ADVANCED TRANSPORT PHENOMENA

ANALYSIS, MODELING, AND COMPUTATIONS

P. A. Ramachandran

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Cover illustration: close-up of ink spreading in water mixed with droplets of paint. This image was created by dropping a small amount of oil- and xylene-based gold paint onto the surface of colored water. Different inks were then dropped onto the gold paint until the weight of the ink caused the gold paint to dip and allowed the inks to burst into the water. The complex colors, shapes, and patterns are a result of varying levels of flow rate, ink density, and surface tension. This creates eddies and vortices that affect the way light is reflected from the surface. Image © Perry Burge/Science Photo Library.

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The analysis, modeling, and computation of processes involving the transport of heat, mass, and momentum (transport phenomena) play a central role in engineering education and practice. The study of this subject originated in the field of chemical engineering but is now an integral part of most engineering curricula, for example, in biological, biomedical, chemical, environmental, mechanical, and metallurgical engineering both at undergraduate and at graduate level. There are many textbooks in this area, with varying levels of treatment from introductory to advanced, all of which are useful to students at various levels. However, my teaching experience over thirty years has convinced me that there is a need for a book that develops the subject of transport phenomena in an integrated manner with an easy-to-follow style of presentation. A book of this nature should ideally combine theory and problem formulation with mathematical and computational tools. It should illustrate the usefulness of the field with regard to practical problems and model development. This is the primary motivation for writing this book. This comprehensive textbook is intended mainly as a graduate-level text in a modern engineering curriculum, but parts of it are also useful for an advanced senior undergraduate class. Students studying this book will understand the methodology of modeling transport processes, along with the fundamentals and governing differential equations. They will develop an ability to think through a given physical problem and cast an appropriate model for the system. They will also become aware of the common analytical and numerical methods to solve these models, and develop a feel for the diverse technological areas where these concepts can be used.

Goals and outcome

The book is written with the objective that students finishing a first-year-level graduate course in this field should acquire the following skills and knowledge.

- Fundamentals and basic understanding of the phenomena and the governing differential equations. They should develop an ability to analyze a given physical problem and cast an appropriate model for the system. They should be exposed to the philosophy of the modeling process and appreciate the various levels at which models can be developed, and the interconnection and parameter requirements of various models.
- Analytical and numerical skills to solve these problems. They should develop the capability to solve some of the transport problems in a purely analytical setting and also expand their capability using numerical methods with some common software or programming tools. Often solving the same problem by both methods reinforces the physics and speeds up the learning process.
- An understanding of technological areas where transport models are useful. Students should develop an understanding of the diverse range of applications of this subject and

understand how the basic theory, models, and computations can be used in practical applications.

To achieve these goals the book focuses on analysis and model development of transport process in detail, starting from the very basics. It illustrates the solution methods by using the classical analytical tools as well as some common computational tools. The application of the theory is demonstrated with numerous illustrative problems; some sample numerical codes are provided for some problems to facilitate learning and the development of problem-solving abilities. References to many areas of application are provided, and some case-study problems are included.

Intended audience

The level and the sequence of presentation are such that the book is suitable for a first-level graduate course or a comprehensive advanced undergraduate course. In a modern graduate engineering curriculum, the entering students often have diverse backgrounds, and some graduate students might not have taken introductory undergraduate courses in transport phenomena. The introductory part of the book presented in the first two chapters is expected to bring these students up to speed.

Style and scope

The style of presentation is informal, and has more of a "classroom" conversational tone rather than being heavy scholarly writing. Each chapter starts off with clearly defined learning objectives and ends with a summary of "must-know" things that should have been mastered from that chapter. Computer simulations are also illustrated, together with analytical solutions. Often solutions to the same problem obtained by both analytical and numerical methods are shown. This helps the students to validate and benchmark their solutions, and to develop confidence in their computational skills. Also sample packages are included to accelerate the application of computer-aided problem solving in the classroom. These sample codes are presented in separate subsections or are boxed off for easier reading of the main text. Key equations are shown in boxes for easy reference. Case studies are given in several chapters, although the space limitation prohibits an extensive discussion of these applications. Additional material and computer codes will be posted on the accompanying website, which is being developed as supplementary material. This web-based material can be viewed as a living and evolving component of the book.

