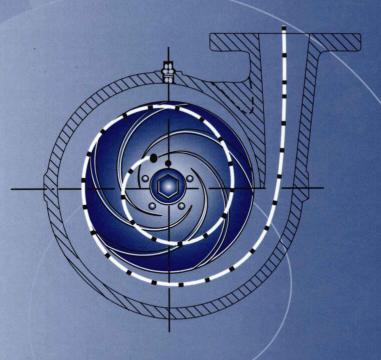
Second Edition, Revised and Expanded



Ron Darby

Second Edition, Revised and Expanded

Ron Darby

Texas A&M University College Station, Texas

江苏工业学院图书馆 藏 书 章



ISBN: 0-8247-0444-4

This book is printed on acid-free paper.

Headquarters

Marcel Dekker, Inc.

270 Madison Avenue, New York, NY 10016

tel: 212-696-9000; fax: 212-685-4540

Eastern Hemisphere Distribution

Marcel Dekker A

Hutgasse 4, Postfach 812, CH-4001 Basel, Switzerland

tel: 41-61-261-8482: fax: 41-61-261-8896

World Wide We

http://www.dekker.com

The publisher offers discounts on this book when ordered in bulk quantities. For more information, write to Special Sales/Professional Marketing at the headquarters address above.

Copyright © 2001 by Marcel Dekker, Inc. All Rights Reserved.

Neither this book nor any part may be reproduced or transmitted in any form or by any means, electronic or mechanical, including photocopying, microfilming, and recording, or by any information storage and retrieval system, without permission in writing from the publisher.

Current printing (last digit):

10 9 8 7 6 5 4 3 2

PRINTED IN THE UNITED STATES OF AMERICA

Preface

The objectives of this book are twofold: (1) for the student, to show how the fundamental principles underlying the behavior of fluids (with emphasis on one-dimensional macroscopic balances) can be applied in an organized and systematic manner to the solution of practical engineering problems, and (2) for the practicing engineer, to provide a ready reference of current information and basic methods for the analysis of a variety of problems encountered in practical engineering situations.

The scope of coverage includes internal flows of Newtonian and non-Newtonian incompressible fluids, adiabatic and isothermal compressible flows (up to sonic or choking conditions), two-phase (gas-liquid, solid-liquid, and gas-solid) flows, external flows (e.g., drag), and flow in porous media. Applications include dimensional analysis and scale-up, piping systems with fittings for Newtonian and non-Newtonian fluids (for unknown driving force, unknown flow rate, unknown diameter, or most economical diameter), compressible pipe flows up to choked flow, flow measurement and control, pumps, compressors, fluid-particle separation methods (e.g.,

iv Preface

centrifugal, sedimentation, filtration), packed columns, fluidized beds, sedimentation, solids transport in slurry and pneumatic flow, and frozen and flashing two-phase gas—liquid flows. The treatment is from the viewpoint of the process engineer, who is concerned with equipment operation, performance, sizing, and selection, as opposed to the details of mechanical design or the details of flow patterns in such situations.

For the student, this is a basic text for a first-level course in process engineering fluid mechanics, which emphasizes the systematic application of fundamental principles (e.g., macroscopic mass, energy, and momentum balances and economics) to the analysis of a variety of fluid problems of a practical nature. Methods of analysis of many of these operations have been taken from the recent technical literature, and have not previously been available in textbooks. This book includes numerous problems that illustrate these applications at the end of each chapter.

For the practicing engineer, this book serves as a useful reference for the working equations that govern many applications of practical interest, as well as a source for basic principles needed to analyze other fluid systems not covered explicitly in the book. The objective here is not to provide a mindless set of recipes for rote application, however, but to demonstrate an organized approach to problem analysis beginning with basic principles and ending with results of very practical applicability.

Chemical Engineering Fluid Mechanics is based on notes that I have complied and continually revised while teaching the junior-level fluid mechanics course for chemical engineering students at Texas A&M University over the last 30 years. It has been my experience that, when being introduced to a new subject, students learn best by starting with simple special cases that they can easily relate to physically, and then progressing to more generalized formulations and more complex problems. That is the philosophy adopted in this book. It will certainly be criticized by some, since it is contrary to the usual procedure followed by most textbooks, in which the basic principles are presented first in the most general and mathematical form (e.g., the divergence theorem, Reynolds transport theorem, Navier Stokes equations, etc.), and the special cases are then derived from these. Esoterically, it is very appealing to progress from the general to the specific, rather than vice versa. However, having taught from both perspectives, it is my observation that most beginning students do not gain an appreciation or understanding from the very general, mathematically complex, theoretical vector expressions until they have gained a certain physical feel for how fluids behave, and the laws governing their behavior, in special situations to which they can easily relate. They also understand and appreciate the principles much better if they see how they can be applied to the analysis of practical and useful situations, with results that actually work Preface v

in practice. That is why the multi-dimensional vector generalizations of the basic conservations laws have been eschewed in favor of the simpler component and one-dimensional form of these laws.

