# THE CHEMICAL EQUILIBRIUM OF GASEOUS SYSTEMS

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### CZECHOSLOVAK ACADEMY OF SCIENCES

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### **Preface**

It is the purpose of this book to present a concise and sufficiently detailed description of the present state and possibilities of calculating chemical equilibria of gas mixtures. It is based on a book by one of the authors, published in Czech by the Publishing House Academia in Prague. The rapid development of the topic during the two years since publication of the Czech edition has made it necessary to revise practically all the sections in order to bring them up to the present level of knowledge.

One reason for writing this book was the practical requirement of contemporary industry, where a rational utilization of equilibrium composition calculations may provide valuable information concerning processes under study in all stages of their implementation. A second reason was the need of a text-book for studying this part of chemical thermodynamics in the scope as taught at the Institute of Chemical Technology, Prague.

These two basic motives determine the overall structure of the book, as well as the proportions and arrangement of the chapters. The book includes fundamental thermodynamic concepts as well as the mathematical apparatus needed to solve the problems involved, care being taken that the discussion should always lead to a practical procedure of performing equilibrium calculations in gas-phase systems of any degree of complexity whatever. Knowledge of chemical thermodynamics on the level of a fundamental university course is assumed.

The book is divided into seven chapters. A brief definition of the topic in Chapter 1 is followed by stoichiometric analysis of chemically reacting systems, leading up to an absolutely generalized description of the application of linear algebra methods.

Chapter 3 discusses the thermodynamic fundamentals of equilibrium behaviour, defines equilibrium criteria and indicates briefly the possibilities of their characterization.

Chapter 4 includes the calculation of chemical equilibria in simple systems in the ideal gas state, and the determination of the influence of simple reaction variables.

Chapter 5 is a review of methods employed to calculate complicated chemical equilibria in the ideal gas state. By means of detailed analysis, four very reliable and quite generalized procedures were selected. These have been practically tested and are described in complete detail up to the stage of block diagrams, from which prac-

tical programmes can be developed easily. Thus the procedures can readily be used to solve practical tasks in isothermic and adiabatic arrangements.

Chapter 6 describes the application of the individual methods for calculating equilibria in real gas systems.

Chapter 7 presents a critical survey of sources of thermochemical data, their calculation or estimation, method of tabulation, instructions for carrying out calculations with respect to maximum technological utilization of the results of calculations and an example of the treatment of a system of practical interest; errors, which may cause some uncertainty in the calculation, are briefly analyzed.

The book is amplified by a number of Appendices summing up some non-conventional mathematical procedures, proofs and some of the most important thermo chemical and physico-chemical data. In order to facilitate the understanding of illustrative problems and — at the same time — to stimulate the interest of the workers active in the industrial branches, we retained the traditional units (cal, K, atm).

We hope that this book will contribute to a more intensive application of methods of chemical equilibrium calculation, for which modern data processing equipment provides all necessary conditions. We also hope to have contributed a little towards making this branch of chemical thermodynamics as well known as it deserves to be in view of its practical application.

Finally, we should like to express our sincere thanks to Prof. Dr. Ing. Eduard Hála, Dr.Sc. and Prof. Dr. Ing. Jiří Pick, Dr.Sc. for valuable advice, Ing. Milan Šolc for carefully reading the manuscript and for helpful discussion, Dr. Ota Sofr for the translation and last not least, Mrs. Jaroslava Margoliusová for carefully typing the manuscript and drawing the pictures.

Prague, June 1974

Robert Holub Petr Voňka

# List of Symbols

```
constant of the relationship C_P as function of T
a
             constant of the relationship (C_P)_i as function of T
a;
             constant of the Beattie-Bridgman equation
a, a_i
             constant of the Benedict-Webb-Rubin equation
a, a_i
             activity of the constituent i
a_i
             constitution coefficient (denotes the number of atoms of the element j,
a_{ij}
             present in the compound i)
             chemical formula of the compound i
A_i
A_0
             constant of the Beattie-Bridgman equation
A_k
             constant of the power series K_a as function of T
h
             constant of the relationship C_P as function of T
             constant of the relationship (C_P)_i as function of T
b_i
b, b,
             constant of the Beattie-Bridgman equation
             constant of the Benedict-Webb-Rubin equation
b, b_i
B
             constant
B, B'
             second virial coefficient
             second virial coefficient of the interaction between constituents j and k
B_{ik}
             reduced second virial coefficient
B_{r}
             chemical symbol of an element, or chemical formula of a basic particle
\mathbf{B}_{i}
             species
\mathbf{B}_{k}
             constant of the relationship of the second virial coefficient as function
\mathbf{B}_{0}
             constant of the Beattie-Bridgman equation
             constant of the Benedict-Webb-Rubin equation
\mathbf{B}_{0}
             constant of the relationship C_P as function of T
             constant of the relationship (C_P)_i as function of T
C_i
             constant of the Beattie-Bridgman equation
c, c;
             constant of the Benedict-Webb-Rubin equation
c, c_i
             constituent concentration
C_i
             = (G_i^{\circ}/RT) + \ln P
C_i
C, C'
            constant
             molar heat
C_{P}
```

