

Power Production from Coal

Since the problem thus is centered in power plants and mainly in coal-burning power plants, the future of coal-based power becomes a major consideration. With the exception of oil, the other major competitors to coal as an energy source, hydroelectric and nuclear, do not produce SO₂ and therefore one way of reducing the problem is to adopt such alternate sources to a greater degree. The potential for hydroelectric is well nigh exhausted and further significant growth is not expected.

Nuclear, however, is increasing rapidly (Figure 1.1). It is estimated that by 2000 over half of the electrical power will be generated by the nuclear method, with coal (plus other fossil fuel) declining to about 30%. Nevertheless, overall power production is expected to increase so much by 2000 that fossil fuels, while losing percentagewise, will increase in total usage by almost twofold over current consumption. Hence the severity of the SO₂ problem will continue to grow.

FIGURE 1.1: PROJECTED SOURCES OF POWER IN THE U.S.

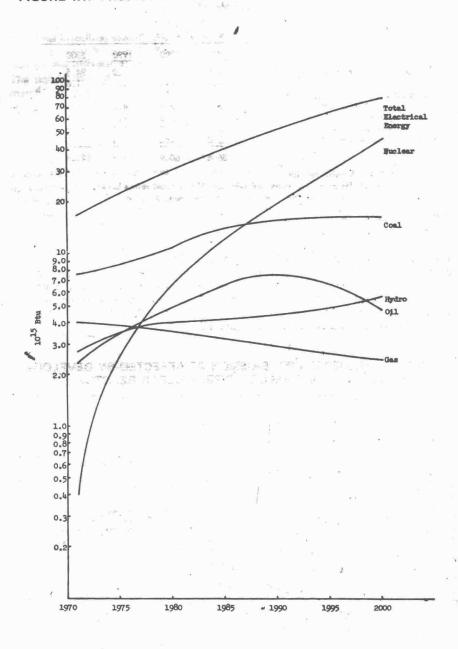


TABLE 1.2: ESTIMATED SULFUR DIOXIDE EMISSION IN U.S. WITHOUT ABATEMENT

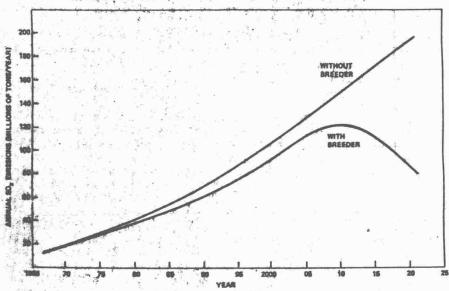
	And the second second	Annual	Emission	of Sulfur	Dioxide	(millions of	tons)
			1970	1980	1990	2000	
	Power plant operation (soal and oil)*	100	20.0	41.1	62.0	94.5	
	Other combustion of capl	104	4.8	4.0	3.1	1.6	
	Combustion of petroleum products						19
ŕ	(excluding power plant oil)	9	3.4	3.9 >	4.3	5.1	
	Smelting of metallic ores		4.0	5,3	7.1	9.6	
,	Petroleum refinery operation		2.4	4.0	6.5	10.5	
	Miscellaneous sources**	114	2.0	2,6	3.4	4.5	
	Total		36.6	60.9	86.4	125.8	

^{*}With breeder reactor.

February 1970 estimates by National Air Pollution Control Administration, excluding transportation.

The changing distribution between sources is given in Table 1.2 above. It should be noted that even the major increase in this estimate may be conservative as it assumes development and wide adoption of the breeder reactor, which is generally considered essential for major conversion to nuclear power as an energy source. Potential power plant emission of SO₂ in the U.S. with and without the breeder reactor are compared in Figure 1.2.

FIGURE 12: PROJECTED SO₂ EMISSION AS AFFECTED BY DEVELOPMENT OF THE BREEDER TYPE NUCLEAR REACTOR



Source: NAPCA, February 1970

^{**} Includes cake processing, sulfuric acid plants, coal refuse banks, refuse incineration, and pulp and paper manufacturing.

Another factor will also aggravate the situation. In the interest of economy, the evolutionary trend has been to larger and larger power production units and to greater production (by multiple units) at individual sites. Boiler size has reached the 1100 to 1300 Mw (megawatt; equals 1000 kilowatts or 1,000,000 watts) range and central stations producing over 2500 Mw are in operation; for a typical coal of the high-sulfur type, such stations emit over 1,500 tons of SO₂ per day. The significance of this is that damage from a pollutant such as SO₂ depends mainly on its concentration at ground level, and this depends much more on the amount emitted at a particular site than on the total amount over the entire country.