It is also important to maintain a balanced perspective between fundamental, or theoretical, and empirical information, for the practicing engineer must use both to be effective. It has been said that all the tools of mathematics and physics in the world are not sufficient to calculate how much water will flow in a given time from a kitchen tap when it is opened. However, by proper formulation and utilization of certain experimental observations, this is a routine problem for the engineer. The engineer must be able to solve certain problems by direct application of theoretical principles only (e.g., laminar flow in uniform conduits), others by utilizing hypothetical models that account for a limited understanding of the basic flow phenomena by incorporation of empirical parameters (e.g., :turbulent flow in conduits and fittings), and still other problems in which important information is purely empirical (e.g., pump efficiencies, two-phase flow in packed columns). In many of these problems (of all types), application of dimensional analysis (or the principle of "conservation of dimensions") for generalizing the results of specific analysis, guiding experimental design, and scaling up both theoretical and experimental results can be a very powerful tool.

This second edition of the book includes a new chapter on two-phase flow, which deals with solid-liquid, solid-gas, and frozen and flashing liquid-gas systems, as well as revised, updated, and extended material throughout each chapter. For example, the method for selecting the proper control valve trim to use with a given piping configuration is presented and illustrated by example in Chapter 10. The section on cyclone separators has been completely revised and updated, and new material has been incorporated in a revision of the material on particles in non-Newtonian fluids. Changes have made throughout the book in an attempt to improve the clarity and utility of the presentation wherever possible. For example, the equations for compressible flow in pipes have been reformulated in terms of variables that are easier to evaluate and represent in dimensionless form.

It is the aim of this book to provide a useful introduction to the simplified form of basic governing equations and an illustration of a consistent method of applying these to the analysis of a variety of practical flow problems. Hopefully, the reader will use this as a starting point to delve more deeply into the limitless expanse of the world of fluid mechanics.

Unit Conversion Factors

Dimension	Equivalent Units
Mass	1 kg = 1000 g = 0.001 metric ton (tonne) = $2.20461 \text{ lb}_m = 35.27392 \text{ oz}$
	1 lb _m = 453.593 g = 0.453593 kg = 5×10^{-4} ton = 16 oz
Force	$1 \text{ N} = 1 \text{ kg m/s}^2 = 10^5 \text{ dyn} = 10^5 \text{ g cm/s}^2 = 0.22418 \text{ lb}_1$
	1 lb _t = 32.174 lb _m ft/s ² = 4.4482 N = 4.4482×10^{5} dyn
Length	1 m = 100 cm = $10^6 \mu m = 10^{10} \text{ Å} = 39.37 in. = 3.2808 ft =$
	1.0936 yd = 0.0006214 mi
	1 ft = 12 in. = 1/3 yd = 0.3048 m = 30.48 cm
Volume	1 m^3 = 1000 liters = 10^6 cm^3 = 35.3145 ft ³ = 264.17 gal
	1 ft ³ = 1728 in. ³ = 7.4805 gal = 0.028317 m^3 = 28.317 liters =
Pressure	28,317 cm ³ 1 atm = 1.01325 \times 10 ⁵ N/m ² (Pa) = 1.01325 bar = 1.01325 \times
1 1033010	$10^6 \text{ dyn/cm}^2 = 760 \text{ mm Hg } @ 0^{\circ}\text{C (torr)} = 10.333 \text{ m}$
	$H_2O @ 4^{\circ}C = 33.9 \text{ ft } H_2O @ 4^{\circ}C = 29.921 \text{ in. Hg } @$
	0° C = 14.696 lb _t /in. ² (psi)
Energy	1 J = 1 N m = 10^7 erg = 10^7 dyn cm = 2.667×10^{-7} kWh =
Liloigy	$0.23901 \text{ cal} = 0.7376 \text{ ft lb}_t = 9.486 \times 10^{-4} \text{ Btu } [550 \text{ ft lb}_t/$
	(hp s)]
Power	1 W = 1 J/s = 0.23901 cal/s = 0.7376 ft lb _t /s = 9.486×10^{-4}
	Btu/s = 1 \times 10 ³ kW = 1.341 \times 10 ³ hp
Flow Rate	1 m ³ /s = 35.3145 ft ³ /s = 264.17 gal/s = 1.585×10^4 gal/min = 10^6 cm ³ /s
	1 gpm = 6.309×10^{-5} m ³ /s = 2.228×10^{-3} ft ³ /s = 63.09 cm ³ /s

