

**INORGANIC**  
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**CHEMICALS**  
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**HANDBOOK**  
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VOLUME  
**1**

EDITED BY

**JOHN J. MCKETTA**

# INORGANIC CHEMICALS HANDBOOK

VOLUME  
1

EDITED BY

JOHN J. MCKETTA

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**INORGANIC  
CHEMICALS  
HANDBOOK**

## Preface

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We feel there is a need for a handbook for inorganic chemicals, covered in a well-organized manner. This handbook presents up-to-date inorganic processing operations and includes design and operating information. Each topic is written by a world expert in that particular area in such a manner that it is easily understood and applied. Each professional practicing engineer or industrial chemist involved in inorganic chemicals should have a copy of this book on his or her working shelf.

The handbook is conveniently presented in alphabetical order. Volume 1 covers topics from aluminum through chloralkali and chlorine; Volume 2 continues with subtopics of chloralkali and proceeds through potash, caustic. An upcoming Volume 3 will cover the rest of the alphabet. Each of the processing articles contains information on plant design as well as significant chemical reactions. Wherever possible, shortcut methods of calculations are included, along with nomographic methods of solutions. In the front of the book are two convenient sections that will be very helpful to the reader. These are (1) conversion to and from SI units and (2) cost indexes that will enable the reader to update any cost information.

As editor, I am grateful for all the help I have received from the great numbers of authors who have contributed to this book. I am also grateful to the huge number of readers who have written to me with suggestions of topics to be included.

JOHN J. McKETTA

## Contributors

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- Joseph M. Abrardo** Technology Manager, PSG Process Engineering, Air Products and Chemicals, Inc., Allentown, Pennsylvania
- J. C. Agarwal** Charles River Associates Incorporated, Boston, Massachusetts
- E. S. Atkinson** Product Manager, Pulp Mill Systems, Industrial Systems, Hooker Chemicals and Plastics Corporation, Niagara Falls, New York
- Calvin L. Ayres** Lead Process Engineer, PSG Process Engineering, Air Products and Chemicals, Inc., Allentown, Pennsylvania
- P. G. Blakey** Vice President, Electronic Gases, Airco, Murray Hill, New Jersey
- Roger Bowlin** Technical Manager, Process Research, Dow Chemical Company, Plaquemine, Louisiana
- Robert H. Brown** Natrona Heights, Pennsylvania; Former Assistant Director of Research, Alcoa Laboratories, Alcoa Center, Pennsylvania
- Jack E. Buice** Process Associate, Technology Center, Dow Chemical Company, Freeport, Texas
- David W. Bunch** Supervisor, Research and Development Department, Ethyl Corporation, Baton Rouge, Louisiana
- A. B. Campanaro** Purchasing Department, Stauffer Chemical Company, Westport, Connecticut
- S. C. Carapella, Jr.** Central Research Department, ASARCO, Inc., South Plainfield, New Jersey
- E. J. Claassen, Ph.D.** Consultant, and Champion Technologies, Inc. (Retired), Odessa, Texas
- Thomas W. Clapper, Ph.D.** President, Clapper Enterprises Inc., Oklahoma City, Oklahoma
- D. A. Coleman** Industrial Chemical Division, Stauffer Chemical Company, Westport, Connecticut
- Bruce D. Craig, Ph.D.** Metallurgical Consultants, Inc. of Denver, Denver, Colorado
- John E. Currey** Manager, Commercial Development, Hooker Chemicals and Plastics Corporation, Niagara Falls, New York
- Dale C. DeWitt** Process Engineering Group Leader, MCC Engineering Department, Monsanto Chemical Company, St. Louis, Missouri

