Jean-Charles Régin Michel Rueher (Eds.)

Integration
of AI and OR Techniques
in Constraint Programming
for Combinatorial
Optimization Problems

First International Conference, CPAIOR 2004 Nice, France, April 2004 Proceedings



1918-53 <del>C88</del>2 Jean-Charles Régin Michel Rueher (Eds.)

# Integration of AI and OR Techniques in Constraint Programming for Combinatorial Optimization Problems

First International Conference, CPAIOR 2004 Nice, France, April 20-22, 2004 Proceedings







Springer

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Library of Congress Control Number: 2004103824

CR Subject Classification (1998): G.1.6, G.1, G.2.1, F.2.2, I.2, J.1

ISSN 0302-9743 ISBN 3-540-21836-X Springer-Verlag Berlin Heidelberg New York

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Typesetting: Camera-ready by author, data conversion by DA-TeX Gerd Blumenstein Printed on acid-free paper SPIN: 10997383 06/3142 5 4 3 2 1 0

## 3011

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### **Preface**

This volume contains the proceedings of the 1st International Conference on Integration of AI and OR Techniques in Constraint Programming for Combinatorial Optimisation Problems. This new conference follows the series of CP-AI-OR International Workshops on Integration of AI and OR Techniques in Constraint Programming for Combinatorial Optimisation Problems held in Ferrara (1999), Paderborn (2000), Ashford (2001), Le Croisic (2002), and Montreal (2003). The success of the previous workshops has demonstrated that CP-AI-OR is becoming a major forum for exchanging ideas and methodologies from both fields. The aim of this new conference is to bring together researchers from AI and OR, and to give them the opportunity to show how the integration of techniques from AI and OR can lead to interesting results on large-scale and complex problems.

The integration of techniques from artificial intelligence and operations research has provided effective algorithms for tackling complex and large-scale combinatorial problems with significant improvements in terms of efficiency, scalability and optimality. The benefit of this integration has been shown in applications such as hoist scheduling, rostering, dynamic scheduling and vehicle routing. At the programming and modelling levels, most constraint languages embed OR techniques to reason about collections of constraints, so-called global constraints. Some languages also provide support for hybridization allowing the programmer to build new integrated algorithms. The resulting multi paradigm programming framework combines the flexibility and modelling facilities of constraint programming with the special purpose and efficient methods from operations research.

CP-AI-OR 2004 was intended primarily as a forum to focus on the integration of the approaches of CP, AI and OR technologies. A secondary aim was to provide an opportunity for researchers in one area to learn about techniques in the others. Fifty-six papers were submitted in response to the call for papers. After the reviewing period and some online discussions, the program committee met physically at Nice on January 30 and 31, 2004. The program committee decided to accept 23 technical papers and 7 short papers. Short papers present interesting recent results or novel thought-provoking ideas that are not quite ready for a regular full-length paper. Both types of papers were reviewed rigorously and held to a very high standard.

CP-AI-OR 2004 was fortunate to attract outstanding invited talks. Heinrich Braun and Thomas Kasper discussed the challenges of optimization problems in supply chain management. Ignacio Grossmann proposed a hybrid framework that uses mathematical and constraint programming for the scheduling of batch chemical processes. Michel Minoux told us about strengthened relaxations for some CP-resistant combinatorial problems and their potential usefulness.

We wish to thank our generous sponsors who allowed us to offer substantial allowances to students attending the conference in order to cover their expenses.

#### VI Preface

We extend our gratitude to the outstanding program committee who worked very hard under tight deadlines. We are deeply grateful to Claude Michel who worked in the trenches in preparing the CP meeting at Nice and who dealt with all the difficult organization aspects of this conference.

April 2004

Jean-Charles Régin and Michel Rueher

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# Using MILP and CP for the Scheduling of Batch Chemical Processes

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Abstract. A hybrid framework that uses Mathematical and Constraint Programming for the scheduling of batch chemical processes is proposed. Mathematical programming is used for the high-level optimization decisions (number and type of tasks, and assignment of equipment units to tasks), and Constraint Programming is used for the low-level sequencing decisions. The original problem is decomposed into an MILP master problem and a CP subproblem. The master MILP is a relaxation of the original problem, and given a relaxed solution, the CP subproblem checks whether there is a feasible solution and generates integer cuts. The proposed framework is based on the hybrid algorithm of Maravelias and Grossmann ([1],[2]), and can be used for different objective functions and different plant configurations. In this paper we present the simplifications and enhancements that allow us to use the proposed framework in a variety of problems, and report computational results.

#### 1 Introduction

Scheduling of operations is a common and very important problem in the chemical industry. While related problems have been extensively studied in the Operations Research literature (see [3]), this area has only been addressed recently in process systems engineering (see [4], [5], [6], [7] for reviews).