Example: The factor to convert Pa to psi is $14.696 \text{ psi/(}1.01325 \times 10^5 \text{ Pa})$ Some values of the gas constant: $R = 8.314 \times 10^3 \text{ kg m}^2/\text{(s}^2 \text{ kg mol K)}$ $= 8.314 \times 10^7 \text{ g cm}^2/\text{(s}^2 \text{ g mol K)}$ $= 82.05 \text{ cm}^3 \text{ atm/(g mol K)}$ = 1.987 cal/(g mol K) or Btu/(lb mol °R) = 15.45 ft lb//(lb mol °R) $= 10.73 \text{ ft}^3 \text{ psi/(lb mol °R)}$ $= 0.730 \text{ ft}^3 \text{ atm/(lb mol °R)}$

Contents

	ace Convei	rsion Factors	iii xvi
1.	BASIC	CONCEPTS	1
	I.	FUNDAMENTALS	1
		A. Basic Laws	1
		B. Experience	2
	II.	OBJECTIVE	2
	III.	PHENOMENOLOGICAL RATE OR TRANSPORT	
		LAWS	3
		A. Fourier's Law of Heat Conduction	4
		B. Fick's Law of Diffusion	5
		C. Ohm's Law of Electrical Conductivity	5
		D. Newton's Law of Viscosity	6

vii

iii		•	Contents
	IV. V.	TURBULENT MACROSCOPIC (CONVECTIVE)	9
	DD O	TRANSPORT MODELS	10
		BLEMS ATION	11 13
	NOT	ATION	13
2.	DIM	ENSIONAL ANALYSIS AND SCALE-UP	15
	I.	INTRODUCTION	15
	II.	UNITS AND DIMENSIONS	16
		A. Dimensions	16
		B. Units	18
		C. Conversion Factors	19
	III.	CONSERVATION OF DIMENSIONS	20
		A. Numerical Values	21
		B. Consistent Units	22
	IV.	DIMENSIONAL ANALYSIS	22
		A. Pipeline Analysis	25
		B. Uniqueness	28
		C. Dimensionless VariablesD. Problem Solution	28 29
			29 29
	V.	E. Alternative Groups SCALE-UP	30
	v. VI.	DIMENSIONLESS GROUPS IN FLUID	30
	٧1.	MECHANICS	35
	VII.		35
		BLEMS	40
		ATION	52
			-
3.	FLUI	D PROPERTIES IN PERSPECTIVE	55
	I.	CLASSIFICATION OF MATERIALS AND FLUI	
		PROPERTIES	55
	II.	DETERMINATION OF FLUID VISCOUS	
		(RHEOLOGICAL) PROPERTIES	59
		A. Cup-and-Bob (Couette) Viscometer	60
	***	B. Tube Flow (Poiseuille) Viscometer	63
	III.	TYPES OF OBSERVED FLUID BEHAVIOR	64
		A. Newtonian Fluid	65
		B. Bingham Plastic Model	65
		C. Power Law Model	66

Contents	ix

		D. Structural Viscosity Models	67
	IV.	TEMPERATURE DEPENDENCE OF VISCOSITY	71
	IV.	A. Liquids	71
		B. Gases	72
	V.	DENSITY	72
		BLEMS	73
		ATION	83
		ERENCES	84
4.	FLU	ID STATICS	85
	I.	STRESS AND PRESSURE	85
	II.	THE BASIC EQUATION OF FLUID STATICS	86
	11.	A. Constant Density Fluids	88
		B. Ideal Gas—Isothermal	89
		C. Ideal Gas—Isentropic	90
		D. The Standard Atmosphere	90
	III.	MOVING SYSTEMS	91
		A. Vertical Acceleration	91
		B. Horizontally Accelerating Free Surface	92
		C. Rotating Fluid	93
	IV.	BUOYANCY	94
	V.	STATIC FORCES ON SOLID BOUNDARIES	94
	PRO	BLEMS	96
	NOT	TATION	104
5.	CON	SERVATION PRINCIPLES	105
	I.	THE SYSTEM	105
	II.	CONSERVATION OF MASS	106
		A. Macroscopic Balance	106
		B. Microscopic Balance	107
	III.	CONSERVATION OF ENERGY	108
		A. Internal Energy	110
		B. Enthalpy	112
	IV.	IRREVERSIBLE EFFECTS	113
		A. Kinetic Energy Correction	116
	V.	CONSERVATION OF MOMENTUM	120
		A. One-Dimensional Flow in a Tube	121
		B. The Loss Coefficient	123
		C. Conservation of Angular Momentum	127