For instructors

Instructors will find the presentations novel and interesting and will be able to motivate the students to appreciate the beauty in the integrated structure of the field. They will also find

the worked examples and exercise problems useful to amplify the class lectures and illustrate the theory. Also the mathematical prerequisites listed at the beginning of each chapter will help the instructor to adjust the lecture content according to the students' mathematical preparedness. Additional web-based material that will aid the teaching of these necessary mathematical tools in a concise manner is being planned.

The book has more material than can be covered in one semester, and it can be used in the following manner in teaching.

- For an integrated course for students entering a modern graduate program with diverse undergraduate background, Chapters 1–13 can be covered at a reasonable pace in a onesemester course with some reading materials assigned from the other chapters.
- For a course focused mainly on flow problems Chapters 3–6 followed by Chapters 14–17 will provide a nice one-semester textbook.
- For a course focused mainly on heat and mass transfer the course can start with Chapters 7–13 and end with Chapters 18–22.

Distinguishing features

The book provides an integrated approach to the field. Theory is illustrated with many worked examples and case-study problems are indicated. The book also discusses many important and practically relevant topics that are not adequately covered in many earlier books. Some novel topics and features of the current book are indicated below.

- Discussion on multiscale modeling, model reduction by averaging and "information" flow.
- Solution of illustrative problems by both numerical and analytical methods.
- Sample codes in MATLAB for help in the development of numerical problem-solving skills.
- Detailed analysis of coupled transport problems.
- Introduction to non-Newtonian flow, microfluid analysis, and magnetohydrodynamics.
- · Introduction to perturbation, bifurcation, and stability analysis.
- Detailed discussion on analysis of transport with chemical reaction.
- Detailed analysis of multicomponent diffusion with many worked examples.
- · A full chapter on electrochemical systems and ionic transport.
- Application examples drawn from a wide range of areas and some suggested case-study problems.

Acknowledgement

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TOPICAL OUTLINE

The topical organization of this book is as follows.

Chapter 1 is the basic introductory material which illustrates the richness of the subject, spanning applications to a wide range of problems in science and engineering. This chapter also provides the introduction to the basics of model building and shows the relationships among models of various levels of hierarchy. The basic vocabulary is introduced, and the physical properties needed in transport problems are discussed. The link between continuum and molecular models is indicated. The chapter concludes with a brief note on the historical development of the subject.

Chapter 2 illustrates the formulation of model equations for many common transport problems using a basic control-volume-balance type of approach. All three modes of transport are illustrated so that the student can grasp the similarities. Some "standard" problems are illustrated. This chapter is written assuming no significant earlier background knowledge in this field, and is therefore useful to bring such students up to speed.

The next few chapters, Chapters 3–6, provide the detailed framework for the analysis of momentum transport problems. The kinematics of flow are reviewed in Chapter 3, while the kinetics of flow are discussed in Chapter 4, leading to the derivation of the differential equations for the stress field and the velocity field in Chapter 5. Solutions to illustrative flow problems are then reviewed in Chapter 6, and here some "standard" flow problems shown in Chapters 1 and 2 are revisited in a more general setting, and solutions to some additional complex problems are reviewed. Flows involving non-Newtonian fluids and magnetohydrodynamics are also treated briefly, since they find extensive applications in practice and it is necessary to expose the student to these topics.

Chapters 7 and 8 deal with the differential equations for energy transport and the temperature field, with many illustrative heat-transfer problems in Chapter 8. Similarly, Chapters 9 and 10 deal with differential equations for mass transport and illustrative applications. These chapters bring out the close analogy and common problem-solving strategies for these two transport processes. In the heat-transfer context entropy balance is introduced in a simple manner and the relation to the second law is pointed out in a succinct manner. In the mass-transfer context several important topics such as gas—liquid reactions, membrane transport, and dispersion are presented in detail. Numerical methods involving MATLAB for both ODE and PDE are presented. Sample codes are provided as examples, and side-by-side comparisons with analytical solutions are provided for many problems, so that the students can benchmark their results. The transient problems for both heat and mass are then analysed in Chapter 11 in a unified setting, while some convective transport problems are studied in Chapter 12.

Chapter 13 provides an analysis of a number of coupled problems, for example natural convection, simultaneous heat and mass transfer, condensation, fog formation, and temperature effects in porous catalysts.