 $(C_P)_i$ molar heat of constituent i C, C'third virial coefficient  $C_{ikl}$ third virial coefficient of the interaction between the constituents i, k and I  $C_k$ constant of the relationship  $C_P$  as function of T  $C_{r}$ reduced third virial coefficient d total differential of the quantity denoted by the following symbol d bond length D, D'fourth virial coefficient fourth virial coefficient of the interaction between the constituents  $D_{jklp}$ j, k, l, and pvalue of  $(G^{\circ}/RT)$  corresponding to the j-th element or basic particle  $e_{j}$  $E^{o}$ standard electromotoric force f fugacity  $f_i$ fugacity of constituent i  $f_r$ function symbol Ffree energy (Helmholtz function)  $F_{i}$ free energy (Helmholtz function) of constituent i FFaraday constant F function symbol G free enthalpy (Gibbs function) free enthalpy (Gibbs function) of constituent i  $G_i$  $G_{\mathbf{f}}$ free enthalpy of formation Hrank of a matrix of constitution coefficients Henthalpy  $H_i$ enthalpy of the constituent i enthalpy of formation  $H_{\mathbf{f}}$  $H_{r}$ enthalpy of chemical reaction (heat of reaction) integration constant of the heat of reaction vs. temperature relationship  $I_H$ integration constant of the equilibrium constant vs. temperature re- $I_{K}$ lationship K Kelvin  $K, K_a, K_r$ equilibrium constant  $K_f$ equilibrium constant of reaction of formation Mnumber of elements (basic particle species) in a closed system  $M_i$ molecular weight of compound i overall number of moles in a system nnumber of moles of constituent i  $n_i$ number of compounds in a closed system N  $= \sum_{k=1}^{M} a_{ik} \lambda_k - c_i$ 

 $p_i$ 

```
P
             number of linear combinations of columns of the matrix of constitution
             coefficients
P
             overall pressure in a system
             partial pressure of constituent i
P_i
P_c
             critical pressure
             reduced pressure
P_{r}
             coefficient of a system of linear equations
r_{ik}
             number of linearly independent reactions
R
R
             gas constant
            = n_i + \sum_{r=H+1}^N v_{ri} n_r
q_i
            function symbol V, G/RT
Q
S
            entropy
             reciprocal value of the overall number of moles (1/n)
t
T
            absolute temperature
T_c
            critical temperature (K)
             reduced temperature
T_{r}
            function symbol
u
             = (n^{(p+1)}/n^{(p)} - 1)
u
U
            internal energy
            molar volume
V
            molar volume of the constituent i
V ;
V
            overall volume
W
            function symbol
            molar fraction of constituent i
y_i
            linking condition
Z
            compressibility factor
            critical compressibility factor
Z_{c}
            Superscripts
            quantity in equilibrium
e
M
            quantity of mixing
            quantity in standard state (or pure constituent)
0
            initial value (zero-th approximation)
0
            step (p-th approximation of the quantity denoted by the preceding
p
            symbol)
            notation of alternative quantity, denoted by the preceding symbol
            partial molar quantity
            under conditions close to ideal ones
            Subscripts
            critical state
C
```

```
f
             for reaction of formation
i
             index of summation for compounds (1, 2, ..., N)
             index of summation for elements (basic particle species) (1, 2, ..., N)
j
k
             index of summation
1
             index of summation
             relating to mixture
m
             index of summation
p
             index of summation for reactions (1, 2, ..., R)
             reduced state
r
             index of summation
S
             required value of quantity denoted by the preceding symbol
X
             Greek letters
             constant of the Benedic-Webb-Rubin equation
\alpha, \alpha_i
             directional angle
α
B
             functional expression in the Beattie-Bridgman equation
\beta_r
             correction factor, replacing the reaction coordinate \xi_r
             functional expression in the Beattie-Bridgman equation
γ
             constant of the Benedict-Webb-Rubin equation
\gamma, \gamma_i
             dimension-less function of free enthalpy (equal to G/RT, or \sum_{i=1}^{N} f_i)
Г
0
             partial differential
8
             functional expression in the Beattie-Bridgman equation
             Kronecker's delta (unit diagonal matrix of the dimension j \times k)
\delta_{ik}
Δ
             final difference, or deviation of quantity following the symbol
             arbitrarily small positive number
3
2
             Lagrangian multiplier
λ
             magnitude of step
\lambda_i
             arbitrary chosen vector, substituting a stoichiometric coefficient
             chemical potential of constituent i
\mu_i
             stoichiometric coefficient (denotes the number of moles of the i-th
v_{ri}
             constituent taking part in the r-th reaction)
\xi_{r}
\prod_{i=1}^{N}
             reaction coordinate (degree of conversion, extent of reaction)
             reaction coordinate of the r-th reaction
             denotes the product over i (i = 1, 2, ..., N)
             reciprocal molar volume (1/v)
             denotes the sum over i (i = 1, 2, ..., N)
             fugacity coefficient of constituent i
\varphi_i
             function symbol
Φ
```