In terms of plant configurations, problems in chemical industry can be classified into four major categories. In multiple-unit or single-stage plants (Figure 1.a), there are N orders to be scheduled in M units. In flow-shop multi-stage plants (Figure 1.b), there are N orders to be processed in K stages, following the same order. Each stage  $k \in \{1, ... K\}$  consists of  $M_k$  units, and each order must be processed by one unit in each stage. In general multi-stage plants (Figure 1.c), each order must be processed in all stages but not in the same order. Multipurpose batch plants (Figure 1.d), finally, can be viewed as a generalization of all previous configurations, where batch splitting and mixing, as well as recycle streams are present. It should be noted that the original work in process scheduling concentrated mostly on flow-shop and general multi-stage batch plants (see [3], [5]). The study of general multipurpose plants was largely promoted by the work of Kondili et al. [8].

Preemption is usually not allowed, and utility constraints (e.g. manpower, cooling water, etc.), and release/due times may be present in all configurations. Different storage policies, such as unlimited intermediate storage (UIS), finite intermediate

J.-C. Régin and M. Rueher (Eds.): CPAIOR 2004, LNCS 3011, pp. 1-20, 2004. © Springer-Verlag Berlin Heidelberg 2004

storage (FIS), no intermediate storage (NIS) and zero-wait (ZW), are used in multipurpose and multi-stage plants, while in singe-stage plants it is usually assumed that unlimited storage is available. Furthermore, the batch size of a task may be variable, which in many cases leads to variable duration and utility requirements. In terms of objective functions, the most common ones: maximization of production over a fixed time horizon, minimization of makespan for given demand and minimization of cost for given demand with due dates.

A feature that makes scheduling problems in chemical industry hard to solve is that usually the type and number of tasks (jobs) are not uniquely defined, and moreover, a specific task can be performed in more than one unit. These problems are hard to solve because of the large number of different solutions, and have not been studied extensively. Problems where the number and type of tasks are fixed and each task can be assigned to only one machine, on the other hand, have been extensively studied in OR community and efficient algorithms exist for many of these problems.

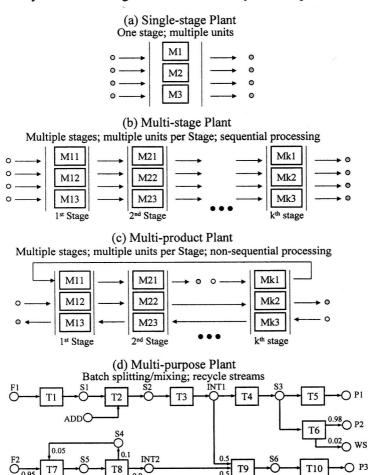


Fig. 1. Common plant configurations in chemical industry

Due to the different plant configurations and process specifications, a wide variety of optimization models, mainly MILP models, have been proposed in the process systems engineering literature. In multipurpose batch plants, for instance, where the level of inventories and the level of resource consumption should be monitored and constrained, the time horizon is partitioned into a sufficiently large number of periods, and variables and constraints are defined for each time period. In single-stage plants, on the other hand, where no batch splitting, mixing and recycle streams are allowed, batch sizes are usually assumed to be constant and this, in turn means that mass balance equations need not be included in the formulation. If, in addition, there are no utility constraints the time horizon is not partitioned into common time periods, and hence, assignment binaries are indexed by tasks and unit time slots, which are generally fewer than time periods. When the number of tasks and the assignments of tasks to units are known, assignments binaries and constraints are dropped, and sequencing binaries are used instead.

In an effort to develop a general representation that can be used in the majority of scheduling problems of chemical industry, Kondili et al. [8] proposed the discrete-time State Task Network (STN) representation, and the equivalent Resource Task Network (RTN) representation was proposed by Pantelides [9]. To overcome some limitations of discrete-time models, several authors proposed continuous-time STN/RTN models ([10], [11], [12], [13], [14]). While being very general, STN and RTN-based models are computationally inefficient for many classes of problems. The computational performance of both models is very poor, for instance, when the objective is the minimization of makespan for a given demand. Finally, STN-based models do not exploit the special structure of simple configurations, being orders of magnitude slower than special purpose MILP models.

To address these issues, Maravelias and Grossmann proposed a general hybrid MILP/CP iterative algorithm ([1], [2]) for the scheduling of multipurpose plants that exploits the complementary strengths of Mathematical and Constraint Programming. In this paper we show how this hybrid algorithm can be modified to address scheduling problems in multi-stage and single-stage plants. It is shown that the same idea can be used in all these configurations: use MILP to find a partial solution that includes the type and number of tasks and the assignments of units to tasks, and use CP to check feasibility, generate integer cuts and derive complete schedules.

In the section 2 we briefly present the hybrid algorithm of Maravelias and Grossmann. In section 3 we present the different types of problems, and in sections 4 and 5 we present how this algorithm can be modified to address these problems. Finally, we report computational results to show that order-magnitude reductions in computation time are possible with the proposed hybrid schemes.

### 2 Hybrid MILP/CP Algorithm

The main idea of the proposed algorithm is to use MILP to optimize (identify partial, potentially good solutions), and CP to check feasibility and derive complete, feasible schedules. Specifically, an iterative scheme where we iterate between a MILP master problem and a CP subproblem is proposed. The type and number of tasks to be performed and the assignment of tasks to equipment units are determined in the