

# Fuel Cell Systems Explained

James Larminie

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#### Foreword

### By Dr Gary Acres OBE, formerly Director of Research, Johnson Matthey Plc.

A significant time generally elapses before any new technological development is fully exploited. The fuel cell, first demonstrated by Sir William Grove in 1839, has taken longer than most, despite the promise of clean and efficient power generation.

Following Bacon's pioneering work in the 1950s fuel cells were successfully developed for the American manned space programme. This success, together with a policy to commercialise space technology, led to substantial development programmes in America and Japan in the 1970 and 80s, and more recently in Europe. Despite these efforts, which resulted in considerable technical progress, fuel cell systems were seen to be "always five years away from commercial exploitation".

During the last few years of the 20<sup>th</sup> century much changed to stimulate new and expanding interest in fuel cell technology. Environmental concerns about global warming and the need to reduce CO<sub>2</sub> emissions provided the stimulus to seek ways of improving energy conversion efficiency. The motor vehicle industry, as well as seeking higher fuel efficiencies, is also required to pursue technologies capable of eliminating emissions: the ultimate goal being the zero emission car. The utility industries, following the impact of privatisation and deregulation, are seeking ways to increase their competitive position while at the same time contributing to reduced environmental emissions.

As these developments have occurred, interest in fuel cell technology has expanded. Increased numbers of people from disciplines ranging from chemistry through engineering to strategic analysis, not familiar with fuel cell technology, have needed to become involved. The need by such people for a single, comprehensive and up to date exposition of the technology and its applications has become apparent, and is amply provided for by this book.

While the fuel cell itself is the key component and an understanding of its features is essential, a practical fuel cell system requires the integration of the stack with fuel processing, heat exchange, power conditioning and control systems. The importance of each of these components and their integration is rightly emphasised in sufficient detail for the chemical and engineering disciplines to understand the system requirements of this novel technology.

Fuel cell technology has largely been the preserve of a limited group consisting primarily of electro and catalyst chemists and chemical engineers. There is a need to develop more people with a knowledge of fuel cell technology. The lack of a comprehensive review of fuel cells and their applications has been a limiting factor in the inclusion of this subject in academic undergraduate and graduate student science and engineering courses. This book, providing as it does a review of the fundamental aspects of the technology, as well as its applications, forms an ideal basis for bringing fuel cells into appropriate courses and postgraduate activities.

The first three chapters describe the operating features of a fuel cell and the underlying thermodynamics and physical factors that determine their performance. A good

understanding of these factors is essential to an appreciation of the benefits of fuel cell systems and their operating characteristics compared with conventional combustion based technology. A feature of fuel cell technology is that it gives rise to a range of five main types of system, each with its own operating parameters and applications. These are described in Chapters 4 to 6.

The preferred fuel for a fuel cell is hydrogen. While there are applications where hydrogen can be used directly, such as in space vehicles and local transport, in the foreseeable future, for other stationary and mobile applications, the choice of fuel and its conversion into hydrogen rich gas are essential features of practical systems. The range of fuels and their processing for use in fuel cell systems are described in Chapter 7. Chapters 8 and 9 describe the mechanical and electrical components that make up the complete fuel cell plant for both stationary and mobile applications.

This book offers those new to fuel cells a comprehensive, clear exposition and review to further their understanding, and also provides those familiar with the subject a convenient reference. I hope it will also contribute to a wider knowledge about, and a critical appreciation of, fuel cell systems, and thus to the widest possible application of an exciting 21st century technology that could do much to move our use of energy onto a more sustainable basis.

Gary Acres

February 2000

## Acknowledgements

The point will frequently be made in this book that fuels cells are highly interdisciplinary, involving many aspects of science and engineering. This is reflected in the number and diversity of companies that have helped with advice, information and pictures in connection with this project. The authors would like to put on record their thanks to the following companies or organisations who have made this book possible:-

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James Larminie, Oxford Brookes University, Oxford Andrew Dicks, BG Technology, Loughborough

#### **Abbreviations**

ACAlternating current

**AES** Air electrode supported **AFC** Alkaline (electrolyte) fuel cell

Area specific resistance, the resistance of 1 cm<sup>2</sup> of fuel cell. (N.B. total **ASR** 

resistance is ASR divided by area.)