- Robert DiNapoli** Vice President and Partner, Merlin Associates, Inc., Atlanta, Georgia
- A. M. Dowell, III, P.E.** Technical Fellow, Risk Analysis, Rohm and Haas Texas Inc., Deer Park, Texas
- C. R. Eberline** Senior Development Engineer, Research and Development, Phillips Petroleum Company, Bartlesville, Oklahoma
- Philip J. Ehman** Technical Consultant, Technical Center, The Ansul Company, Weslaco, Texas
- Richard A. Flinn, Sc.D.** Professor Emeritus, Materials Science and Engineering, The University of Michigan, Ann Arbor, Michigan
- Gary E. Foltz, Ph.D.** Technology Director, FINC-Lithium Division, Bessemer City, North Carolina
- J. M. Ford** Senior Engineering Associate, Olin Corporation, Charleston, Tennessee
- R. C. Fullerton-Batten** Product Manager, Beryllium Metal Sales, Kawecki Berylco Industries, Inc., Reading, Pennsylvania
- David R. Gard, Ph.D.** Associate Science Fellow, Detergents and Phosphates Division, Monsanto Chemical Company, St. Louis, Missouri
- Thomas E. Guenter** Engineering Associate, E. I. du Pont de Nemours and Company, Memphis, Tennessee
- Subhash C. Gupta** Metallurgical Engineer, Badger Engineers, Inc., Cambridge, Massachusetts
- Donald J. Haase** Manager of COSORB Technology, Organics and Polymers Division, Tenneco Chemicals, Houston, Texas
- Lucius Hannon, Jr.** President, Hannon-Western Engineers, Dallas, Texas
- J. A. Hawk, Jr.** Vice President, Kawecki Berylco Industries, Inc., Reading, Pennsylvania
- D. W. Hayes** E. I. du Pont de Nemours and Company, Aiken, South Carolina
- Lyn M. Himmelberger** Regional Manager, Sales and Marketing, Cryogenics Industries, Inc., Allentown, Pennsylvania
- Herwig Höger** Works Manager, Süddeutsche Kalkstickstoff-Werke AG, Trostberg, Germany
- Robert R. Huebel, P.E.** Director, Process Design Engineering, The Randall Corporation, Houston, Texas
- H. Z. Hurlburt** Director, Peiser Laboratories, Stauffer Chemical Company, Houston, Texas
- Daniel W. Hurley** Chief Administrative Officer, Cookson America, Inc. Providence, Rhode Island

- Bimal Kumar Jain** Chemical Engineer, New Alipore, Calcutta, India
- Paul H. Johnson** Manager, Carbon Black Branch, Research and Development, Phillips Petroleum Company, Florham Park, New Jersey
- D.W. Jones** E. I. du Pont de Nemours and Company, Aiken, South Carolina
- Werner Joseph** Director of Metallurgy, South American Consolidated Enterprises, Brussels, Belgium
- R. S. Joyce** Senior Research Associate, Activated Carbon Research, Research and Development Department, Calgon Corporation, Pittsburgh, Pennsylvania
- Vinayaka Kahol** Himachal Pradesh State Industrial Development Ltd., Shimla, Himachal Pradesh, India
- F. E. Katrak** Charles River Associates Incorporated, Boston, Massachusetts
- Kestutis A. Keblys** Supervisor, Research and Development Department, Ethyl Corporation, Ferndale, Michigan
- S. Krishnamurthy** Central Electrochemical Research Institute, Kararkudi, Tamilnadu, India
- Walter B. Kropf** Metals Division, Vulcan Materials Company, Sandusky, Ohio
- A. J. Kubicek** Area Superintendent, Houston Chemical Company, Beaumont, Texas
- Joseph B. Kuhn** Product Engineer, Kawecki Berylco Industries, Inc., Reading, Pennsylvania
- C. R. Lahiri, Ph.D.** Professor, Department of Applied Chemistry, University College of Technology, Calcutta University, Calcutta, India
- M. J. Loreth** Charles River Associates Incorporated, Boston, Massachusetts
- W. Stuart Lyman** Manager, Technical and Market Services, Copper Development Association Inc., New York, New York
- Kenneth W. Mall** Senior Environmental Associate, Dow Chemical Company, Midland, Michigan
- W. L. Marter** E. I. du Pont de Nemours and Company, Aiken, South Carolina
- Zenji Matsumoto** Senior Researcher, Takeda Chemical Industries, Ltd., Shimizushi, Japan
- Allen B. Mavity** Engineering Associate, Chemicals Group Technical Center, PPG Industries, Inc., Monroeville, Pennsylvania
- D. J. Maykuth** Assistant Division Manager (Retired), Nonferrous Metallurgy Division, Battelle Columbus Laboratories, Columbus, Ohio
- John J. McKetta, Ph.D., P.E.** The Joe C. Walter Professor of Chemical Engineering, The University of Texas at Austin, Austin, Texas