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### 1 Introduction

Chemical equilibrium can be established when a system contains constituents between which chemical conversion can take place. Determination of the products which can be formed by chemical conversion of the initial constituents and of the composition of the system in equilibrium is one of the frequent, important and often highly interesting problems which have to be solved in practice.

Up to recent times, when the chemical industry was still mainly based on coal, organic syntheses set out from relatively pure individual compounds e.g. acetylene, ethylene, benzene, etc., reacting systems could generally be described by means of a simple chemical reaction. With conversion of the chemical industry to oil and petrochemical processes, it becomes increasingly important to utilize multi-component mixtures as raw materials. This development is supported by economic aspects as well as progress in chemical technology, instrumental analysis and engineering. Separation of the components from petroleum or its fractions is difficult and expensive, while on the other hand, contemporary technology, utilizing modern analytical techniques is able to study even highly complex reaction systems. In this situation it is essential to be able to calculate the chemical equilibrium of systems in which several chemical reactions will be taking place.

There is no difficulty in calculating the chemical equilibrium of a system, in which a single chemical reaction takes place. The calculation, however, becomes increasingly difficult with the rising number of simultaneous reactions, until application of the same procedure to systems with more than three reactions proceeding simultaneously is practically impossible. Therefore, techniques have had to be worked out for more complicated chemically reacting systems, based on principles somewhat different from those of simple equilibrium calculation. The result are methods which allow equilibrium compositions to be calculated for systems of any degree of complexity whatever, in the ideal as well as real gas state.

A survey of the most important and generally applicable procedures, together with practical instructions for their application in solving actual problems is the topic of this book.

# 2 Stoichiometry of chemical reactions

In chemistry, stoichiometry is conventionally understood to mean the relationship between elements or fundamental particles and components in their mutual conversions. In the field of chemical equilibria, stoichiometry permits investigation of concentration changes as well as an accurate determination of the maximum number of reactions which may take place in a system, and allows the optimum combinations of these reactions to be selected. For this reason, equilibrium considerations proper must be preceded by a detailed stoichiometrical analysis of the system involved. This puppose may well be achieved by utilization of linear algebra, and a closed system may be described formally as a system of linear algebraic equations.

### 2.1 DEFINITION OF A CHEMICAL REACTION

Let us consider a closed system consisting of M elements and N constituents. Let  $A_i$  stand for the i-th constituent and  $B_j$  for the j-th element. Then,

$$A_i = \sum_{j=1}^{M} a_{ij} B_j \quad i = 1, 2, ..., N$$
 (2.1)

where  $a_{ij}$  is the constitution coefficient, denoting the number of gram atoms of the j-th element in the i-th constituent.

For conventional use this intuitive concept of a compound is sufficient, and there is no difficulty in extending it to a radical. Provided an electron is additionally defined as one of the set of elementary particles  $B_j$ , ions may also be considered to be independent constituents.

When every compound is described as a line vector of constitutional coefficients, a system of N constituents may be defined by a matrix of  $N \times M$  elements. Clearly the elements of this matrix must be non-negative integers. With regard to the physical sense of the matrix, none of its rows or columns may be composed exclusively of zeros.