Topical outline

Chapter 14 develops some tools to analyze transport problems in further detail. The dimensionless analysis is revisited using novel matrix-algebra-based methods. The concept of scaling and pertubation methods is introduced together with many applications. The scaling tools also provide the necessary background to the boundary-layer flows discussed in Chapter 15. Chapter 15 also discusses additional topics in fluid mechanics such as low-Reynolds-number flow and irrotational flows. Chapter 16 deals with bifurcation and stability analysis. Chapter 17 provides an introductory treatment of turbulent flows.

Chapters 18 and 19 deal with additional topics in heat transfer, including convection in turbulent flow, boiling, condensation, and radiation heat transfer (Chapter 19). The final three chapters (Chapters 20–22) discuss some topics in mass transfer, including more discussion on convective transport and axial dispersion (Chapter 20), multicomponent systems (Chapter 21), and transport of charged species (Chapter 22).

NOTATION

 c_p

a_{w}	activity of water or solute indicated in the subscript in Section 10.7
A	area of cross-section for flow
A	Arrhenius pre-exponential factor in Section 8.3.2
A	amplitude of surface temperature oscillation in Section 11.10, K
A_1, A_2	usually integration constants
A_{p}	projected area of solid in the direction of flow
Ar	Archimedes number
B	dimensionless parameter defined as $(L/R)Pe$ in Section 12.4
Bi_{G}	Biot number in gas–liquid mass transfer, $k_{\rm G}H_{\rm A}/k_{\rm L}$
Bi_h	Biot number for heat transfer, hL_{ref}/k_{solid}
Bim	Biot number for mass transfer, $k_{\rm m}L_{\rm ref}/D$
Bo	Bond number
Br	Brinkman number for viscous production of heat, Eq. (13.23)
C	total molar concentration of a multicomponent mixture, mol/m ³
Ca	capillary number, $\mu v_{\rm ref}/\sigma$
C_{A}	local concentration of species indicated in the subscript (A here), mol/m ³
$C_{\rm A}^*$	concentration of A in liquid if in equilibrium with the bulk gas (Section 10.5)
$\langle C_{\rm A} \rangle$	cross-sectionally averaged concentration
C_{Ab}	concentration of species A indicated in the bulk phase, mol/m ³
C_{Ab}	cup mixed average concentration of species A, Section 12.4
C_{Ai}	concentration of species A, section 12.4
$C_{A,i}$	inlet concentration of species A for flow reactor, Chapter 2, mol/m ³
C_{As}	concentration of species A at a solid surface, mol/m ³
	Concentration of species indicated in the subscript in the bulk gas, mol/m ³
C_{AG}	Concentration of species indicated in the subscript in the bulk liquid, mol/m ³
$C_{\rm AL}$	
$C_{\rm AL}^*$	hypothetical concentration of A if in equilibrium with the bulk gas, mol/m ³
$C_{A,e}$	concentration of species indicated in the subscript exit
$C_{\rm b}$	cup mixed (flow) average concentration of species A, Section 20.5
$C_{\rm BL}$	concentration of liquid-phase reactant in bulk liquid in Section 10.5
<i>c</i>	molecular speed in Chapter 1 (kinetic theory)
\bar{c}	average molecular speed in Chapter 1 (kinetic theory)
c^2	average of the squares of the molecular speed in Chapter 1 (kinetic theory)
C	speed of sound in Chapter 2