- Richard F. Merritt, Ph.D.** Research Section Manager, Rohm and Haas Company, Spring House, Pennsylvania
- Leonard O. Moore** Manager of Research and Development, Technical Center, The Ansul Company, Weslaco, Texas
- R. A. Mostello, Ph.D., P.E.** Principal Engineering Associate, Process Engineering, BOC Cryopplants, Murray Hill, New Jersey
- S. Muthukumaraswamy** Executive Supervisor, Switchgear Engineering, Bharat Heavy Electricals Ltd., Bhopal, Madhya Pradesh, India
- D. J. Muyskens** Market Research, FMC Corporation, Princeton, New Jersey
- V. Narasimham** Chief Mechanical Engineer, Gwalior Rayon Silk Manufacturing (Weaving) Company, Ltd., Chemical Division, Bombay, India
- Koichi Numasaki** Senior Deputy General Manager, CWM Business Promotion Office, JGC Corporation, Tokyo, Japan
- Ernest O. Ohsol, Sc.D.** Consulting Chemical Engineer, Crosby, Texas
- Keith W. Padgett** The Canadian Kellogg Company, Ltd., Toronto, Canada
- Ashok V. Parekh** Works Manager, Gwalior Rayon Silk Manufacturing (Weaving) Company, Ltd., Chemical Division, Bombay, India
- Kashinath Z. Patil, M.Sc., M.Tech.** Catalyst Consultant, Houston, Texas
- Gerald G. Pumplin** Consultant, Hooker Chemicals and Plastics Corporation, Niagara Falls, New York
- Orlando J. Quartulli** Pullman Kellogg Division, Pullman Incorporated, Hackensack, New Jersey
- E. Rau** Assistant Director, Process Development, FMC Corporation, Princeton, New Jersey
- S. Ray** Department of Applied Chemistry, University College of Technology, Calcutta, India
- James G. Rigsby** Senior Associate Development Engineer (Retired), Olin Corporation, Lake Charles, Louisiana
- A. M. Sass** Consultant, San Rafael, California
- W. A. Satterwhite** Cities Service Company, Minerals Group, Tulsa, Oklahoma
- Charles M. Schillmoller** Consultant, Nickel Development Institute, Toronto, Ontario, Canada
- W. C. Schreiner** Director of Development, Pullman Kellogg, Houston, Texas
- S. N. Sharma** Scientist, Department of Technology Utilisation, Council of Scientific and Industrial Research, New Delhi, India

- Kenneth J. Shaver** Senior Research Group Leader, Monsanto Company, St. Louis, Missouri
- Baldev Singh** Professorial Fellow, Centre for Contemporary Studies, Nehru Memorial Museum and Library, New Delhi, India
- N. M. Singh, Ph.D.** Consultant, New Delhi, India
- J. D. Stephens, P. Eng.** Materials Engineering and Testing, Cominco Engineering Services, Ltd., Trail, British Columbia, Canada
- R. E. Strock, Jr.** Regional Manager, Beryllium Metal Sales, Kawecki Berylco Industries, Inc., Reading, Pennsylvania
- Cheryl I. Teich, Ph.D.** Research Process Engineer, Separation Technologies Research, Rohm and Haas Company, Spring House, Pennsylvania
- R. Thangappan** Central Electrochemical Research Institute, Kararkudi, Tamilnadu, India
- D. H. Tucker** Production Area Manager, Cyanohydrin Department, Rohm and Haas Texas, Inc., Deer Park, Texas
- Philip C. Tully, Ph.D., P.E.** Chief, Office of Planning and Analysis, Helium Field Operations, U.S. Bureau of Mines, Amarillo, Texas
- D. W. Tunison** Technical Superintendent, FMC Corporation, Modesto, California
- William Turner** Director of Process Engineering, Kellogg International Corporation (affiliate of Pullman Kellogg), Wembley, Middlesex, England
- Christiaan P. van Dijk** Senior Scientist, Pullman Kellogg, Houston, Texas
- John S. Waltrip** Chemicals and Metals Department, Magnesium TS & D, Lake Jackson Research Center, Dow Chemical Company, Freeport, Texas
- William P. Webb** Senior Engineer, Failure Analysis Associates, Alexandria, Virginia
- Keith G. Wikle** Application Engineering, Kawecki Berylco Industries, Inc., Reading, Pennsylvania
- J. Wilder** Charles River Associates Incorporated, Boston, Massachusetts
- S. Mark Wilhelm, Ph.D.** Manager, Chemistry Division, Cortest Laboratories, Inc., Houston, Texas
- James A. Wilkinson** Associate Process Consultant, Dow Chemical Company, Freeport, Texas