X	Contents

		D. Moving Boundary Systems and Relative Motion	128
		E. Microscopic Momentum Balance	130
	PROB.	LEMS	134
	NOTA	TION	146
6.	PIPE I	FLOW	149
	I.	FLOW REGIMES	149
	II.	GENERAL RELATIONS FOR PIPE FLOWS	151
		A. Energy Balance	151
		B. Momentum Balance	152
		C. Continuity	153
		D. Energy Dissipation	153
	III.	NEWTONIAN FLUIDS	154
		A. Laminar Flow	154
		B. Turbulent Flow	155
		C. All Flow Regimes	164
	IV.	POWER LAW FLUIDS	164
		A. Laminar Flow	165
		B. Turbulent Flow	166
		C. All Flow Regimes	166
	V.	BINGHAM PLASTICS	167
		A. Laminar Flow	168
		B. Turbulent Flow	169
		C. All Reynolds Numbers	169
	VI.	PIPE FLOW PROBLEMS	169
		A. Unknown Driving Force	170
		B. Unknown Flow Rate	172
		C. Unknown Diameter	174
		D. Use of Tables	177
	VII.	TUBE FLOW (POISEUILLE) VISCOMETER	177
	VIII.	TURBULENT DRAG REDUCTION	178
	PROB	LEMS	184
	NOTA	TION	192
	REFE	RENCES	193
7.	INTER	RNAL FLOW APPLICATIONS	195
	I.	NONCIRCULAR CONDUITS	195
		A. Laminar Flows	195
		B. Turbulent Flows	198