C	speed of light in radiation heat transfer in Chapter 19
c_{A}	dimensionless concentration of species indicated in the subscript (A here), C_A/C_{re}
\bar{c}	average speed of molecules in Section 1.8.1
C_{D}	drag coefficient
$C_{\rm L}$	lift coefficient
C_p	specific heat of a species, mass basis, under constant-pressure conditions, J/kg · K

```
C_p
           specific heat of a species, mole basis, J/mol·K
           specific heat of a species, mass basis, under constant-volume conditions, J/kg · K
Cv
           diameter of the molecules treated as rigid spheres in Section 1.8.1
d
d. d.
           diameter of a tube or pipe
di
           impeller or pump diameter, Sections 14.1.5 and 14.1.6
           particle or solid diameter
dp
D_{\rm e}
           effective diffusivity of a species in a heterogeneous medium
           molecular diffusivity of species i
D_i
D_{K}
           Knudsen diffusion coefficient for small pores
           turbulent mass diffusivity, m<sup>2</sup>/s
D_{\mathsf{t}}
           Damköhler number Vk/Q
Da
           charge on an electron in Chapter 22
e
           pipe roughness parameter in Sections 5.5 and 17.6.1
e
           total energy content per unit mass
e
           unit vector in the x-direction
e_r
           electric field
\mathbf{E}
E^2
           operator defined by Eq. (3.53) or Eq. (3.55)
E^4
           Stokes operator defined as E^2E^2
E
           emissive power of a gray body
           emissive power of a black body, W/m<sup>2</sup>
E_{\rm b}
E_{bk}
           emissive power of a black body from surface k, W/m<sup>2</sup>
E_{b\lambda}
           spectral emissive power, W/m<sup>2</sup> nm
\tilde{E}
           rate-of-strain tensor
f
           dimensionless streamfunction in boundary-layer flow
f
           Fanning friction factor
F_{ik}
           radiation view factor, surface i to k
F
           Faraday constant = 96 485 C/mol
F
           force acting on a control volume
\mathcal{F}, \mathcal{F}_{m}
           correction factor for unidirectional mass transfer, Sections 10.1 and 20.2.1
           augmentation factor for heat transfer due to blowing
\mathcal{F}_{h}
           acceleration due to gravity
g
           rate of production of entropy per unit volume, W/K·m<sup>3</sup>
gs
G
           pressure-drop parameter defined as -dP/dx
Ġ
           superficial gas velocity, kg/m<sup>2</sup>·s
           Grashof number
Gr
ĥ
           enthalpy per unit mass
           heat transfer coefficient (usually from solid to fluid), W/m<sup>2</sup> · k
h
h
           elevation or height from a datum plane for flow problems
           Planck's constant in radiation chapter, 6.6208 \times 10^{-34} \text{ J} \cdot \text{s}
h
           head loss due to friction
hf
hG
           heat transfer coefficient in the gas film
           heat transfer coefficient in the liquid film
hL
hol
           heat released on condensation of a species, J/kg
           heat of vaporization, J/kg
hig
hsl
           heat needed for melting a solid, J/kg
           Henry's-law constant for solubility of A defined by P_A = H_A C_A, Pa m<sup>3</sup>/mol
H_{A}
```