# Conversion to SI Units

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To convert from	To	Multiply by
acre	square meter (m <sup>2</sup> )	$4.046 \times 10^3$
angstrom	meter (m)	$1.0 \times 10^{-10}$
are	square meter (m <sup>2</sup> )	$1.0 \times 10^2$
atmosphere	newton/square meter (N/m <sup>2</sup> )	$1.013 \times 10^5$
bar	newton/square meter (N/m <sup>2</sup> )	$1.0 \times 10^5$
barrel (42 gallon)	cubic meter (m <sup>3</sup> )	0.159
Btu (International Steam Table)	joule (J)	$1.055 \times 10^3$
Btu (mean)	joule (J)	$1.056 \times 10^3$
Btu (thermochemical)	joule (J)	$1.054 \times 10^3$
bushel	cubic meter (m <sup>3</sup> )	$3.52 \times 10^{-2}$
calorie (International Steam Table)	joule (J)	4.187
calorie (mean)	joule (J)	4.190
calorie (thermochemical)	joule (J)	4.184
centimeter of mercury	newton/square meter (N/m <sup>2</sup> )	$1.333 \times 10^3$
centimeter of water	newton/square meter (N/m <sup>2</sup> )	98.06
cubit	meter (m)	0.457
degree (angle)	radian (rad)	$1.745 \times 10^{-2}$
denier (international)	kilogram/meter (kg/m)	$1.0 \times 10^{-7}$
dram (avoirdupois)	kilogram (kg)	$1.772 \times 10^{-3}$
dram (troy)	kilogram (kg)	$3.888 \times 10^{-3}$
dram (U.S. fluid)	cubic meter (m <sup>3</sup> )	$3.697 \times 10^{-6}$
dyne	newton (N)	$1.0 \times 10^{-5}$
electron volt	joule (J)	$1.60 \times 10^{-19}$
erg	joule (J)	$1.0 \times 10^{-7}$
fluid ounce (U.S.)	cubic meter (m <sup>3</sup> )	$2.96 \times 10^{-5}$
foot	meter (m)	0.305
furlong	meter (m)	$2.01 \times 10^2$
gallon (U.S. dry)	cubic meter (m <sup>3</sup> )	$4.404 \times 10^{-3}$
gallon (U.S. liquid)	cubic meter (m <sup>3</sup> )	$3.785 \times 10^{-3}$
gill (U.S.)	cubic meter (m <sup>3</sup> )	$1.183 \times 10^{-4}$
grain	kilogram (kg)	$6.48 \times 10^{-5}$
gram	kilogram (kg)	$1.0 \times 10^{-3}$
horsepower	watt (W)	$7.457 \times 10^2$
horsepower (boiler)	watt (W)	$9.81 \times 10^3$
horsepower (electric)	watt (W)	$7.46 \times 10^2$
hundred weight (long)	kilogram (kg)	50.80
hundred weight (short)	kilogram (kg)	45.36
inch	meter (m)	$2.54 \times 10^{-2}$
inch mercury	newton/square meter (N/m <sup>2</sup> )	$3.386 \times 10^3$
inch water	newton/square meter (N/m <sup>2</sup> )	$2.49 \times 10^2$
kilogram force	newton (N)	9.806