Increase in overall amount mainly produces more sites at which emission becomes a problem; larger central stations, however, make the individual problem more severe and intensify the need for remedial action. The amount of \$0₂ emitted at a particular site depends, of course, on the sulfur content of the coal burned. Coals vary widely in this respect; the bituminous type generally used in power plants is highest in sulfur, although there is much bituminous coal of low sulfur content. Subbituminous, lignite, and anthracite generally contain less than 1% sulfur. The situation in regard to coal type and geographical location of reserves (in the U.S.) is summarized in Table 1.3. The totals given are for the total coal in the United States of the type listed. States with small amounts are not listed and for some of the states listed, the amount is insignificant as indicated by a dash.

TABLE 1.3: SULFUR CONTENT OF U.S. COAL RESERVES*

1 to 398	>3%
	-
1 1.00	
21	119
16	19
5	32
7	
	79
10	38
50	N. E.
45	4
43" 23	
_	-
191	322
40-40	
-	
× 1	-0
	in 🕶 rasing
	21 16 5 7

(continued)

TABLE 1.3: (continued)

Coal Type and Location	Billion Tons	of Coal with Indica	ated Sulfur Content
	<u><1%</u>	1 to 3%	>3%
Lignite Montana North Dakota	84 319		
	otal 406	41	
Anthracite Pennsylvania	12		_
To	otal 15	JEL IN. T	
Grand To	المستور أراز المراز المعارف	234	322
Per c	ent 65	314 L REGIO	and the same

^{*} Orly major reserves are included.

From this it is evident that there is plenty of low sulfur coal (defined as coal of less than 1% sulfur content) in the ground. Unfortunately, most of it is of the type not usually burned in power plants. Moreover, by far the greatest tonnages are in the western states where population density is low; in the eastern areas, where power consumption is high and where most of the power is produced, only a relatively small area (West Virginia and eastern Kentucky) has significant low sulfur coal reserves.

The nonbituminous, low sulfur types can be burned in power plants, of course, but normally are not because of factors such as low heating value, difficulty in getting good combustion, and location. Recent advancements have reduced the boiler design problem, but the other drawbacks still remain.

The composition of the combustion gases evolved in the burning of coal is an important factor in pollution abatement, not only because of pollutant concentrations but also because nonpollutants in the gas stream can have major effects on processes or techniques for pollutant removal. Only nitrogen (from the combustion air) passes through the removal system without effect.

Coal is such a complex and variable raw material (Table 1.4) that the combustion gas contains many compounds, both gaseous and solid. Moreover, the variability in coal composition is so great that a generally applicable analysis of the stack gas cannot be given.

The composition given in Table 1.5 is fairly typical of stack gases evolved in burning western Kentucky coal. Variations from this occur for various reasons, including composition of the coal, type of boiler, and the way in which the boiler is operated; typical effects of such factors are shown in Table 1.6.

TABLE 1.4: EXAMPLE OF COAL COMPOSITION*

1 - THE DISC T

Constituent	Percent by Weight
Volatile matter	32.9
Fixed carbon	46.4
Sulfur	3.3
Moisture	5.4
Ash · -	12.0
	100.0
H., .	4.5
N	1.3
China and the same	66.0
0	7.3
20 AND A SECTION OF ANY AND ADDRESS.	
Ash	12.0
Moisture	5.4
	100.0

^{*} Coal from western Kentucky. Coals vary so widely in composition that this example should not be regarded as typical.

TABLE 1.5: COMPOSITION OF STACK GAS EVOLVED IN BURNING COAL FROM WESTERN KENTUCKY*

Constituent	ent by Vol	ume**
Nitrogen (N2)	74.56	
Carbon diaxide (CO2)	12.55	
Oxygen (O2)	4.87	311
Water vapor (H2O)	7.76	ie.
Sulfur oxides (SO _x)		
Sulfur dioxide (SO ₂)	0.22	š .
Sulfur trioxide (SO ₃)	0.001	
Nitrogen oxides (NO _v)	0.04	
Particulate matter		
Percent by weight	0.66	-
Grains per standard cu. ft. (scf)	3.59	

^{*} Composition, percent: C, 66.0; S, 3.3; ash, 12.0; N, 1.3.

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TABLE 1.6: EFFECT OF BOILER TYPE AND SULFUR CONTENT OF COAL ON STACK GAS COMPOSITION

Boiler type	Pulverised of (horisontal, front		Сус	lone-fired	
Sulfur content of coel, \$ by wt	2.0 3.5	5.0	2.0	3-5	5.0
Flue gas composition,				D Ha	. *
% by volume Hitrogen	74.62 74.55	74.49	74.59	74.52 7	4.46
Carbon dioxide	12.57 12.55	12.54	12.57	12.55 1	2.54
Oxygen	\$.86 4.86	4.85	4.83	4.83	4.82
			M (1 1)	(continued)

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^{**} Except as indicated.