На	Hartmann number
На	Hatta number for gas—liquid reactions
i	current density in Chapter 22, A/m ²
i.	square root of -1 in Section 11.11
<i>I</i>	intensity of radiation, W/m ²
$j_{\rm A}$	mass diffusion flux of A (mass reference), kg/m ² · s
$J_{\rm A}$	molar diffusion flux of A (mole reference), mol/m ² · s
J_k	radiosity of a surface in radiation, W/m ²
$k_{\rm G}$	mass transfer coefficient from gas to interface
1	(partial pressure driving force), mol/Pa·m²·s
$k_{ m L}$	mass transfer coefficient from an interface to bulk liquid
ī.	(concentration driving force), m/s
k	thermal conductivity of a species, subscript 1 for liquid, g for gas, s for solid, W/m · K
k	turbulent kinetic energy per unit mass, m ² /s ²
k	rate constant for reaction, general
$k_{\rm B}$	Boltzmann constant, 1.38×10^{-23} J/K
k_0	rate constant for a zeroth-order reaction, mol/m ³ · s
<i>k</i> ₁	rate constant for a first-order reaction, 1/s
k ₂	rate constant for a second-order reaction, m ³ /mol·s
k _m	mass transfer coefficient from a solid to fluid (concentration driving force), m/s mass transfer coefficient under low-mass-flux conditions, m/s
$k_{ m m}^{ m o}$	
\tilde{K}	diffusivity matrix in Section 21.4
	matrix of multicomponent diffusion coefficient in Section 21.4
$K_{\rm G}$	overall mass transfer coefficient from a bulk gas to a bulk liquid
ν	(gas phase partial pressure driving force), mol/m ² · s · Pa
$K_{\rm L}$	overall mass transfer coefficient from a bulk gas to a bulk liquid
L	(liquid concentration driving force), m/s
M	length of the plate or tube or catalyst slab, m local Mach number, v/c
	mass of a molecule in Section 1.8.1
\dot{m}	mass flow rate, kg/s
	total mass of A in an unit or control volue, kg
$\dot{m}_{\mathrm{A,tot}}$	mass flow rate of A entering a unit, kg/s
$\dot{m}_{\rm Ae}$	mass flow rate of A exiting a unit, kg/s
$\dot{m}_{\rm AW,tot}$	total mass of A transferred to walls from an unit or procss, kg/s
\bar{M}	average molecular weight of a mixture, kg/g.mol
M	momentum flow rate vector, N
M_{A}	molecular weight of species indicated in the subscript, kg/g.mol
$M_{ m W}$	molecular weight in general
$\widetilde{\mathcal{M}}$	total moles present in a control volume, g-mol
$\dot{\mathcal{M}}$	moles per second entering/leaving the unit, i = inlet, e = exit
\mathcal{M}_{A}	moles of A in the system or control volume
Nu	Nusselt number, usually defined as hd_t/k or hx/k
$N_{\rm Av}$	Avogadro number = 6.23×10^{23} molecules/g-mol
n	number density of molecules in Section 1.8.1
	V

```
normal vector outward from a control surface
n
         mass flux vector of species A, stationary frame, kg-A/m<sup>2</sup> · s
n_{\mathsf{A}}
         component of mass flux vector of A in the x-direction, kg-A/m<sup>2</sup> · s
n_{Ax}
         number of transfer of unit parameter
N_{\rm fu}
         fluid pressure; equal to the average normal stress, Pa
         vapor pressure of a species, Pa
Pvap
         thermodynamic pressure used in equation of state, Pa
P
         the concentration gradient or temperature gradient in the p-substitution method
p
p^*
         dimensionless pressure, p/\rho v_{\rm ref}^2
p^{**}
         dimensionless pressure, p^*Re
P
         power input for agitated vessels, W
         critical pressure of a species, Pa
P_{c}
P
         modified pressure defined as p + \rho gh
         temperature gradient in Example 8.3 and concentration gradient in Section 10.4.6
         Péclet number, d_t\langle v \rangle / \alpha
Pe
         Péclet number based on pipe radius, d_t\langle v \rangle/D
Pe_R
Pe^*
         dispersion Péclet number in Section 12.5, \langle v \rangle L/D_E
         power number as p/(\rho N_i^3 d_i^5) in Section 14.15
Po
Pr
         Prandtl number, c_p \mu/k
         dimensionless stoichiometric ratio defined by Eq. (10.44) in Section 10.5
q
Q
         volumetric flow rate in a pipe, m<sup>3</sup>/s
(Q)_{v}
         internal heat generation rate, W/m<sup>3</sup>
         heat flux vector (molecular) W/m<sup>2</sup>
q
a^{(m)}
         heat flux vector (molecular), same as q, W/m<sup>2</sup>
         heat flux from a surface or wall to a flowing fluid
q_s
q^{(t)}
         heat flux vector due to turbulence, W/m<sup>2</sup>
         component of the heat flux vector in the x-direction
q_x
         component of the heat flux vector in the y-direction
q_{\nu}
         heat flux to the wall of a pipe from a fluid
q_{\mathrm{W}}
         rate at which heat is added to the control volume; unit volume basis, W/m<sup>3</sup>
         rate at which heat is generated within control volume per unit volume, W/m<sup>3</sup>
Òν
         component of the heat flux vector in the z-direction
q_z
         radial coordinate in cylindrical and spherical system
r
R
         radius of cylinder or catalyst particle
         local rate of mass production of A by reaction per unit volume, mass units, kg/m<sup>3</sup> · s
rA
         local rate of mole production of A by reaction per unit volume, mole units, mol/m<sup>3</sup> · s
R_{A}
R^*
         gas constant defined as R_G/M_W
R_{A}
         rate of production of a species A by reaction
         Reynolds number, L_{\text{ref}}v_{\text{ref}}\rho/\mu
Re
         gas constant, 8.314 Pa m<sup>3</sup>/mol · K
R_{G}
         entropy energy per unit mass of fluid, J/K · kg
ŝ
         entropy flux vector, W/K · m<sup>2</sup>
s
         shape parameter for conduction or diffusion,
S
         1 for slab, 2 for long cylinder, 3 for sphere
```