To convert from	To	Multiply by
kip	newton (N)	$4.45 \times 10^3$
knot (international)	meter/second (m/s)	0.5144
league (British nautical)	meter (m)	$5.559 \times 10^3$
league (statute)	meter (m)	$4.83 \times 10^3$
light year	meter (m)	$9.46 \times 10^{15}$
liter	cubic meter (m <sup>3</sup> )	0.001
micron	meter (m)	$1.0 \times 10^{-6}$
mil	meter (m)	$2.54 \times 10^{-6}$
mile (U.S. nautical)	meter (m)	$1.852 \times 10^3$
mile (U.S. statute)	meter (m)	$1.609 \times 10^3$
millibar	newton/square meter (N/m <sup>2</sup> )	100.0
millimeter mercury	newton/square meter (N/m <sup>2</sup> )	$1.333 \times 10^2$
oersted	ampere/meter (A/m)	79.58
ounce force (avoirdupois)	newton (N)	0.278
ounce mass (avoirdupois)	kilogram (kg)	$2.835 \times 10^{-2}$
ounce mass (troy)	kilogram (kg)	$3.11 \times 10^{-2}$
ounce (U.S. fluid)	cubic meter (m <sup>3</sup> )	$2.96 \times 10^{-5}$
pascal	newton/square meter (N/m <sup>2</sup> )	1.0
peck (U.S.)	cubic meter (m <sup>3</sup> )	$8.81 \times 10^{-3}$
pennyweight	kilogram (kg)	$1.555 \times 10^{-3}$
pint (U.S. dry)	cubic meter (m <sup>3</sup> )	$5.506 \times 10^{-4}$
pint (U.S. liquid)	cubic meter (m <sup>3</sup> )	$4.732 \times 10^{-4}$
poise	newton second/square meter (N · s/m <sup>2</sup> )	0.10
pound force (avoirdupois)	newton (N)	4.448
pound mass (avoirdupois)	kilogram (kg)	0.4536
pound mass (troy)	kilogram (kg)	0.373
poundal	newton (N)	0.138
quart (U.S. dry)	cubic meter (m <sup>3</sup> )	$1.10 \times 10^{-3}$
quart (U.S. liquid)	cubic meter (m <sup>3</sup> )	$9.46 \times 10^{-4}$
rod	meter (m)	5.03
roentgen	coulomb/kilogram (c/kg)	$2.579 \times 10^{-4}$
second (angle)	radian (rad)	$4.85 \times 10^{-6}$
section	square meter (m <sup>2</sup> )	$2.59 \times 10^6$
slug	kilogram (kg)	14.59
span	meter (m)	0.229
stoke	square meter/second (m <sup>2</sup> /s)	$1.0 \times 10^{-4}$
ton (long)	kilogram (kg)	$1.016 \times 10^3$
ton (metric)	kilogram (kg)	$1.0 \times 10^3$
ton (short, 2000 pounds)	kilogram (kg)	$9.072 \times 10^2$
torr	newton/square meter (N/m <sup>2</sup> )	$1.333 \times 10^2$
yard	meter (m)	0.914

## Bringing Costs up to Date

Cost escalation via inflation bears critically on estimates of plant costs. Historical costs of process plants are updated by means of an escalation factor. Several published cost indexes are widely used in the chemical process industries:

Nelson-Farrar Cost Indexes (*Oil and Gas J.*), quarterly  
Marshall and Swift (M&S) Equipment Cost Index, updated monthly  
CE Plant Cost Index (*Chemical Engineering*), updated monthly  
ENR Construction Cost Index (*Engineering News-Record*), updated weekly

All these indexes were developed with various elements, such as material availability and labor productivity, taken into account. However, the proportion allotted to each element differs with each index. The differences in overall results of each index are due to uneven price changes for each element. In other words, the total escalation derived by each index will vary because different bases are used. The engineer should become familiar with each index and its limitations before using it.

Table 1 compares the CE Plant Index with the M&S Equipment Cost

**TABLE 1** *Chemical Engineering and Marshall and Swift Plant and Equipment Cost Indexes since 1950*

Year	CE Index	M&S Index	Year	CE Index	M&S Index
1950	73.9	167.9	1971	132.3	321.3
1951	80.4	180.3	1972	137.2	332.0
1952	81.3	180.5	1973	144.1	344.1
1953	84.7	182.5	1974	165.4	398.4
1954	86.1	184.6	1975	182.4	444.3
1955	88.3	190.6	1976	192.1	472.1
1956	93.9	208.8	1977	204.1	505.4
1957	98.5	225.1	1978	218.8	545.3
1958	99.7	229.2	1979	238.7	599.4
1959	101.8	234.5	1980	261.2	659.6
1960	102.0	237.7	1981	297.0	721.3
1961	101.5	237.2	1982	314.0	745.6
1962	102.0	238.5	1983	316.9	760.8
1963	102.4	239.2	1984	322.7	780.4
1964	103.3	241.8	1985	325.3	789.6
1965	104.2	244.9	1986	318.4	797.6
1966	107.2	252.5	1987	323.8	813.6
1967	109.7	262.9	1988	342.5	852.0
1968	113.6	273.1	1989	355.4	895.1
1969	119.0	285.0	1990	357.6	915.1
1970	125.7	303.3	1991	361.3	930.6