**BLDC** Brushless DC (motor) **BOP** Balance of plant CFM Cubic feet per minute **CHP** Combined heat and power

DC Direct current

CPO

DIR Direct internal reforming EC **European Community EMF** Electro-motive-force

**EVD** Electrochemical vapour deposition

Catalytic partial oxidation

**FCV** Fuel cell vehicle GT Gas turbine GTO Gate turn off

**HDS** Hydrodesulphurisation HHV Higher heating value

**IEC** International Electrotechnical Commission

**IGBT** Insulated gate bipolar transistor IIR Indirect internal reforming LHV Lower heating value

LH Liquid (cryogenic) hydrogen

LPG Liquid petroleum gas

LSGM Lanthanum, strontium, gallium, and magnesium oxide mixture **MCFC** Molten carbonate (electrolyte) fuel cell

**MEA** Membrane electrode assembly

MOSFET Metal oxide semiconductor field effect transistor

**NASA** National Aeronautics and Space Administration NL Normal litre, 1 litre at NTP

NTP Normal temperature and pressure (20 °C and 1 atm.)

**OCV** Open circuit voltage

Phosphoric acid (electrolyte) fuel cell PAFC

Proton exchange membrane or polymer electrolyte membrane - different **PEM** 

names for the same thing which fortunately have the same abbreviation.

Proton exchange membrane fuel cell or polymer electrolyte membrane fuel **PEMFC** 

**PFD** Process flow diagram **PM** Permanent Magnet ppb Parts per billion

PURPA Public utilities regulatory policies act

PTFE Polytetrafluoroethylene
PSI Pounds per square inch
PWM Pulse width modulation
SCG Simulated coal gas

SL Standard litre, 1 litre at STP

SOFC Solid oxide fuel cell

SPFC Solid polymer fuel cell (= PEMFC)

SPP Small power producer SRM Switched reluctance motor

SRS Standard reference state (25 °C and 1 bar) STP Standard temperature and pressure (= SRS)

TEM Transmission electron microscope t/ha Tonnes per hectare annual yield THT Tetrahydrothiophene ( $C_4H_8O_2S$ )

TOU Time of use

UL Underwriters' Laboratory YSZ Yttria stabilised zirconia

## **Symbols**

а	Coefficient in base 10 logarithm form of Tafel equation also Chemical activity
$a_{x}$	Chemical activity of substance x
A	Coefficient in natural logarithm form of Tafel equation also Area
В С	Coefficient in equation for mass transport voltage loss Constant in various equations also Capacitance
$c_p$	Specific heat capacity at constant pressure, in J.K <sup>-1</sup> .kg <sup>-1</sup>
$\tilde{c}_p$	Molar specific heat capacity at constant pressure, in J.K <sup>-1</sup> .mol <sup>-1</sup>
d e E	separation of charge layers in a capacitor Magnitude of the charge on one electron, $1.602 \times 10^{-19}$ Coulombs EMF or open circuit voltage
E <sup>0</sup> F G	EMF at standard temperature and pressure, and with pure reactants Faraday constant, the charge on one mole of electrons, 96 485 Coulombs Gibbs free energy
$\Delta G^0$	Change in Gibbs free energy at standard temperature and pressure, and with purreactants
$\Delta G_{T_A}$	Change in Gibbs free energy at ambient temperature
$\overline{g}$	Gibbs free energy per mole-
$\overline{g}_f$	Gibbs free energy of formation per mole
$(\overline{g}_f)_X$	Gibbs free energy of formation per mole of substance $X$
Н	Enthalpy
$\bar{h}$	Enthalpy per mole
$\overline{h}_f$	Enthalpy of formation per mole
$\left(\overline{h}_f\right)_X$	Enthalpy of formation per mole of substance X
I .	Current
i	Current density, current per unit area
ij	Limiting current density
$i_o$	Exchange current density at an electrode/electrolyte interface
oc	Exchange current density at the cathode
oa	Exchange current density at the anode
n	Mass
'n	Mass flow rate
$n_{x}$	Mass of substance x