Notation

~	
Sc	Schmidt number, $\mu/(\rho D)$
Sh	Sherwood number, $k_{\rm m}x/D$
St	Stanton number, $Nu/(RePr)$ or $Sh/(ReSc)$
t	time variable
$t_{\rm E}$	exposure time for a gas-liquid interface
T	local temperature in the medium
$T_{\rm a}$	temperature of the surroundings
$\langle T \rangle$	cross-sectionally averaged temperature
T_{b}	cup mixing (flow-averaged) temperature
$T_{\rm c}$	critical temperature of a species
$T_{\mathbf{f}}$	temperature of the surrounding fluid in contact with a solid
$T_{\mathbf{i}}$	temperature of a gas-liquid interface
T_{w}	temperature of a wall or tube
T_{∞}	temperature of the approaching fluid
\hat{u}	internal energy unit mass of fluid, J/kg
Û	internal energy per unit mole of fluid, J/mol
U	overall heat transfer coefficient from hot fluid to cold fluid, W/m ² · K
\hat{v}	specific volume, $1/\rho$, m ³ /kg.
v	velocity vector; also mass-fraction-averaged velocity in a multicomponent mixture, m/s
$oldsymbol{v}'$	fluctuating velocity vector in turbulent flow
$ar{v}$	time-averaged velocity vector in turbulent flow
v^*	mole-fraction-averaged velocity in a multicomponent mixture, m/s
ν_{x}	x-component of the velocity; v_y and v_z defined similarly
v_z	axial (z-) component of velocity in cylindrical coordinates
v_{θ}	velocity component in the tangential (θ) direction
v_{A}	velocity of species A in a multicomponent mixture, stationary frame, m/s
$v_{\rm e}$	velocity component in the fluid outside the boundary layer, m/s
V	total control volume
\hat{V}	molar volume, m ³ /mol
V	speed of a moving solid in shear flow in flow direction, m/s
v_{b}	molecular volume at boiling point of solvent
$V_{\rm f}$	friction velocity defined as $\sqrt{\tau_{f/\rho}}$ used in turbulent flow, m/s
W	rate at which work is done on the control volume, W/m ³
$\dot{W}_{ m S}$	rate at which work is done by a moving part on the control volume, W/m ³
W_{f}	rate at which heat energy is produced by friction, W/m ³
X	distance variable in the x-direction, y and x defined similarly.
x_i	mole fraction of species indicated by the subscript (usually in the liquid phase)
y	distance variable in the y-direction
y_i	mole fraction of species indicated by the subscript (usually in the gas phase)
y^+	dimensionless length used in turbulence analysis near a wall
$y_{\rm B}(1.{\rm m})$	log-mean mole fraction of the non-diffusing component
Z _*	axial distance variable in cylindrical coordinates
z*	dimensionless axial distance variable in cylindrical coordinates, z/R
z_i	number of charges on an ionic species frequency of molecular collisions in Section 1.8.1
Z	requercy of molecular comstons in Section 1.6.1

Greek letters and other symbols

α	thermal diffusivity of a solid, m ² /s
α	absorptivity of a surface in radiation
α_t	turbulent heat diffusivity, m ² /s
$\epsilon_{\rm H}$	turbulent heat diffusivity, m ² /s
β	bulk modulus of elasticity, N/m ²
β	angular velocity vector
γ	dimensionless activation energy in Section 13.7 and Example 16.1
γ	ratio of specific-heat values, c_p/c_v
∇	gradient operator
∇_*	gradient operator in dimensionless coordinates
∇^2	Laplacian operator defined by Eqs. (1.56)–(1.58) for scalars
∇^2	Laplacian operator defined in Sections 5.3.1 and 5.3.2 for vectors
∇^4	biharmonic operator defined by Eq. (5.31)
Δ	difference operator, out – in,
Δ	ratio of boundary-layer thickness, heat/mass to momentum
ΔH	heat of reaction, J/mol
$\Delta H_{\rm v}$	heat of vaporization, mole basis, J/mol
$\Delta \pi$	osmotic pressure diffference in Section 10.7, Pa
δ	parameter in Frank-Kamenetskii model
δ	thickness of momentum boundary layer in general
δ_{f}	film thickness for mass transfer,
	abbreviated as δ in Chapter 10
δ_{m}	thickness of mass-transfer boundary layer
δ_{t}	thickness of thermal boundary layer
ϵ	dielectric permittivity of a medium in Chapter 22
ϵ	emissivity of the medium
ϵ	energy dissipation rate in turbulent flow analysis
ϵ	a parameter in Lennard-Jones model in Chapter 1
η	effectiveness factor of a porous catalyst in Chapter 10
5	dimensionless axial distance, z^*/Pe
η	similarity variable defined by Eq. (11.30) in Chapter 11 for heat conduction
η	similarity variable defined in Chapter 12.2 for convective heat transfer
K	circulation (line integration of tangential velocity) in Section 15.4.3
K	conductivity of an ionized liquid in Section 22.1.3
K	ratio of radius values, R_c/R_o , in Chapter 6
κ	Boltzmann constant, also denoted as $k_{\rm B}$
λ	Debye length in Sections 22.5 and 22.6
λ	mean free path in Section 1.8.1
Λ	consistency index parameter for power law fluids
θ	angular direction in polar coordinates