**TABLE 2** Nelson-Farrar Inflation Refinery Construction Indexes since 1946  
(1946 = 100)

Date	Materials Component	Labor Component	Miscellaneous Equipment	Nelson-Farrar Inflation Index
1946	100.0	100.0	100.0	100.0
1947	122.4	113.5	114.2	117.0
1948	139.5	128.0	122.1	132.5
1949	143.6	137.1	121.6	139.7
1950	149.5	144.0	126.2	146.2
1951	164.0	152.5	145.0	157.2
1952	164.3	163.1	153.1	163.6
1953	172.4	174.2	158.8	173.5
1954	174.6	183.3	160.7	179.8
1955	176.1	189.6	161.5	184.2
1956	190.4	198.2	180.5	195.3
1957	201.9	208.6	192.1	205.9
1958	204.1	220.4	192.4	213.9
1959	207.8	231.6	196.1	222.1
1960	207.6	241.9	200.0	228.1
1961	207.7	249.4	199.5	232.7
1962	205.9	258.8	198.8	237.6
1963	206.3	268.4	201.4	243.6
1964	209.6	280.5	206.8	252.1
1965	212.0	294.4	211.6	261.4
1966	216.2	310.9	220.9	273.0
1967	219.7	331.3	226.1	286.7
1968	224.1	357.4	228.8	304.1
1969	234.9	391.8	239.3	329.0
1970	250.5	441.1	254.3	364.9
1971	265.2	499.9	268.7	406.0
1972	277.8	545.6	278.0	438.5
1973	292.3	585.2	291.4	468.0
1974	373.3	623.6	361.8	522.7
1975	421.0	678.5	415.9	575.5
1976	445.2	729.4	423.8	615.7
1977	471.3	774.1	438.2	653.0
1978	516.7	824.1	474.1	701.1
1979	573.1	879.0	515.4	756.6
1980	629.2	951.9	578.1	822.8
1981	693.2	1044.2	647.9	903.8
1982	707.6	1154.2	622.8	976.9
1983	712.4	1234.8	656.8	1025.8
1984	735.3	1278.1	665.6	1061.0
1985	739.6	1297.6	673.4	1074.4
1986	730.0	1330.0	684.4	1089.9
1987	748.9	1370.0	703.1	1121.5
1988	802.8	1405.6	732.5	1164.5
1989	829.2	1440.4	769.9	1195.9
1990	832.8	1487.7	797.5	1225.7
1991	832.3	1533.3	827.5	1252.9

Index. Table 2 shows the Nelson-Farrar Inflation Petroleum Refinery Construction Indexes since 1946. It is recommended that the CE Index be used for updating total plant costs and the M&S Index or Nelson-Farrar Index for updating equipment costs. The Nelson-Farrar Indexes are better suited for petroleum refinery materials, labor, equipment, and general refinery inflation.

Since

$$C_B = C_A(B/A)^n \quad (1)$$

Here,  $A$  = the size of units for which the cost is known, expressed in terms of capacity, throughput, or volume;  $B$  = the size of unit for which a cost is required, expressed in the units of  $A$ ;  $n = 0.6$  (i.e., the six-tenths exponent);  $C_A$  = actual cost of unit  $A$ ; and  $C_B$  = the cost of  $B$  being sought for the same time period as cost  $C_A$ .

To approximate a current cost, multiply the old cost by the ratio of the current index value to the index at the date of the old cost:

$$C_B = C_A I_B / I_A \quad (2)$$

Here,  $C_A$  = old cost;  $I_B$  = current index value; and  $I_A$  = index value at the date of old cost.

Combining Eqs. (1) and (2),

$$C_B = C_A(B/A)^n(I_B/I_A) \quad (3)$$

For example, if the total investment cost of plant  $A$  was \$25,000,000 for 200-million-lb/yr capacity in 1974, find the cost of plant  $B$  at a throughput of 300 million lb/yr on the same basis for 1986. Let the sizing exponent,  $n$ , be equal to 0.6.

From Table 1, the CE Index for 1986 was 318.4, and for 1974 it was 165.4. Via Eq. (3),

$$\begin{aligned} C_B &= C_A(B/A)^n(I_B/I_A) \\ &= 25.0(300/200)^{0.6}(318.4/165.4) \\ &= \$61,200,000 \end{aligned}$$

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