N	Avagadro's number, $6.022 \times 10^{23}$
	also Revolutions per second
n	Number of cells in a fuel cell stack
P D D	Pressure The pressure at different stages in a process
$P_X$	Partial pressure of gas X
$P^0$	Standard pressure, 100 kPa
$P_{SAT}$	Saturated vapour pressure
$P_e$	Electrical power, only used when context is clear that pressure is not meant.
R	Molar or 'universal' gas constant, 8.314 J.K '.mol' also Electrical resistance
r	Area specific resistance, resistance of unit area
S	Entropy
$\overline{s}$	Entropy per mole
$(\bar{s})_X$	Entropy per mole of substance <i>X</i>
T	Temperature
$T_1, T_2$	Temperatures at different stages in a process
$T_A$	Ambient temperature
$T_c$	Combustion temperature
t	Time
V	Voltage
$V_c$	Average voltage of one cell in a stack
$V_a$	Activation overvoltage
$V_r$	Ohmic voltage loss
W	Work done
W'	Work done under isentropic conditions
$\dot{W}$	Power
z	Number of electrons transferred in a reaction
α	Charge transfer coefficient
Δ	Change in
$\varepsilon$	Electrical permittivity Ratio of the specific heat capacities of a gas
γ n	Efficiency
η	•
$\eta_c$	Isentropic efficiency (or compressor or turbine)
φ	Relative humidity
λ	Stoichiometric ratio
ω	Humidity ratio
$\mu_f$	Fuel utilisation

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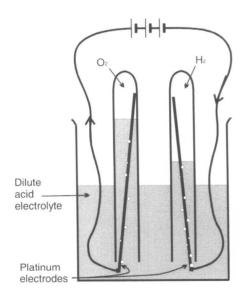
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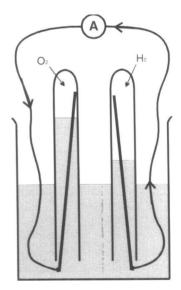
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#### Introduction

#### 1.1 Hydrogen Fuel Cells - Basic Principles

The basic operation of the hydrogen fuel cell is extremely simple. The first demonstration of a fuel cell was by lawyer-cum-inventor William Grove in 1839, using an experiment along the lines of that shown in Figures 1.1a and 1.1b. In Figure 1.1a water is being electrolysed into hydrogen and oxygen by passing an electric current through it. In Figure 1.1b the power supply has been replaced with an ammeter, and a small current is flowing. The electrolysis is being reversed – the hydrogen and oxygen are recombining, and an electric current is being produced.





**Figure 1.1a** The electrolysis of water. The water is separated into hydrogen and oxygen by the passage of an electric current.

**Figure 1.1b** A small current flows. The oxygen and hydrogen are recombining.

Note, the arrows show the direction of flow of the *negative electrons*, from – to +.

Another way of looking at the fuel cell is to say that the hydrogen fuel is being "burnt" or combusted in the simple reaction:

$$2H_2 + O_2 \rightarrow 2H_2O$$
 [1.1]

However, instead of heat energy being liberated, electrical energy is produced.

The experiment of Figures 1.1a and 1.1b makes a reasonable demonstration of the basic principle of the fuel cell, but the currents produced are very small. The main reasons for the small current are:

- the low 'contact area' between the gas, the electrode and the electrolyte basically just a small ring where the electrode emerges from the electrolyte.
- the large distance between the electrodes the electrolyte resists the flow of electric current.

To overcome these problems the electrodes are usually made flat, with a thin layer of electrolyte as in Figure 1.2. The structure of the electrode is porous, so that both the electrolyte from one side and the gas from the other can penetrate it. This is to give the maximum possible contact between the electrode, the electrolyte and the gas.

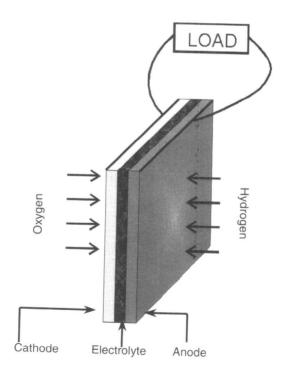


Figure 1.2 Basic cathode-electrolyte-anode construction of a fuel cell