Notation

θ	latitude direction in spherical coordinates
θ	dimensionless temperature in heat transfer examples
μ	coefficient of viscosity, Pa · s
μ_i	mobility of charged species i in Chapter 22
μ_{w}	chemical potential of water in Section 10.7
υ	coefficient of kinematic viscosity, μ/ρ , m ² /s
ν_{t}	turbulent kinematic viscosity, μ_t/ρ , m ² /s
$v_{\rm T}^+$	dimensionless total (molecular + turbulent) kinematic viscosity
ρ	density of the medium or the fluid, kg/m ³
ρ_c	electric charge density in Chapter 22
$\rho_{\rm A}$	density of A in a multicomponent mixture, kg/m ³
σ	surface tension, N/m
$\sigma_{\chi\chi}$	total stress (viscous and pressure) in the x-direction
σ	Staverman constant in Section 10.7.1
σ_{yx}	same as τ_{yx} since shear stress has no pressure contribution
σ	Stefan-Boltzmann constant
τ	dimensionless time in Chapter 11, t/t_{ref}
$ au_{ m W} $	stress exerted by the wall opposite to the flow direction in response to $-\tau_0$
τ_{w}	stress exerted by the solid on the fluid in pipe flow,
	$\mu dv_z/dr$ at $r=R$, usually negative in the flow direction
$ au_{ m f}$	stress exerted by the fluid on the solid, $\mu dv_x/dy$ at $y=0$
τ_0	yield stress for Bingham flow
$ au_{\chi\chi}$	viscous stress in the x-direction on a plane whose unit
	normal is in the <i>x</i> -direction
$ au_{yx}$	viscous stress in the x-direction on a plane whose
	unit normal is in the y-direction; other components are defined similarly
ϕ	blowing parameter in Section 13.6.1
ϕ	electric potential in Chapter 22
ϕ	longitude in the spherical coordinate system
ϕ	velocity potential defined by Eq. (3.49) in Section 3.10
ϕ	Thiele parameter for a first-order reaction
ϕ_0	Thiele parameter for a zeroth-order reaction defined by Eq. (10.34)
$\Phi_{\rm v}$	rate of heat production by viscosity per unit volume, Eq. (7.12), W/m ³
ψ	streamfunction defined by Eq. (3.39) or Eq. (3.40)
ω	frequency of oscillation in periodic flow, s ⁻¹
ω^*	dimensionless frequency of oscillation in periodic flow, $\omega t_{\rm ref}$
ω	vorticity for a plane flow defined as ω_z
ω	vorticity vector for a general 3D flow, $\nabla \times V$
ω	specific energy-dissipation rate in turbulent flow
ω_{A}	mass fraction of species indicated by the subscript, kg-A/kg-total
ξ	dimensionless radial position, r/R or x/L
Ω	angular velocity, rotational speed
Ω_i	speed of rotation or agitation in Section 14.1.5 and 14.1.6, r.p.s.

Common subscripts

0	bulk conditions
g, G	gas-phase properties
9	exit values (Chapter 2)
i	inlet values (Chapter 2)
i	interface conditions (Chapters 9 and 10)
,L	liquid-phase properties
S	conditions at a surface of a solid or catalyst