Contents	хi
----------	----

	TT	MOOT FOOMOMICAL DIAMETER	200
	II.	MOST ECONOMICAL DIAMETER	200
		A. Newtonian Fluids	203
	111	B. Non-Newtonian Fluids EDICTION LOSS IN VALVES AND EITTINGS	205
	III.	FRICTION LOSS IN VALVES AND FITTINGS	206
		A. Loss Coefficient B. Favirulant I / D Mathed	207
		B. Equivalent L/D MethodC. Crane Method	207 208
			208 209
		D. 2-K (Hooper) Method	209
	IV.	E. 3-K (Darby) Method NON-NEWTONIAN FLUIDS	209
	1 V . V.	PIPE FLOW PROBLEMS WITH FITTINGS	214
	v .		215
		A. Unknown Driving ForceB. Unknown Flow Rate	217
		C. Unknown Diameter	217
	VI.		221
		PIPE NETWORKS	225
		BLEMS	228
		ATION	237
		ERENCES	238
8.	PUM	PS AND COMPRESSORS	239
8.	PUMI	PUMPS	239
8.		PUMPS A. Positive Displacement Pumps	239 239
8.	I.	PUMPS A. Positive Displacement Pumps B. Centrifugal Pumps	239 239 240
8.	I.	PUMPS A. Positive Displacement Pumps B. Centrifugal Pumps PUMP CHARACTERISTICS	239 239
8.	I.	PUMPS A. Positive Displacement Pumps B. Centrifugal Pumps PUMP CHARACTERISTICS PUMPING REQUIREMENTS AND PUMP	239 239 240 241
8.	I.	PUMPS A. Positive Displacement Pumps B. Centrifugal Pumps PUMP CHARACTERISTICS PUMPING REQUIREMENTS AND PUMP SELECTION	239 239 240 241 243
8.	I.	PUMPS A. Positive Displacement Pumps B. Centrifugal Pumps PUMP CHARACTERISTICS PUMPING REQUIREMENTS AND PUMP SELECTION A. Required Head	239 239 240 241 243 244
8.	I. II. III.	PUMPS A. Positive Displacement Pumps B. Centrifugal Pumps PUMP CHARACTERISTICS PUMPING REQUIREMENTS AND PUMP SELECTION A. Required Head B. Composite Curves	239 239 240 241 243
8.	I.	PUMPS A. Positive Displacement Pumps B. Centrifugal Pumps PUMP CHARACTERISTICS PUMPING REQUIREMENTS AND PUMP SELECTION A. Required Head B. Composite Curves CAVITATION AND NET POSITIVE SUCTION	239 239 240 241 243 244 245
8.	I. II. III.	PUMPS A. Positive Displacement Pumps B. Centrifugal Pumps PUMP CHARACTERISTICS PUMPING REQUIREMENTS AND PUMP SELECTION A. Required Head B. Composite Curves CAVITATION AND NET POSITIVE SUCTION HEAD (NPSH)	239 239 240 241 243 244 245
8.	I. II. III.	PUMPS A. Positive Displacement Pumps B. Centrifugal Pumps PUMP CHARACTERISTICS PUMPING REQUIREMENTS AND PUMP SELECTION A. Required Head B. Composite Curves CAVITATION AND NET POSITIVE SUCTION HEAD (NPSH) A. Vapor Lock and Cavitation	239 239 240 241 243 244 245 247
8.	I. II. III.	PUMPS A. Positive Displacement Pumps B. Centrifugal Pumps PUMP CHARACTERISTICS PUMPING REQUIREMENTS AND PUMP SELECTION A. Required Head B. Composite Curves CAVITATION AND NET POSITIVE SUCTION HEAD (NPSH) A. Vapor Lock and Cavitation B. NPSH	239 239 240 241 243 244 245 247 247 247
8.	I. II. III.	PUMPS A. Positive Displacement Pumps B. Centrifugal Pumps PUMP CHARACTERISTICS PUMPING REQUIREMENTS AND PUMP SELECTION A. Required Head B. Composite Curves CAVITATION AND NET POSITIVE SUCTION HEAD (NPSH) A. Vapor Lock and Cavitation B. NPSH C. Specific Speed	239 239 240 241 243 244 245 247 247 247 248 249
8.	I. II. III.	PUMPS A. Positive Displacement Pumps B. Centrifugal Pumps PUMP CHARACTERISTICS PUMPING REQUIREMENTS AND PUMP SELECTION A. Required Head B. Composite Curves CAVITATION AND NET POSITIVE SUCTION HEAD (NPSH) A. Vapor Lock and Cavitation B. NPSH C. Specific Speed D. Suction Specific Speed	239 239 240 241 243 244 245 247 247 248 249 250
8.	I. II. III.	PUMPS A. Positive Displacement Pumps B. Centrifugal Pumps PUMP CHARACTERISTICS PUMPING REQUIREMENTS AND PUMP SELECTION A. Required Head B. Composite Curves CAVITATION AND NET POSITIVE SUCTION HEAD (NPSH) A. Vapor Lock and Cavitation B. NPSH C. Specific Speed D. Suction Specific Speed COMPRESSORS	239 239 240 241 243 244 245 247 247 248 249 250 252
8.	I. II. III.	PUMPS A. Positive Displacement Pumps B. Centrifugal Pumps PUMP CHARACTERISTICS PUMPING REQUIREMENTS AND PUMP SELECTION A. Required Head B. Composite Curves CAVITATION AND NET POSITIVE SUCTION HEAD (NPSH) A. Vapor Lock and Cavitation B. NPSH C. Specific Speed D. Suction Specific Speed COMPRESSORS A. Isothermal Compression	239 239 240 241 243 244 245 247 247 248 249 250 252 254
8.	I. II. III.	PUMPS A. Positive Displacement Pumps B. Centrifugal Pumps PUMP CHARACTERISTICS PUMPING REQUIREMENTS AND PUMP SELECTION A. Required Head B. Composite Curves CAVITATION AND NET POSITIVE SUCTION HEAD (NPSH) A. Vapor Lock and Cavitation B. NPSH C. Specific Speed D. Suction Specific Speed COMPRESSORS A. Isothermal Compression B. Isentropic Compression	239 239 240 241 243 244 245 247 247 248 249 250 252 254 254
8.	I. II. III.	PUMPS A. Positive Displacement Pumps B. Centrifugal Pumps PUMP CHARACTERISTICS PUMPING REQUIREMENTS AND PUMP SELECTION A. Required Head B. Composite Curves CAVITATION AND NET POSITIVE SUCTION HEAD (NPSH) A. Vapor Lock and Cavitation B. NPSH C. Specific Speed D. Suction Specific Speed COMPRESSORS A. Isothermal Compression	239 239 240 241 243 244 245 247 247 248 249 250 252 254

xii		Contents
	PROBLEMS	256
	NOTATION	265
	REFERENCES	266
9.	COMPRESSIBLE FLOWS	267
	I. GAS PROPERTIES	267
	A. Ideal Gas	267
	B. The Speed of Sound	268
	II. PIPE FLOW	270
	A. Isothermal Flow	271
	B. Adiabatic Flow	273
	C. Choked Flow	273
	D. The Expansion Factor	275
	E. Ideal Adiabatic Flow	277
	III. GENERALIZED EXPRESSIONS	279
	A. Governing Equations	279
	B. Applications	281
	C. Solution of High-Speed Gas Problems	283
	PROBLEMS	286
	NOTATION	290
	REFERENCES	291
10.	FLOW MEASUREMENT AND CONTROL	293
	I. SCOPE	293
	II. THE PITOT TUBE	293
	III. THE VENTURI AND NOZZLE	295
	IV. THE ORIFICE METER	304
	A. Incompressible Flow	305
	B. Compressible Flow	306
	V. LOSS COEFFICIENT	308
	VI. ORIFICE PROBLEMS	310
	A. Unknown Pressure Drop	311
	B. Unknown Flow Rate	311
	C. Unknown Diameter	312
	VII. CONTROL VALVES	312
	A. Valve Characteristics	313
	B. Valve Sizing Relations	314
	C. Compressible Fluids	327
	D. Viscosity Correction	330
	PROBLEMS	333

Con	Contents		xiii
		ATION ERENCES	338 339
11.	EXT	ERNAL FLOWS	341
	Ι.	DRAG COEFFICIENT	341
		A. Stokes Flow	342
		B. Form Drag	343
		C. All Reynolds Numbers	343
		D. Cylinder Drag	344
		E. Boundary Layer Effects	345
	11.	FALLING PARTICLES	347
		A. Unknown Velocity	348
		B. Unknown Diameter	349
		C. Unknown Viscosity	349
	III.	CORRECTION FACTORS	350
		A. Wall Effects	350
		B. Drops and Bubbles	351
	IV.	NON-NEWTONIAN FLUIDS	352
		A. Power Law Fluids	352
		B. Wall Effects	357
		C. Carreau Fluids	358
		D. Bingham Plastics	358
	PRO:	BLEMS	361
	NOT	ATION	363
	REF	ERENCES	364
12.	FLUI	ID-SOLID SEPARATIONS BY FREE SETTLING	365
	I.	FLUID-SOLID SEPARATIONS	365
	II.	GRAVITY SETTLING	366
	III.	CENTRIFUGAL SEPARATION	367
		A. Fluid-Solid Separation	367
		B. Separation of Immiscible Liquids	371
	IV.	CYCLONE SEPARATIONS	375
	2	A. General Characteristics	375
		B. Aerocyclones	376
		C. Hydrocyclones	382
	PRO	BLEMS	385
		ATION	389
		ERENCES	390

XIV			Contents
13.	FLO	W IN POROUS MEDIA	391
	I.	DESCRIPTION OF POROUS MEDIA	391
		A. Hydraulic Diameter	392
		B. Porous Medium Friction Factor	393
		C. Porous Medium Reynolds Number	394
	Π.	FRICTION LOSS IN POROUS MEDIA	394
		A. Laminar Flow	394
		B. Turbulent Flow	395
		C. All Reynolds Numbers	395
	III.	PERMEABILITY	395
	IV.	MULTIDIMENSIONAL FLOW	396
	V.	PACKED COLUMNS	398
	VI.	FILTRATION	401
		A. Governing Equations	401
		B. Constant Pressure Operation	405
		C. Constant Flow Operation	406
		D. Cycle Time	406
		E. Plate-and-Frame Filters	407
		F. Rotary Drum Filter	408
		G. Compressible Cake	408
		BLEMS	409
		TATION	417
	REF	ERENCES	418
14.	FLU	IDIZATION AND SEDIMENTATION	419
	I.	FLUIDIZATION	419
		A. Governing Equations	420
		B. Minimum Bed Voidage	421
		C. Nonspherical Particles	421
	11.	SEDIMENTATION	423
		A. Hindered Settling	423
		B. Fine Particles	425
		C. Coarse Particles	428
		D. All Flow Regimes	428
	III.	GENERALIZED SEDIMENTATION/	
		FLUIDIZATION	430
	IV.	THICKENING	430
		BLEMS	436
	NOT	ATION	441
	REF	ERENCES	442